



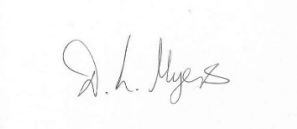
Client
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 Ermine Business Park
 Huntingdon
 Cambridgeshire
 PE29 6XX

Part 1: Executive Summary

Report for the Periodic Monitoring of Emissions to Air.

Site	Huntingdon
Plant	LEV 1
Sampling Date	28th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4

Report Approved by:	Sign		
	Print	Derek Myers	
	MCERTS No.	MM02 115	Level 2 TE: 1,2,3,4

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Monitoring Objectives

The monitoring was undertaken to check compliance with authorised emission limits.

All monitoring procedures were carried out to the MCERTS requirements under the Exova (UK) Ltd quality system to ISO 17025: 2005.

Monitoring was undertaken for the listed emissions from the following sampling positions:

Sampling Location	Emission
LEV 1	Total volatile organic carbon

Special Monitoring Requirements

There were no special requirements for this monitoring campaign.

Summary of Methods

Emission	Method number	Method standard
Gas velocity and volume flow TOC	TPM/01A MM0002	BS EN ISO 16911-1:2013 BS EN 12619 : 2013

Summary Of Results

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 1	Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
	Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	28/01/16	14:23	15:53	49.7	75	1.5	0.2	171.5

* at reference conditions	Stack Gas Weight 29.00 Kg/kmol	0 °C 101.3 kPa	Without correction for moisture Oxygen No Correction %
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Where applicable

Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report:

* Reference conditions (see above)
** Analysis not required
ND Non detectable
s - Subcontracted laboratory analysis

Nm³ 273 K, 101.3 kPa
- UKAS accredited only
- Not Accredited
N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated.
Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Summary Of Results, Exhaust Gases

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 1		Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
		Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	Test 1	28/01/16	14:23	14:53	48.4	75	1.5	0.2	167.1
TOC	Test 2	28/01/16	14:53	15:23	44.9	75	1.5	0.2	154.9
TOC	Test 3	28/01/16	15:23	15:53	55.8	75	1.6	0.2	192.6

* at ref	Stack Gas Weight	0 °C	Without correction for moisture
Conditions	29.00 Kg/kmol	101.3 kPa	Oxygen No Correction %

Where applicable

Oxides of nitrogen results are expressed as nitrogen dioxide

TOC results are expressed as total carbon

Throughout Report:

* Reference conditions (see above)

Nm³ 273 K, 101.3 kPa

** Analysis not required

- UKAS accredited only

ND Non detectable

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s - Subcontracted laboratory analysis

N/A Not applicable

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Operating Information

The table below shows details of the operating information on each sampling date for: **LEV 1**

Date	Process type	Process duration	Fuel	Feedstock	Abatement	Load
28/01/2016	Production and cleaning of inkjet cartridges	Continuous	N/A	N/A	N/A	Normal

No CEMs installed on the emission point.

Comments & Monitoring Deviations

A waste gas homogeneity test to BS EN 15259:2007 (MID) is not required:-

The homogeneity test is not applicable to non-combustion processes.

The homogeneity test is not applicable to duct areas less than 1m².

The homogeneity test is not usually applicable to pollutant emissions that are less than 30% of the ELV.

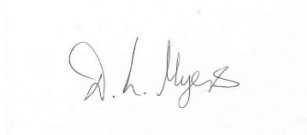
All monitoring was performed in accordance with the relevant procedures.



Part 2: Supporting Information

Report for the Periodic Monitoring of Emissions to Air.

Client	Xaarjet Ltd
Site	Huntingdon
Plant	LEV 1
Sampling Date	28th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
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APPENDIX 1

Emission Monitoring Procedures And Instrumentation

Gas velocity and temperature

Documented in-house procedure TPM01/A to the main procedural requirements of BS EN ISO 16911-1:2013
Velocity and temperature measurements are performed using a calibrated Pitot tube, a calibrated pressure differential reading device and a calibrated thermocouple. Velocity and possible flow deviation measurements are carried out at selected, representative points in the gas stream.

Total organic carbon

Documented in-house procedure MM0002 to the main procedural requirements of BS EN 12619:2013.
Continuous analysis using probe, sample line and multi range Flame Ionisation Detector (FID) analyser. The analyser is calibrated before and during the tests using certified gas mixtures of nitrogen, oxygen and propane. Sampling points are selected in accordance with the findings of any BS EN 15259 assessment.

Sampling Project Personnel Competency And Expiry Dates

		MCERTS No	Level 1	Level 2	TE1	TE2	TE3	TE4
Report prepared by:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Report authorised by:	Derek Myers	MM02 115	-	30/09/2017	31/05/2018	30/11/2018	30/11/2018	30/11/2018
Team leader:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Team leader:	Harpreet Badwal	MM03 149	-	30/09/2018	30/09/2018	30/04/2019	31/10/2019	31/10/2019

Equipment References

Equipment	Reference Number
FID	AQ271
Heated Line	HL40
Stack Thermocouple	PTTS97
Timer / Stopwatch	ST41
Barometer	WS03
Pitot	PT97
Thermometer	TK24
Manometer	PI03

APPENDIX 2

Date	28/01/2016
Time	12:20
Pitot Cp	0.79

Barometric pressure	101.6	kPa
Duct static pressure	0.08	kPa
Stack Area	0.126	m ²

Stack Diameter (circular)	0.40	m
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Traverse Point	Traverse Line	Depth cm	ΔP mmH ₂ O	T °C	Angle °	velocity m/s	Traverse Line	Depth cm	ΔP mmH ₂ O	T °C	Angle °	velocity m/s
1	A						B					
2	A						B					
3	A	5.0	3.1	22	<15	5.6	B	5.0	9.0	22	<15	9.6
4	A	7.1	4.0	22	<15	6.4	B	7.1	7.4	22	<15	8.7
5	A	10.0	4.8	22	<15	7.0	B	10.0	7.0	22	<15	8.5
6	A	14.2	5.7	22	<15	7.6	B	14.2	6.2	22	<15	8.0
7	A	25.8	7.4	22	<15	8.7	B	25.8	5.4	22	<15	7.4
8	A	30.0	8.5	22	<15	9.3	B	30.0	6.0	22	<15	7.8
9	A	32.9	8.9	22	<15	9.5	B	32.9	7.3	22	<15	8.6
10	A	35.0	8.5	22	<15	9.3	B	35.0	8.8	22	<15	9.5
11	A						B					
12	A						B					

Average Pitot DP	6.62	mmH ₂ O
Average Temperature	295.2	K
Average Velocity	8.2	m/s
Average volumetric flow rate	1.03	m ³ /s at stack conditions
Average volumetric flow rate	0.96	m ³ /s (wet STP)

Sampling plane requirements Re: BS EN 13284-1:2001 5.2

a	Angle of gas flow less than 15° with regard to duct axis	YES
b	No local negative flow	YES
c	Minimum pitot greater than 5Pa	YES
d	Ratio of highest to lowest local gas velocity less than 3:1	YES
	Minimum local gas velocity	5.6
	Maximum local gas velocity	9.6
	Ratio of highest to lowest local gas velocity	1.71

Preliminary Velocity Traverse Data

Date 28/01/2016

From 14:23 to 14:53 30 minute mean

Volatile organic compounds	vppm, wet	30.13	mg/m ³ *	48.42
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From 14:53 to 15:23 30 minute mean

Volatile organic compounds	vppm, wet	27.92	mg/m ³ *	44.87
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From 15:23 to 15:53 30 minute mean

Volatile organic compounds	vppm, wet	34.72	mg/m ³ *	55.80
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Sampling Detection Limits

Volatile organic compounds	vppm	0.10	mg/m ³ *	0.16
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Reference Gas Details

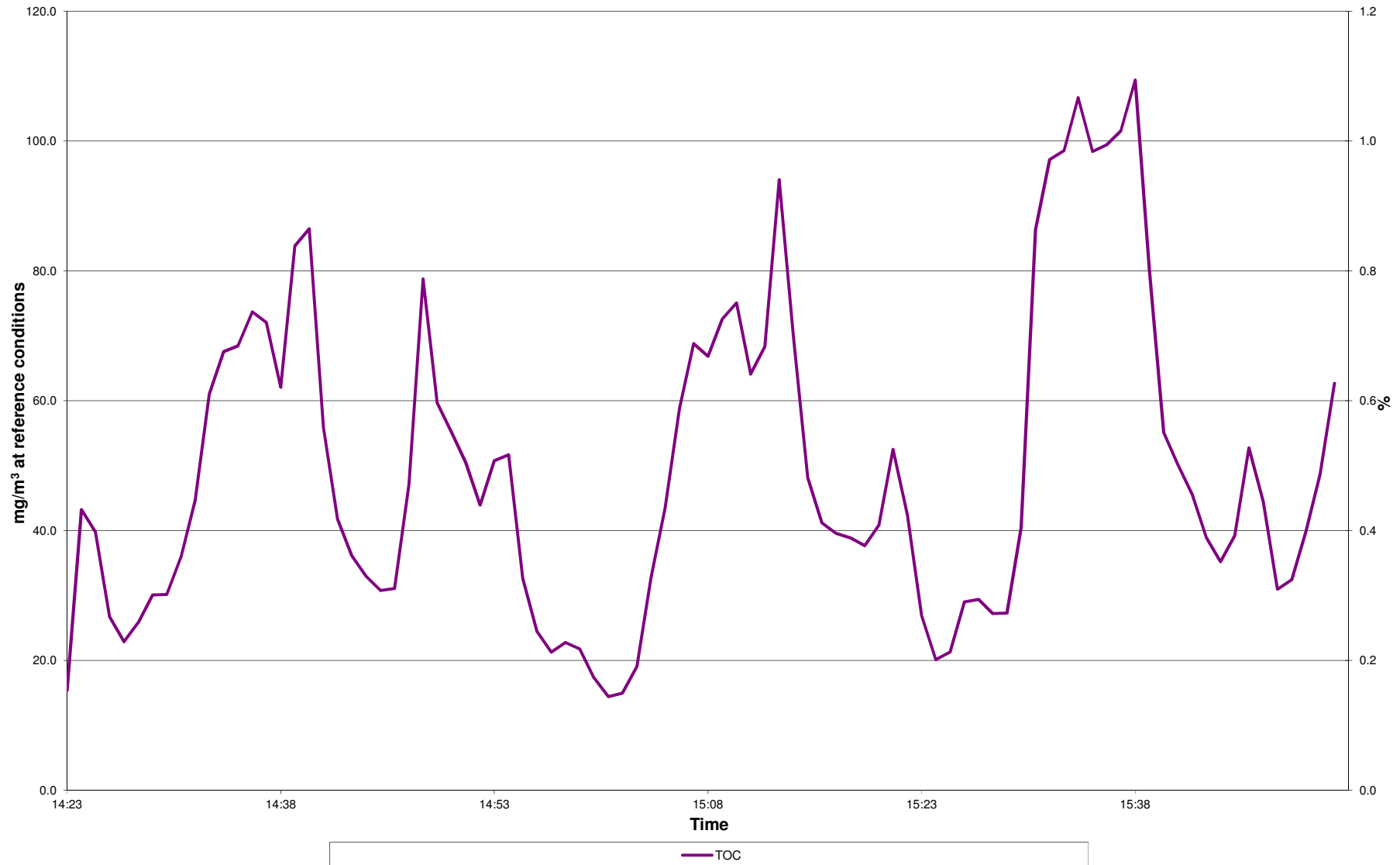
Species	Units	Value	Cylinder Reference	Analyser Range	Uncertainty <i>k</i> = 2
Nitrogen	%	99.999	VCK01959	-	± 2
Volatile organic compounds	vppm	75.50	VCSMG3066	10	± 2

Zero And Span Gas Details

Species	units	Initial Time	11:30	Final Time	16:00
		Initial Zero	Initial Span	Final Zero	Final Span
Volatile organic compounds	vppm	0.00	75.50	-0.04	75.63

Exhaust Gases - Continuous Analysis Data

Chart 1 - Exhaust Gases - Xaarjet Ltd, Huntingdon, LEV 1, 28/01/16



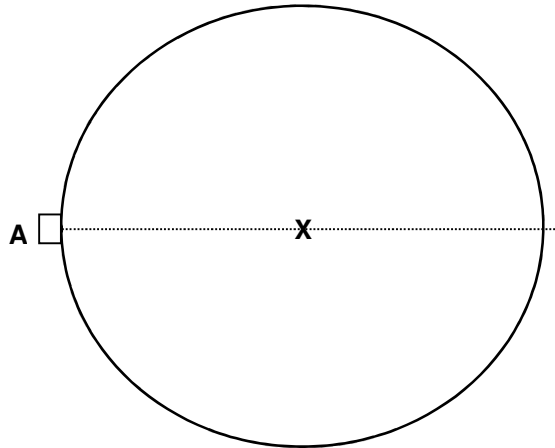
APPENDIX 3

Diagram Of The Sampling Location

Diagram of sampling points across the cross section of the duct (not to scale).

Traverse length = 0.40 m

Point	% of D	Location cm
1	50.0	20.0



General Calculations

Stack area:

$$\text{Area of a circle} = \frac{\pi \cdot D^2}{4}$$

D = Diameter (m)

π = 3.142

Pressure conversion:

1mmH₂O = 0.00980665 kPa

1mmH₂O = 9.80665 Pa

1 mar = 0.1 kPa

Water vapour concentration:

From reference calculations (taken from BS EN 14790):

$$V_{WC(\%)} = \frac{\frac{m_{WC} \cdot V_{mol(std)}}{M_w}}{\frac{m_{WC} \cdot V_{mol(std)}}{M_w} + V_{m(std)}} \times 100$$

WVC (%) = Water vapour content on wet basis, in volume % (m³ of water vapour in m³ of wet gas)

V_{m(std)} = Dry gas volume measured, corrected to standard conditions (m³)

m_{WC} = Mass of water collected in the impingers (g)

M_w = Molecular weight of water, 18.01534 rounded to 18 (g/mol)

V_{mol(std)} = Molar volume of water at standard conditions = 0.0224 (m³/mol)

Gas meter volume at standard conditions (STP)

From reference calculations (taken from BS EN 14790):

$$V_{m(std)} = y_d \times (V_2 - V_1) \times \frac{T_{std}}{T_m} \times \frac{p_m}{p_{std}}$$

V_{m(std)} = Dry gas meter volume at standard conditions (m³)

y_d = Gas meter calibration coefficient

(V₂-V₁) = Dry gas meter volume at actual conditions (m³)

T_m = Actual Temperature (K)

T_{std} = Standard temperature (273 K)

p_m = Absolute pressure at the gas meter (kPa)

p_{std} = Standard gas pressure (101.3 kPa)

Isokenetic Ratio (%):

From reference calculations (taken from EA TGN M2):

$$\text{IsokineticRatio}(\%) = \frac{\text{Velocity at the sampling nozzle}}{\text{Velocity of the stack gas}} \times 100$$

Estimating Measurement Uncertainty

Uncertainty estimates are calculated using the general rule of uncertainty propagation. Guidance is taken from publications including UKAS document M3003 and ISO 20988:2007.

Flow Calculations

Velocity:

From reference calculations (taken from ISO 10780):

$$\bar{v} = KC \sqrt{\frac{T_s \Delta p}{p_e M_s}}$$

\bar{v} = Average velocity (m/s)

C = velocity calculation constant = 129

T_s = Average stack temperature (K)

M_s = Molar mass of gas; assume 29 kg/kmol unless the molar mass is < 27 kg/kmol or > 31 g/kmol

K = Pitot calibration coefficient

p_e = Absolute gas pressure (kPa)

Δp = Average pitot tube pressure differential (kPa)

Volume flow rate

From reference calculations (taken from ISO 10780):

$$q_{va} = \bar{v} A$$

q_{va} = Average flow rate (m³/s)

\bar{v} = Average velocity (m/s)

A = Stack cross-sectional area (m²)

Volume flow rate corrected for moisture

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(100 - H_a)}{(100 - H_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

H_a = Moisture at actual conditions (%volume)

H_m = Reference moisture (%volume)

Volume flow rate corrected for temperature and pressure

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(T_m p_a)}{(T_a p_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

T_a = Temperature at actual conditions (K)

T_m = Reference Temperature (K)

p_a = Absolute gas pressure at actual conditions (kPa)

p_m = Reference pressure (kPa)

Volume flow rate corrected for oxygen

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(20.9 - O_{2,ref})}{(20.9 - O_{2,m})}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

$O_{2,m}$ = Actual oxygen concentration (%)

$O_{2,ref}$ = Reference oxygen concentration (%)

Concentration Calculations

Concentration:

From reference calculations (taken from BS EN 13284-1):

$$c = \frac{m}{V}$$

c = Concentration
 m = Mass of substance
 V = Volume sampled

Mass Emission

$$\text{Mass emission} = c \times q_m$$

c = Concentration
 q = Volume flow rate

Concentration corrected for oxygen:

From reference calculations (taken from BS ISO 9096):

$$c_m = c_a \times \frac{20.9 - O_{2,ref}}{20.9 - O_{2,a}}$$

cm = Concentration at reference conditions
 ca = Actual concentration
 $O_{2, ref}$ = Reference oxygen (%)
 $O_{2, a}$ = Actual Oxygen (%)

Concentration corrected for moisture:

From reference calculations (taken from BS ISO 9096):

Convert wet gas to dry gas

$$c_{dry} = c_{wet} \times \frac{100}{100 - H_a}$$

Convert dry gas to wet gas

$$c_{wet} = c_{dry} \times \frac{100 - H_a}{100}$$

c_{wet} = Concentration wet gas
 c_{dry} = Concentration dry gas
 H_a = Water vapour content (%vol)

Conversion of parts per million (ppm) to mg/m³

From reference calculations (taken from EA TGN M2):

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

When Converting TOC

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight of carbon in span gas}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

Calculation of Uncertainty Estimates - Instrumental Monitoring Techniques

Model equation

$$C_{ppm} = C_{reading} + Corr_{fit} + Corr_{0,dr} + Corr_{s,dr} + Corr_{rep} + Corr_{adj} + \sum_{i=1}^p Corr_{inf} + Corr_{int}$$

Where:

C_{ppm}	=	concentration in ppm	$Corr_{rep}$	=	correction of repeatability of measurement
$C_{NO,reading}$	=	concentration given by analyser	$Corr_{adj}$	=	correction of adjustment
$Corr_{fit}$	=	correction of lack of fit	$Corr_{inf}$	=	correction of influence quantities
$Corr_{0,dr}$	=	correction of zero drift	$Corr_{int}$	=	correction of interferences
$Corr_{s,dr}$	=	correction of span drift			

Calculation of partial uncertainties

$$u(Corr_{fit}) = \frac{\left(\frac{X_{fit,max}}{100 \times range} \right)}{\sqrt{3}} \quad \text{Where: } X_{fit,max} \text{ is the maximum allowable deviation from linearity}$$

Expressed as % of the range and calculated by applying a rectangular probability distribution

$$u(Corr_{0,dr}) = \frac{X_{0,dr}}{\sqrt{3}} \quad u(Corr_{s,dr}) = \frac{X_{s,dr}}{\sqrt{3}}$$

$$u(Corr_{rep}) = \max(S_{0,rep}; S_{s,rep}) = S_{rep} \quad \text{Where: } S_{r,0} \text{ is the standard uncertainty at zero level}$$

$$S_{r,s} \text{ is the standard uncertainty at span level}$$

$$u(Corr_{adj}) = u(Corr_{loss}) + u(Corr_{cal}) \quad \text{Where: } u(Corr_{loss}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{loss}) = \frac{C_{j,loss}}{\sqrt{3}} \quad u(Corr_{cal}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{cal}) = \frac{U_{cal}}{2} \quad c_{j,loss} \text{ is the concentration of sample loss at span level}$$

$$U_{cal} \text{ is the expanded uncertainty of the calibration gas}$$

$$u(Corr_{inf}) = c_j \sqrt{\frac{(x_{j,max} - x_{j,adj})^2 + (x_{j,min} - x_{j,adj})^2 + (x_{j,max} - x_{j,adj})(x_{j,min} - x_{j,adj})}{3}}$$

Where:

- c_j is the sensitivity coefficient of the influence quantity
- $x_{j,min}$ is the minimum value of the influence quantity during monitoring
- $x_{j,max}$ is the maximum value of the influence quantity during monitoring
- $x_{j,adj}$ is the value of the influence quantity during adjustment

$$u(Corr_{int}) = \frac{c_j}{Int_{j,test}} \sqrt{\frac{Int_{j,max}^2 + Int_{j,min} \times Int_{j,max} + Int_{j,min}^2}{3}}$$

and

$$u(\Sigma Corr_{int}) = \max[S_{Int,p}; S_{Int,n}] \quad \text{Where: } c_j \text{ is the sensitivity coefficient of the interferent j}$$

- $Int_{j,test}$ is the concentration of the interferent j used to determine c_j
- $Int_{j,min}$ is the minimum value of the interferent j quantity during monitoring
- $Int_{j,max}$ is the maximum value of the interferent j quantity during monitoring
- $Int_{j,adj}$ is the concentration of the interferent j in the cal gas used to adjust the analyser
- $S_{Int,p}$ is the sum of interferences with positive impact
- $S_{Int,n}$ is the sum of interferences with negative impact

Combined uncertainty

$$u(C_{ppm}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2}$$

$$\text{Overall expanded uncertainty (k = 2)} \quad U(C_m) = u(C_m) \times k$$

Uncertainty of NOx measurements

$$u(C_{NOx,conv}) = \frac{C_{NOx} \times R \times \eta}{\sqrt{3}} \quad \text{Where: } C_{NOx} \text{ is the concentration of NOx measured by the analyser}$$

- R is the ratio of NO:Nox in the stack gas
- η is the NOx converter efficiency

Combined uncertainty NOx measurements

$$u(C_{NOx,stack}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + u^2(Corr_{NOx,conv})}$$

Uncertainty of mass concentration at oxygen reference concentration

$$u(C_{O_2,ref}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + \left(\frac{u^2(O_{2,meas,dry})}{(21 - O_{2,meas,dry})^2} \right)}$$

Where:

$u(C_{O_2,ref})$	=	uncertainty associated with the mass concentration at O ₂ ref. concentration	in	mg/m ³
$C_{O_2,ref}$	=	mass concentration at O ₂ reference concentration	in	mg/m ³
$O_{2,meas}$	=	O ₂ measured concentration	in	% volume
$u((O_{2,meas})_{dry})$	=	uncertainty associated to the measured O ₂ concentration	in	% (relative to O ₂ meas)

APPENDIX 4

Uncertainty Estimate For The Measurement Of Total Organic Carbon

Analyser Type/Model

Sick Maihak

Reference Oxygen %

0

(0 = No correction)

		Test 1	Test 2	Test 3
Limit value	mg/m ³	75	75	75
Limit value	ppm	46.7	46.7	46.7
Measured concentration	ppm	30.1	27.9	34.7
Measured concentration	mg/m ³	48.4	44.9	55.8

Calibration gas	ppm	75.5	75.5	75.5
Calibration gas	mg/m ³	121.3	121.3	121.3
Analyser range	ppm	9.3	9.3	9.3
Analyser range	mg/m ³	15.0	15.0	15.0

Correction of Lack of Fit

Lack of fit	% range	2.0	2.0	2.0
	$u(\text{Corr}_{\text{lof}})$	0.11	0.11	0.11

Corrections of Zero and Span Drift

(* All drift is calculated for \therefore the residual is assumed to be < 5% $u(\text{max})$)

Zero Drift	% range	0.00	0.00	0.00
	$u(\text{Corr}_{\text{zdr}})$	0.00	0.00	0.00
Span Drift	% range	0.00	0.00	0.00
	$u(\text{Corr}_{\text{spr}})$	0.00	0.00	0.00

Correction of Repeatability of Measurement

Repeatability SD at span level (Not reported)	% range	0.0	0.0	0.0
	$u(\text{Corr}_{\text{rep}})$	0.00	0.00	0.00

Correction of adjustment

losses in the line	% range	0.13	0.13	0.13
	$u(\text{Corr}_{\text{loss}})$	0.02	0.02	0.03
Uncertainty of calibration gas	% range	2.0	2.0	2.0
	$u(\text{Corr}_{\text{cga}})$	0.30	0.28	0.35

Correction of Influence of Interferents

N ₂ O	% range			
	$u(\text{Corr}_{\text{N2O}})$	0.00	0.00	0.00
CO ₂	% range			
	$u(\text{Corr}_{\text{CO2}})$	0.00	0.00	0.00
CH ₄	% range			
	$u(\text{Corr}_{\text{CH4}})$	0.00	0.00	0.00
Total of interferent influences $u(\Sigma \text{Corr}_{\text{int}}) = \max[S_{\text{int},p}; S_{\text{int},s}]$	% range	2.50	2.50	2.50
	$u(\Sigma \text{Corr}_{\text{int}})$	0.16	0.16	0.16

Correction of Influence Quantities

Sensitivity to sample volume flow	% range	1.60	1.60	1.60
	$u(\text{Corr}_{\text{scv}})$	0.09	0.09	0.09
Sensitivity to atmospheric pressure (Not reported)	% range			
	$u(\text{Corr}_{\text{press}})$	0.00	0.00	0.00
Sensitivity to ambient temperature	% range	-2.40	-2.40	-2.40
	$u(\text{Corr}_{\text{temp}})$	-0.28	-0.28	-0.28
Sensitivity to electrical voltage (Not reported)	% range	0.50	0.50	0.50
	$u(\text{Corr}_{\text{voltage}})$	0.10	0.10	0.10

Maximum standard uncertainty	$u(\text{Corr}_{\text{max}})$	0.30	0.28	0.35
5% of maximum standard uncertainty	$u(\text{Corr}_{\text{5\%}})$	0.02	0.01	0.02

Interferent Concentration Variations	Minimum	Maximum	Value at cal	Performance	Units
CH ₄ range	0	10	0	50	mg/m ³
N ₂ O range	0	0	0	20	mg/m ³
CO ₂ range	8	12	0	15	mg/m ³
Oxygen effect variations	Minimum	Maximum	Value at cal	Performance	Units
Oxygen effect	0	20	0	2	mg/m ³

Influence Quantity Variations

	Minimum	Maximum	Value at cal	Performance	Units
Sensitivity to sample volume flow	55	65	60	5	l/h
Sensitivity to atmospheric pressure	99	100	99	1	kPa
Sensitivity to ambient temperature	278	313	288	10	K
Sensitivity to electrical voltage	187	250	230	5	V

Measurement uncertainty

		Test 1	Test 2	Test 3
Combined uncertainty	ppm	0.47	0.46	0.50
Combined uncertainty	mg/m ³	0.76	0.74	0.81

Expanded uncertainty expressed with a level of confidence of 95%, k=2

Overall uncertainty	ppm	0.9	0.9	1.0
Overall uncertainty	mg/m ³	1.5	1.5	1.6
Overall uncertainty relative to measured value	%	3.1	3.3	2.9
Overall uncertainty relative to range	%	10.2	9.9	10.8
Overall uncertainty relative to ELV	%	1.3	1.2	1.3

The uncertainty evaluation has been carried out in accordance with UKAS requirements.



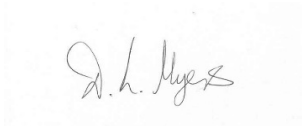
Client Xaarjet Ltd
1 Hurricane Close
Ermine Business Park
Huntingdon
Cambridgeshire
PE29 6XX

Part 1: Executive Summary

Report for the Periodic Monitoring of Emissions to Air.

Site	Huntingdon
Plant	LEV 2
Sampling Date	28th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4

Report Approved by:	Sign		
	Print	Derek Myers	
	MCERTS No.	MM02 115	Level 2 TE: 1,2,3,4



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Company Registration No SC070429

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Monitoring Objectives

The monitoring was undertaken to check compliance with authorised emission limits.

All monitoring procedures were carried out to the MCERTS requirements under the Exova (UK) Ltd quality system to ISO 17025: 2005.

Monitoring was undertaken for the listed emissions from the following sampling positions:

Sampling Location	Emission
LEV 2	Total volatile organic carbon

Special Monitoring Requirements

There were no special requirements for this monitoring campaign.

Summary of Methods

Emission	Method number	Method standard
Gas velocity and volume flow TOC	TPM/01A MM0002	BS EN ISO 16911-1:2013 BS EN 12619 : 2013

Summary Of Results

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 2	Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
	Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	28/01/16	11:45	13:15	3.8	75	1.2	0.2	5.7

* at reference conditions	Stack Gas Weight 29.00 Kg/kmol	0 °C 101.3 kPa	Without correction for moisture Oxygen No Correction %
---------------------------	-----------------------------------	-------------------	---

Where applicable

Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report:

* Reference conditions (see above)
** Analysis not required
ND Non detectable
s - Subcontracted laboratory analysis

Nm³ 273 K, 101.3 kPa
- UKAS accredited only
- Not Accredited
N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated.
Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Summary Of Results, Exhaust Gases

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 2		Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
		Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	Test 1	28/01/16	11:45	12:15	3.7	75	1.2	0.2	5.6
TOC	Test 2	28/01/16	12:15	12:45	3.1	75	1.2	0.2	4.5
TOC	Test 3	28/01/16	12:45	13:15	4.7	75	1.2	0.2	6.9

* at ref	Stack Gas Weight	0 °C	Without correction for moisture
Conditions	29.00 Kg/kmol	101.3 kPa	Oxygen No Correction %

Where applicable Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report: * Reference conditions (see above) Nm³ 273 K, 101.3 kPa
 ** Analysis not required # - UKAS accredited only
 ND Non detectable ## - Not Accredited
 s - Subcontracted laboratory analysis N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated. Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Operating Information

The table below shows details of the operating information on each sampling date for: **LEV 2**

Date	Process type	Process duration	Fuel	Feedstock	Abatement	Load
28/01/2016	Production and cleaning of inkjet cartridges	Continuous	N/A	N/A	N/A	Normal

No CEMs installed on the emission point.

Comments & Monitoring Deviations

A waste gas homogeneity test to BS EN 15259:2007 (MID) is not required:-

The homogeneity test is not applicable to non-combustion processes.

The homogeneity test is not applicable to duct areas less than 1m².


All monitoring was performed in accordance with the relevant procedures.



Part 2: Supporting Information

Report for the Periodic Monitoring of Emissions to Air.

Client	Xaarjet Ltd
Site	Huntingdon
Plant	LEV 2
Sampling Date	28th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4
Report Approved by:	Sign		
	Print	Derek Myers	
	MCERTS No.	MM02 115	Level 2 TE: 1,2,3,4



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APPENDIX 1

Emission Monitoring Procedures And Instrumentation

Gas velocity and temperature

Documented in-house procedure TPM01/A to the main procedural requirements of BS EN ISO 16911-1:2013. Velocity and temperature measurements are performed using a calibrated Pitot tube, a calibrated pressure differential reading device and a calibrated thermocouple. Velocity and possible flow deviation measurements are carried out at selected, representative points in the gas stream.

Total organic carbon

Documented in-house procedure MM0002 to the main procedural requirements of BS EN 12619:2013. Continuous analysis using probe, sample line and multi range Flame Ionisation Detector (FID) analyser. The analyser is calibrated before and during the tests using certified gas mixtures of nitrogen, oxygen and propane. Sampling points are selected in accordance with the findings of any BS EN 15259 assessment.

Sampling Project Personnel Competency And Expiry Dates

		MCERTS No	Level 1	Level 2	TE1	TE2	TE3	TE4
Report prepared by:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Report authorised by:	Derek Myers	MM02 115	-	30/09/2017	31/05/2018	30/11/2018	30/11/2018	30/11/2018
Team leader:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Team leader:	Harpreet Badwal	MM03 149	-	30/09/2018	30/09/2018	30/04/2019	31/10/2019	31/10/2019

Equipment References

Equipment	Reference Number
FID	AQ271
Heated Line	HL40
Stack Thermocouple	PTTS97
Timer / Stopwatch	ST41
Barometer	WS03
Pitot	PT97
Thermometer	TK24
Manometer	PI03

APPENDIX 2

Date	28/01/2016
Time	11:20
Pitot Cp	0.79

Barometric pressure	101.6	kPa
Duct static pressure	0.14	kPa
Stack Area	0.073	m ²

Stack Diameter (circular)	0.31	m
---------------------------	------	---

Traverse	Traverse	Depth	ΔP	T	Angle	velocity	Traverse	Depth	ΔP	T	Angle	velocity
Point	Line	cm	mmH ₂ O	°C	°	m/s	Line	cm	mmH ₂ O	°C	°	m/s
1	A						B					
2	A						B					
3	A	5.0	1.3	23	<15	3.7	B	5.0	3.5	23	<15	6.0
4	A	5.4	2.1	23	<15	4.7	B	5.4	3.2	23	<15	5.7
5	A	7.6	2.9	23	<15	5.4	B	7.6	3.2	23	<15	5.7
6	A	10.9	3.7	23	<15	6.1	B	10.9	2.8	23	<15	5.3
7	A	19.6	4.8	23	<15	7.0	B	19.6	3.0	23	<15	5.5
8	A	22.9	5.4	23	<15	7.4	B	22.9	3.1	23	<15	5.6
9	A	25.1	6.6	23	<15	8.2	B	25.1	4.0	23	<15	6.4
10	A	25.5	6.6	23	<15	8.2	B	25.5	4.5	23	<15	6.8
11	A						B					
12	A						B					

Average Pitot DP	3.64	mmH ₂ O
Average Temperature	296.2	K
Average Velocity	6.1	m/s
Average volumetric flow rate	0.45	m ³ /s at stack conditions
Average volumetric flow rate	0.41	m ³ /s (wet STP)

Sampling plane requirements Re: BS EN 13284-1:2001 5.2

a	Angle of gas flow less than 15° with regard to duct axis	YES
b	No local negative flow	YES
c	Minimum pitot greater than 5Pa	YES
d	Ratio of highest to lowest local gas velocity less than 3:1	YES
	Minimum local gas velocity	3.7
	Maximum local gas velocity	8.2
	Ratio of highest to lowest local gas velocity	2.24

Preliminary Velocity Traverse Data

Date 28/01/2016

From 11:45 to 12:15 30 minute mean

Volatile organic compounds	vppm, wet	2.32	mg/m ³ *	3.74
----------------------------	-----------	------	---------------------	------

From 12:15 to 12:45 30 minute mean

Volatile organic compounds	vppm, wet	1.90	mg/m ³ *	3.05
----------------------------	-----------	------	---------------------	------

From 12:45 to 13:15 30 minute mean

Volatile organic compounds	vppm, wet	2.90	mg/m ³ *	4.65
----------------------------	-----------	------	---------------------	------

Sampling Detection Limits

Volatile organic compounds	vppm	0.10	mg/m ³ *	0.16
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Reference Gas Details

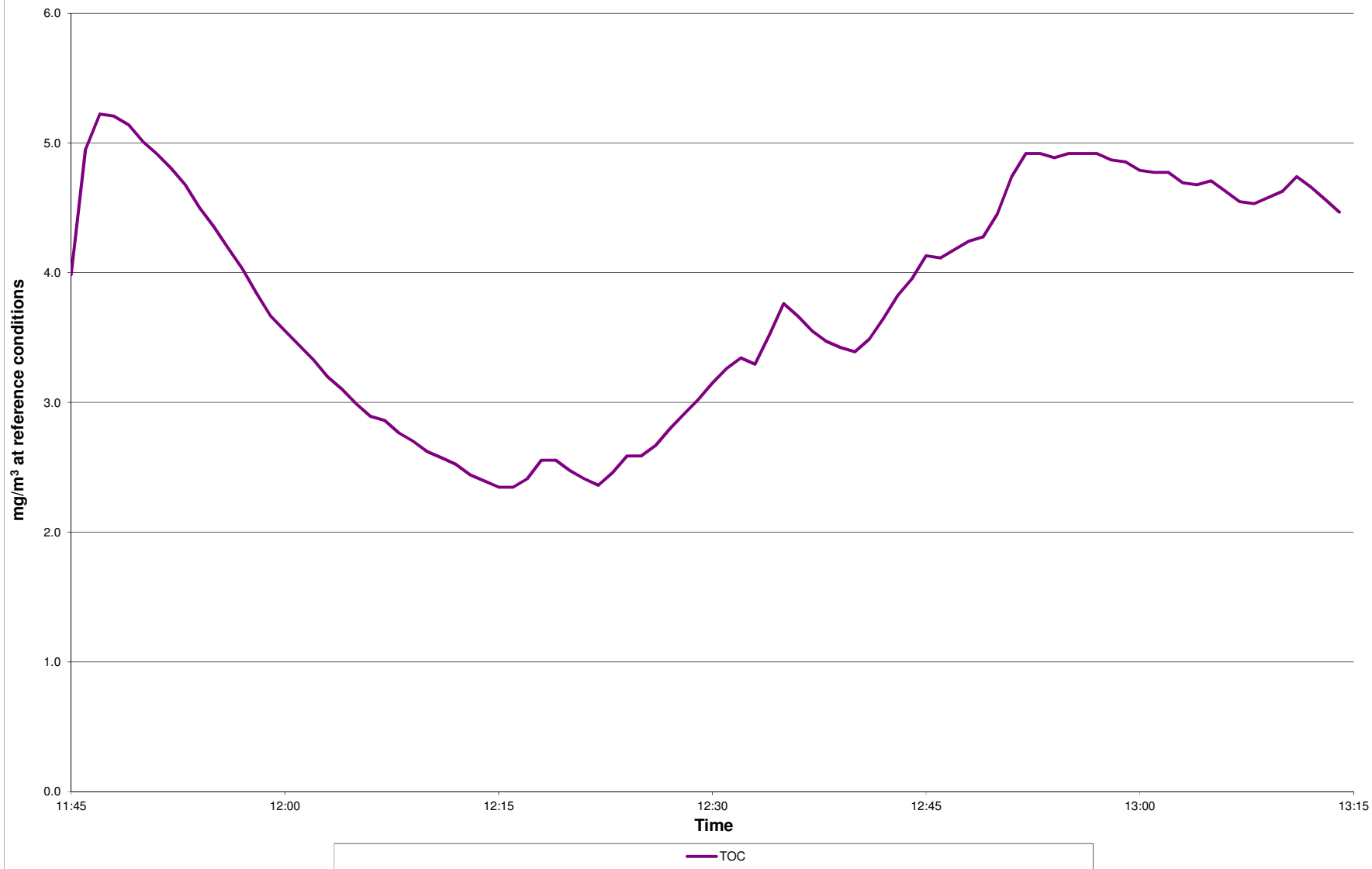
Species	Units	Value	Cylinder Reference	Analyser Range	Uncertainty <i>k</i> = 2
Nitrogen	%	99.999	VCK01959	-	± 2
Volatile organic compounds	vppm	75.5	VCSMG3066	10	± 2

Zero And Span Gas Details

Species	units	Initial Time	11:30	Final Time	16:00
		Initial Zero	Initial Span	Final Zero	Final Span
Volatile organic compounds	vppm	0.00	75.50	-0.04	75.63

Exhaust Gases - Continuous Analysis Data

Chart 1 - Exhaust Gases - Xaarjet Ltd, Huntingdon, LEV 2, 28/01/16



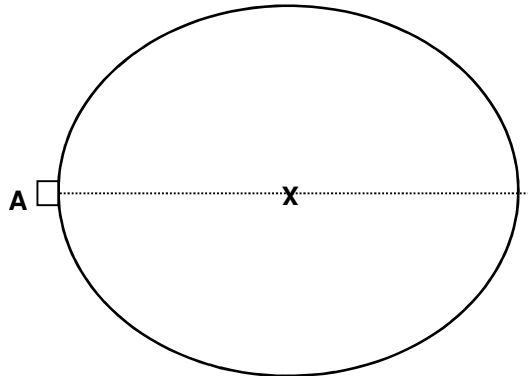
APPENDIX 3

Diagram Of The Sampling Location

Diagram of sampling points across the cross section of the duct (not to scale).

Traverse length = 0.31 m

Point	% of D	Location cm
1	50.0	15.3



General Calculations

Stack area:

$$\text{Area of a circle} = \frac{\pi \cdot D^2}{4}$$

D = Diameter (m)

π = 3.142

Pressure conversion:

1mmH₂O = 0.00980665 kPa

1mmH₂O = 9.80665 Pa

1 mar = 0.1 kPa

Water vapour concentration:

From reference calculations (taken from BS EN 14790):

$$V_{WC(\%)} = \frac{\frac{m_{WC} \cdot V_{mol(std)}}{M_w}}{\frac{m_{WC} \cdot V_{mol(std)}}{M_w} + V_{m(std)}} \times 100$$

WVC (%) = Water vapour content on wet basis, in volume % (m³ of water vapour in m³ of wet gas)

V_{m(std)} = Dry gas volume measured, corrected to standard conditions (m³)

m_{WC} = Mass of water collected in the impingers (g)

M_w = Molecular weight of water, 18.01534 rounded to 18 (g/mol)

V_{mol(std)} = Molar volume of water at standard conditions = 0.0224 (m³/mol)

Gas meter volume at standard conditions (STP)

From reference calculations (taken from BS EN 14790):

$$V_{m(std)} = y_d \times (V_2 - V_1) \times \frac{T_{std}}{T_m} \times \frac{p_m}{p_{std}}$$

V_{m(std)} = Dry gas meter volume at standard conditions (m³)

y_d = Gas meter calibration coefficient

(V₂-V₁) = Dry gas meter volume at actual conditions (m³)

T_m = Actual Temperature (K)

T_{std} = Standard temperature (273 K)

p_m = Absolute pressure at the gas meter (kPa)

p_{std} = Standard gas pressure (101.3 kPa)

Isokenetic Ratio (%):

From reference calculations (taken from EA TGN M2):

$$\text{IsokineticRatio}(\%) = \frac{\text{Velocity at the sampling nozzle}}{\text{Velocity of the stack gas}} \times 100$$

Estimating Measurement Uncertainty

Uncertainty estimates are calculated using the general rule of uncertainty propagation. Guidance is taken from publications including UKAS document M3003 and ISO 20988:2007.

Flow Calculations

Velocity:

From reference calculations (taken from ISO 10780):

$$\bar{v} = KC \sqrt{\frac{T_s \Delta p}{p_e M_s}}$$

\bar{v} = Average velocity (m/s)

C = velocity calculation constant = 129

T_s = Average stack temperature (K)

M_s = Molar mass of gas; assume 29 kg/kmol unless the molar mass is < 27 kg/kmol or > 31 g/kmol

K = Pitot calibration coefficient

p_e = Absolute gas pressure (kPa)

Δp = Average pitot tube pressure differential (kPa)

Volume flow rate

From reference calculations (taken from ISO 10780):

$$q_{va} = \bar{v} A$$

q_{va} = Average flow rate (m³/s)

\bar{v} = Average velocity (m/s)

A = Stack cross-sectional area (m²)

Volume flow rate corrected for moisture

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(100 - H_a)}{(100 - H_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

H_a = Moisture at actual conditions (%volume)

H_m = Reference moisture (%volume)

Volume flow rate corrected for temperature and pressure

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(T_m p_a)}{(T_a p_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

T_a = Temperature at actual conditions (K)

T_m = Reference Temperature (K)

p_a = Absolute gas pressure at actual conditions (kPa)

p_m = Reference pressure (kPa)

Volume flow rate corrected for oxygen

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(20.9 - O_{2,ref})}{(20.9 - O_{2,m})}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

$O_{2,m}$ = Actual oxygen concentration (%)

$O_{2,ref}$ = Reference oxygen concentration (%)

Concentration Calculations

Concentration:

From reference calculations (taken from BS EN 13284-1):

$$c = \frac{m}{V}$$

c = Concentration
 m = Mass of substance
 V = Volume sampled

Mass Emission

$$\text{Mass emission} = c \times q_m$$

c = Concentration
 q = Volume flow rate

Concentration corrected for oxygen:

From reference calculations (taken from BS ISO 9096):

$$c_m = c_a \times \frac{20.9 - O_{2,ref}}{20.9 - O_{2,a}}$$

c_m = Concentration at reference conditions
 c_a = Actual concentration
 $O_{2, ref}$ = Reference oxygen (%)
 $O_{2, a}$ = Actual Oxygen (%)

Concentration corrected for moisture:

From reference calculations (taken from BS ISO 9096):

Convert wet gas to dry gas

$$c_{dry} = c_{wet} \times \frac{100}{100 - H_a}$$

Convert dry gas to wet gas

$$c_{wet} = c_{dry} \times \frac{100 - H_a}{100}$$

c_{wet} = Concentration wet gas
 c_{dry} = Concentration dry gas
 H_a = Water vapour content (%vol)

Conversion of parts per million (ppm) to mg/m³

From reference calculations (taken from EA TGN M2):

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

When Converting TOC

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight of carbon in span gas}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

Calculation of Uncertainty Estimates - Instrumental Monitoring Techniques

Model equation

$$C_{ppm} = C_{reading} + Corr_{fit} + Corr_{0,dr} + Corr_{s,dr} + Corr_{rep} + Corr_{adj} + \sum_{i=1}^p Corr_{inf} + Corr_{int}$$

Where:

C_{ppm}	=	concentration in ppm	$Corr_{rep}$	=	correction of repeatability of measurement
$C_{NO,reading}$	=	concentration given by analyser	$Corr_{adj}$	=	correction of adjustment
$Corr_{fit}$	=	correction of lack of fit	$Corr_{inf}$	=	correction of influence quantities
$Corr_{0,dr}$	=	correction of zero drift	$Corr_{int}$	=	correction of interferences
$Corr_{s,dr}$	=	correction of span drift			

Calculation of partial uncertainties

$$u(Corr_{fit}) = \frac{\left(\frac{X_{fit,max}}{100 \times range} \right)}{\sqrt{3}} \quad \text{Where: } X_{fit,max} \text{ is the maximum allowable deviation from linearity}$$

Expressed as % of the range and calculated by applying a rectangular probability distribution

$$u(Corr_{0,dr}) = \frac{X_{0,dr}}{\sqrt{3}} \quad u(Corr_{s,dr}) = \frac{X_{s,dr}}{\sqrt{3}}$$

$$u(Corr_{rep}) = \max(S_{0,rep}; S_{s,rep}) = S_{rep} \quad \text{Where: } S_{r,0} \text{ is the standard uncertainty at zero level}$$

$$S_{r,s} \text{ is the standard uncertainty at span level}$$

$$u(Corr_{adj}) = u(Corr_{loss}) + u(Corr_{cal}) \quad \text{Where: } u(Corr_{loss}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{loss}) = \frac{C_{j,loss}}{\sqrt{3}} \quad u(Corr_{cal}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{cal}) = \frac{U_{cal}}{2} \quad c_{j,loss} \text{ is the concentration of sample loss at span level}$$

$$U_{cal} \text{ is the expanded uncertainty of the calibration gas}$$

$$u(Corr_{inf}) = c_j \sqrt{\frac{(x_{j,max} - x_{j,adj})^2 + (x_{j,min} - x_{j,adj})^2 + (x_{j,max} - x_{j,adj})(x_{j,min} - x_{j,adj})}{3}}$$

Where:

- c_j is the sensitivity coefficient of the influence quantity
- $x_{j,min}$ is the minimum value of the influence quantity during monitoring
- $x_{j,max}$ is the maximum value of the influence quantity during monitoring
- $x_{j,adj}$ is the value of the influence quantity during adjustment

$$u(Corr_{int}) = \frac{c_j}{Int_{j,test}} \sqrt{\frac{Int_{j,max}^2 + Int_{j,min} \times Int_{j,max} + Int_{j,min}^2}{3}}$$

and

$$u(\Sigma Corr_{int}) = \max[S_{Int,p}; S_{Int,n}] \quad \text{Where: } c_j \text{ is the sensitivity coefficient of the interferent j}$$

- $Int_{j,test}$ is the concentration of the interferent j used to determine c_j
- $Int_{j,min}$ is the minimum value of the interferent j quantity during monitoring
- $Int_{j,max}$ is the maximum value of the interferent j quantity during monitoring
- $Int_{j,adj}$ is the concentration of the interferent j in the cal gas used to adjust the analyser
- $S_{Int,p}$ is the sum of interferences with positive impact
- $S_{Int,n}$ is the sum of interferences with negative impact

Combined uncertainty

$$u(C_{ppm}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2}$$

$$\text{Overall expanded uncertainty (k = 2)} \quad U(C_m) = u(C_m) \times k$$

Uncertainty of NOx measurements

$$u(C_{NOx,conv}) = \frac{C_{NOx} \times R \times \eta}{\sqrt{3}} \quad \text{Where: } C_{NOx} \text{ is the concentration of NOx measured by the analyser}$$

- R is the ratio of NO:Nox in the stack gas
- η is the NOx converter efficiency

Combined uncertainty NOx measurements

$$u(C_{NOx,stack}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + u^2(Corr_{NOx,conv})}$$

Uncertainty of mass concentration at oxygen reference concentration

$$u(C_{O_2,ref}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + \left(\frac{u^2(O_{2,meas,dry})}{(21 - O_{2,meas,dry})^2} \right)}$$

Where:

$u(C_{O_2,ref})$	=	uncertainty associated with the mass concentration at O ₂ ref. concentration	in	mg/m ³
$C_{O_2,ref}$	=	mass concentration at O ₂ reference concentration	in	mg/m ³
$O_{2,meas}$	=	O ₂ measured concentration	in	% volume
$u((O_{2,meas})_{dry})$	=	uncertainty associated to the measured O ₂ concentration	in	% (relative to O ₂ meas)

APPENDIX 4

Uncertainty Estimate For The Measurement Of Total Organic Carbon

Analysers Type/Model
Reference Oxygen %

Sick Maihak
0 (0 = No correction)

		Test 1	Test 2	Test 3
Limit value	mg/m ³	75	75	75
Limit value	ppm	46.7	46.7	46.7
Measured concentration	ppm	2.3	1.9	2.9
Measured concentration	mg/m ³	3.7	3.1	4.7

Calibration gas	ppm	75.5	75.5	75.5
Calibration gas	mg/m ³	121.3	121.3	121.3
Analysers range	ppm	9.3	9.3	9.3
Analysers range	mg/m ³	15.0	15.0	15.0

Correction of Lack of Fit				
Lack of fit	% range	2.0	2.0	2.0
	u(Corr _{fit})	0.11	0.11	0.11

Corrections of Zero and Span Drift (*All drift is calculated for ∴ the residual is assumed to be < 5% u(max))				
Zero Drift	% range	0.00	0.00	0.00
	u(Corr _{zero})	0.00	0.00	0.00
Span Drift	% range	0.00	0.00	0.00
	u(Corr _{span})	0.00	0.00	0.00

Correction of Repeatability of Measurement				
Repeatability SD at span level (Not reported)	% range	0.0	0.0	0.0
	u(Corr _{rep})	0.00	0.00	0.00

Correction of adjustment				
losses in the line	% range	0.13	0.13	0.13
	u(Corr _{loss})	0.00	0.00	0.00
Uncertainty of calibration gas	% range	2.0	2.0	2.0
	u(Corr _{cal})	0.02	0.02	0.03

Correction of Influence of Interferents				
N ₂ O	% range			
	u(Corr _{N2O})	0.00	0.00	0.00
CO ₂	% range			
	u(Corr _{CO2})	0.00	0.00	0.00
CH ₄	% range			
	u(Corr _{CH4})	0.00	0.00	0.00
Total of interferent influences $u(\Sigma Corr_{int}) = \max[S_{int,1}; S_{int,2}]$	% range	2.50	2.50	2.50
	u(ΣCorr _{int})	0.16	0.16	0.16

Correction of Influence Quantities				
Sensitivity to sample volume flow	% range	1.60	1.60	1.60
	u(Corr _{vol})	0.09	0.09	0.09
Sensitivity to atmospheric pressure (Not reported)	% range			
	u(Corr _{press})	0.00	0.00	0.00
Sensitivity to ambient temperature	% range	-2.40	-2.40	-2.40
	u(Corr _{temp})	-0.28	-0.28	-0.28
Sensitivity to electrical voltage (Not reported)	% range	0.50	0.50	0.50
	u(Corr _{volt})	0.10	0.10	0.10

Maximum standard uncertainty	u(Corr _{max})	0.11	0.11	0.11
5% of maximum standard uncertainty	u(Corr _{5%})	0.01	0.01	0.01

Interferent Concentration Variations	Minimum	Maximum	Value at cal	Performance	Units
CH ₄ range	0	10	0	50	mg/m ³
N ₂ O range	0	0	0	20	mg/m ³
CO ₂ range	8	12	0	15	mg/m ³
Oxygen effect variations	Minimum	Maximum	Value at cal	Performance	Units
Oxygen effect	0	20	0	2	mg/m ³

Influence Quantity Variations	Minimum	Maximum	Value at cal	Performance	Units
Sensitivity to sample volume flow	55	65	60	5	l/h
Sensitivity to atmospheric pressure	99	100	99	1	kPa
Sensitivity to ambient temperature	278	313	288	10	K
Sensitivity to electrical voltage	187	250	230	5	V

Measurement uncertainty				
Combined uncertainty	ppm	0.37	0.37	0.37
Combined uncertainty	mg/m ³	0.59	0.59	0.59

Expanded uncertainty expressed with a level of confidence of 95%, k=2

Overall uncertainty	ppm	0.7	0.7	0.7
Overall uncertainty	mg/m ³	1.2	1.2	1.2
Overall uncertainty relative to measured value	%	31.5	38.4	25.3
Overall uncertainty relative to range	%	7.8	7.8	7.8
Overall uncertainty relative to ELV	%	1.0	1.0	1.0

The uncertainty evaluation has been carried out in accordance with UKAS requirements.



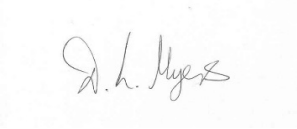
Client Xaarjet Ltd
1 Hurricane Close
Ermine Business Park
Huntingdon
Cambridgeshire
PE29 6XX

Part 1: Executive Summary

Report for the Periodic Monitoring of Emissions to Air.

Site	Huntingdon
Plant	LEV 9
Sampling Date	28th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4

Report Approved by:	Sign		
	Print	Derek Myers	
	MCERTS No.	MM02 115	Level 2 TE: 1,2,3,4



1783

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Company Registration No SC070429

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Monitoring Objectives

The monitoring was undertaken to check compliance with authorised emission limits.

All monitoring procedures were carried out to the MCERTS requirements under the Exova (UK) Ltd quality system to ISO 17025: 2005.

Monitoring was undertaken for the listed emissions from the following sampling positions:

Sampling Location	Emission
LEV 9	Total volatile organic carbon

Special Monitoring Requirements

There were no special requirements for this monitoring campaign.

Summary of Methods

Emission	Method number	Method standard
Gas velocity and volume flow TOC	TPM/01A MM0002	BS EN ISO 16911-1:2013 BS EN 12619 : 2013

Summary Of Results

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 9	Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
	Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	28/01/16	12:13	13:43	14.4	75	1.2	0.2	36.5

* at reference conditions	Stack Gas Weight 29.00 Kg/kmol	0 °C 101.3 kPa	Without correction for moisture Oxygen No Correction %
---------------------------	-----------------------------------	-------------------	---

Where applicable

Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report:

* Reference conditions (see above)
** Analysis not required
ND Non detectable
s - Subcontracted laboratory analysis

Nm³ 273 K, 101.3 kPa
- UKAS accredited only
- Not Accredited
N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated.
Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Summary Of Results, Exhaust Gases

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 9		Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
		Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	Test 1	28/01/16	12:13	12:43	18.4	75	1.3	0.2	46.6
TOC	Test 2	28/01/16	12:43	13:13	15.4	75	1.2	0.2	39.2
TOC	Test 3	28/01/16	13:13	13:43	9.4	75	1.2	0.2	23.9

* at ref	Stack Gas Weight	0 °C	Without correction for moisture
Conditions	29.00 Kg/kmol	101.3 kPa	Oxygen No Correction %

Where applicable Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report: * Reference conditions (see above) Nm³ 273 K, 101.3 kPa
 ** Analysis not required # - UKAS accredited only
 ND Non detectable ## - Not Accredited
 s - Subcontracted laboratory analysis N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated. Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Operating Information

The table below shows details of the operating information on each sampling date for: **LEV 9**

Date	Process type	Process duration	Fuel	Feedstock	Abatement	Load
28/01/2016	Production and cleaning of inkjet cartridges	Continuous	N/A	N/A	N/A	Normal

No CEMs installed on the emission point.

Comments & Monitoring Deviations

A waste gas homogeneity test to BS EN 15259:2007 (MID) is not required:-

The homogeneity test is not applicable to non-combustion processes.

The homogeneity test is not applicable to duct areas less than 1m².

The homogeneity test is not usually applicable to pollutant emissions that are less than 30% of the ELV.

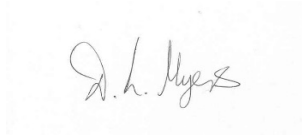
All monitoring was performed in accordance with the relevant procedures.



Part 2: Supporting Information

Report for the Periodic Monitoring of Emissions to Air.

Client	Xaarjet Ltd
Site	Huntingdon
Plant	LEV 9
Sampling Date	28th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4
Report Approved by:	Sign		
	Print	Derek Myers	
	MCERTS No.	MM02 115	Level 2 TE: 1,2,3,4



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APPENDIX 1

Emission Monitoring Procedures And Instrumentation

Gas velocity and temperature

Documented in-house procedure TPM01/A to the main procedural requirements of BS EN ISO 16911-1:2013
Velocity and temperature measurements are performed using a calibrated Pitot tube, a calibrated pressure differential reading device and a calibrated thermocouple. Velocity and possible flow deviation measurements are carried out at selected, representative points in the gas stream.

Total organic carbon

Documented in-house procedure MM0002 to the main procedural requirements of BS EN 12619:2013.
Continuous analysis using probe, sample line and multi range Flame Ionisation Detector (FID) analyser. The analyser is calibrated before and during the tests using certified gas mixtures of nitrogen, oxygen and propane. Sampling points are selected in accordance with the findings of any BS EN 15259 assessment.

Sampling Project Personnel Competency And Expiry Dates

		MCERTS No	Level 1	Level 2	TE1	TE2	TE3	TE4
Report prepared by:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Report authorised by:	Derek Myers	MM02 115	-	30/09/2017	31/05/2018	30/11/2018	30/11/2018	30/11/2018
Team leader:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Team leader:	Harpreet Badwal	MM03 149	-	30/09/2018	30/09/2018	30/04/2019	31/10/2019	31/10/2019

Equipment References

Equipment	Reference Number
FID	AQ270
Heated Line	HL33
Stack Thermocouple	PTTS97
Timer / Stopwatch	ST41
Barometer	WS03
Pitot	PT97
Thermometer	TK24
Manometer	PI03

APPENDIX 2

Date	28/01/2016
Time	11:20
Pitot Cp	0.79

Barometric pressure	101.6	kPa
Duct static pressure	0.33	kPa
Stack Area	0.071	m ²

Stack Diameter (circular)	0.30	m
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Traverse Point	Traverse Line	Depth cm	ΔP mmH ₂ O	T °C	Angle °	velocity m/s	Traverse Line	Depth cm	ΔP mmH ₂ O	T °C	Angle °	velocity m/s
1	A						B					
2	A						B					
3	A	5.0	11.2	24	<15	10.7	B	5.0	10.7	24	<15	10.5
4	A	5.3	11.9	24	<15	11.1	B	5.3	11.2	24	<15	10.7
5	A	7.5	11.9	24	<15	11.0	B	7.5	11.4	24	<15	10.8
6	A	10.7	12.0	24	<15	11.1	B	10.7	11.9	24	<15	11.1
7	A	19.3	12.8	24	<15	11.5	B	19.3	11.3	24	<15	10.8
8	A	22.5	12.2	24	<15	11.2	B	22.5	11.1	24	<15	10.7
9	A	24.7	10.6	24	<15	10.4	B	24.7	10.7	24	<15	10.5
10	A	25.0	10.4	24	<15	10.3	B	25.0	10.3	24	<15	10.3
11	A						B					
12	A						B					

Average Pitot DP	11.35	mmH ₂ O
Average Temperature	297.2	K
Average Velocity	10.8	m/s
Average volumetric flow rate	0.76	m ³ /s at stack conditions
Average volumetric flow rate	0.70	m ³ /s (wet STP)

Sampling plane requirements Re: BS EN 13284-1:2001 5.2

a	Angle of gas flow less than 15° with regard to duct axis	YES
b	No local negative flow	YES
c	Minimum pitot greater than 5Pa	YES
d	Ratio of highest to lowest local gas velocity less than 3:1	YES
	Minimum local gas velocity	10.3
	Maximum local gas velocity	11.5
	Ratio of highest to lowest local gas velocity	1.12

Preliminary Velocity Traverse Data

Date 28/01/2016

From 12:13 to 12:43 30 minute mean

Volatile organic compounds	vppm, wet	11.43	mg/m ³ *	18.37
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From 12:43 to 13:13 30 minute mean

Volatile organic compounds	vppm, wet	9.60	mg/m ³ *	15.43
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From 13:13 to 13:43 30 minute mean

Volatile organic compounds	vppm, wet	5.85	mg/m ³ *	9.40
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Sampling Detection Limits

Volatile organic compounds	vppm	0.10	mg/m ³ *	0.16
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Reference Gas Details

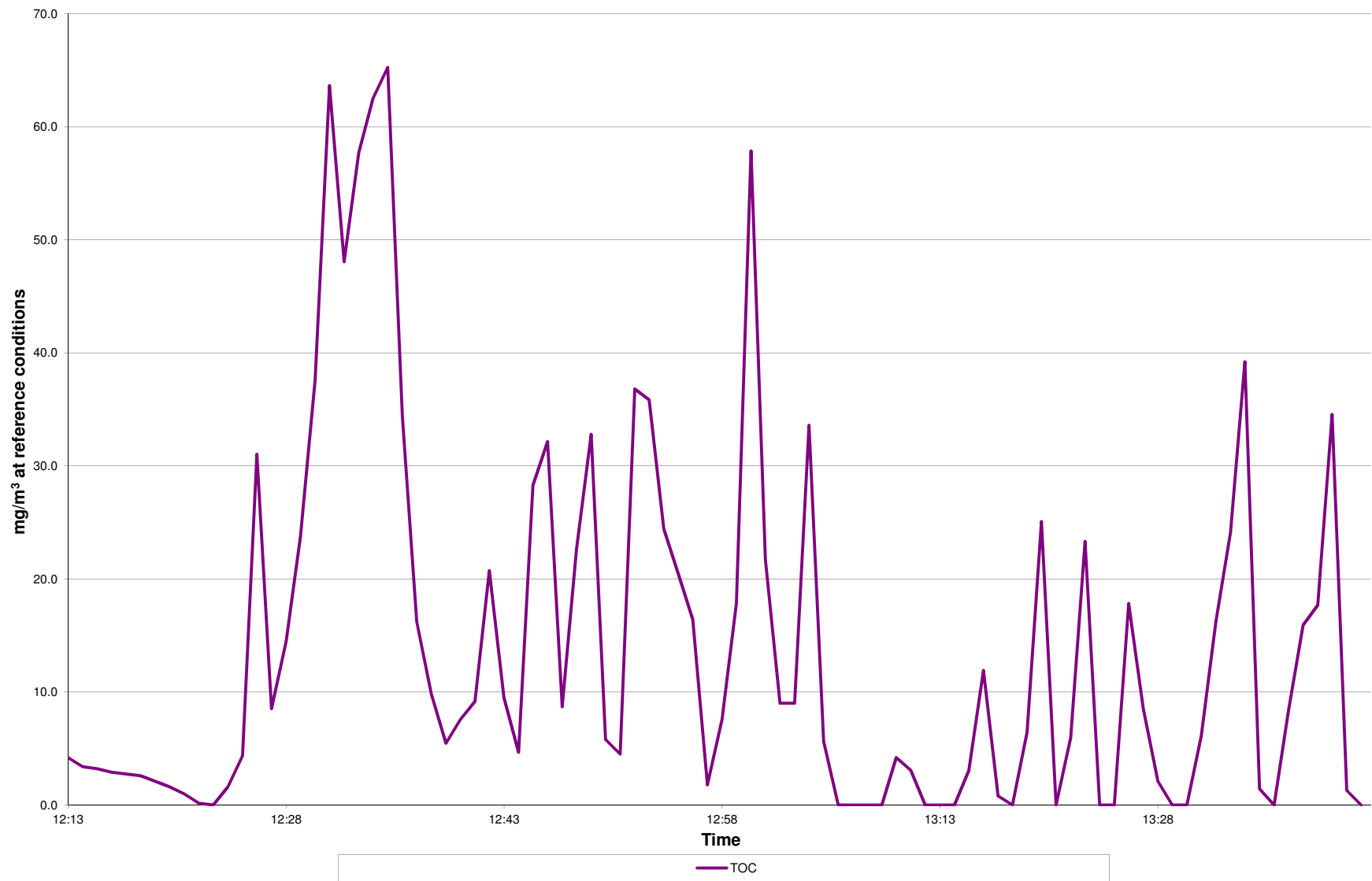
Species	Units	Value	Cylinder Reference	Analyser Range	Uncertainty <i>k</i> = 2
Nitrogen	%	99.999	VC80548	-	± 2
Volatile organic compounds	vppm	76.6	VCD500681	100	± 2

Zero And Span Gas Details

Species	units	Initial Time	11:40	Final Time	17:26
		Initial Zero	Initial Span	Final Zero	Final Span
Volatile organic compounds	vppm	0.0	76.6	-0.8	75.6

Exhaust Gases - Continuous Analysis Data

Chart 1 - Exhaust Gases - Xaarjet Ltd, Huntingdon, LEV 9, 28/01/16



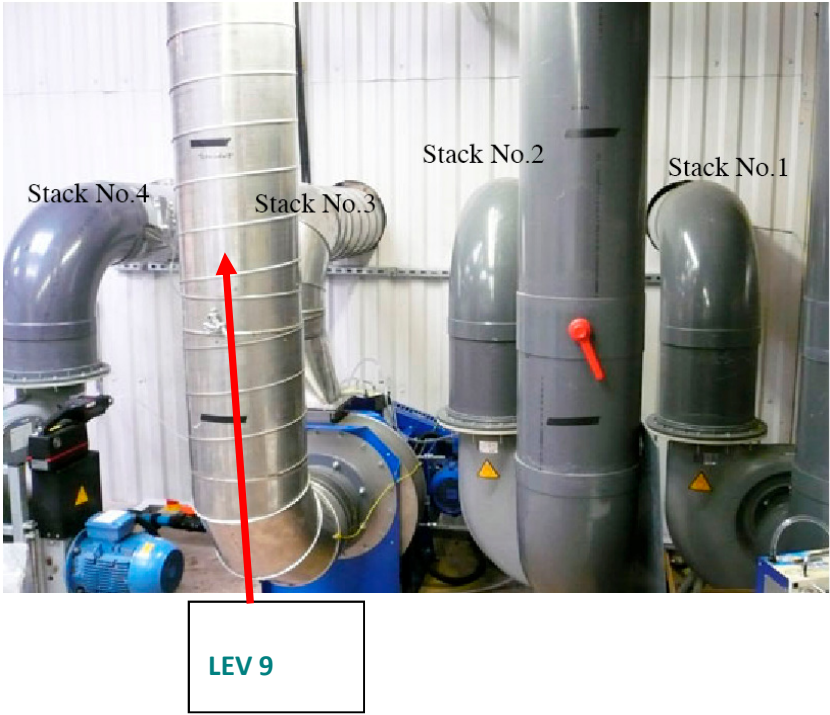
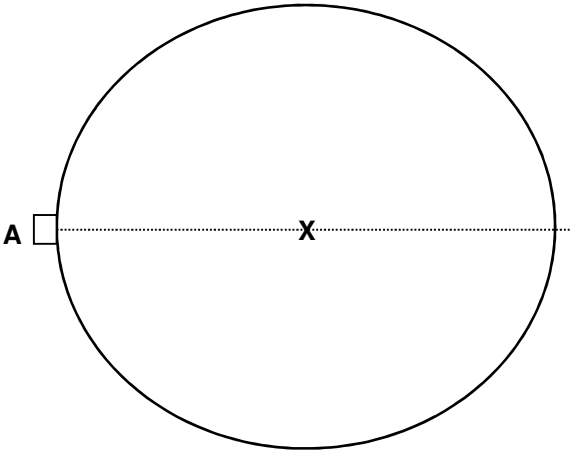
APPENDIX 3

Diagram Of The Sampling Location

Diagram of sampling points across the cross section of the duct (not to scale).

Traverse length = 0.30 m

Point	% of D	Location cm
1	50.0	15.0



General Calculations

Stack area:

$$\text{Area of a circle} = \frac{\pi \cdot D^2}{4}$$

D = Diameter (m)

π = 3.142

Pressure conversion:

1mmH₂O = 0.00980665 kPa

1mmH₂O = 9.80665 Pa

1 mar = 0.1 kPa

Water vapour concentration:

From reference calculations (taken from BS EN 14790):

$$V_{WC(\%)} = \frac{\frac{m_{WC} \cdot V_{mol(std)}}{M_w}}{\frac{m_{WC} \cdot V_{mol(std)}}{M_w} + V_{m(std)}} \times 100$$

WVC (%) = Water vapour content on wet basis, in volume % (m³ of water vapour in m³ of wet gas)

V_{m(std)} = Dry gas volume measured, corrected to standard conditions (m³)

m_{WC} = Mass of water collected in the impingers (g)

M_w = Molecular weight of water, 18.01534 rounded to 18 (g/mol)

V_{mol(std)} = Molar volume of water at standard conditions = 0.0224 (m³/mol)

Gas meter volume at standard conditions (STP)

From reference calculations (taken from BS EN 14790):

$$V_{m(std)} = y_d \times (V_2 - V_1) \times \frac{T_{std}}{T_m} \times \frac{p_m}{p_{std}}$$

V_{m(std)} = Dry gas meter volume at standard conditions (m³)

y_d = Gas meter calibration coefficient

(V₂-V₁) = Dry gas meter volume at actual conditions (m³)

T_m = Actual Temperature (K)

T_{std} = Standard temperature (273 K)

p_m = Absolute pressure at the gas meter (kPa)

p_{std} = Standard gas pressure (101.3 kPa)

Isokenetic Ratio (%):

From reference calculations (taken from EA TGN M2):

$$\text{IsokineticRatio}(\%) = \frac{\text{Velocity at the sampling nozzle}}{\text{Velocity of the stack gas}} \times 100$$

Estimating Measurement Uncertainty

Uncertainty estimates are calculated using the general rule of uncertainty propagation. Guidance is taken from publications including UKAS document M3003 and ISO 20988:2007.

Flow Calculations

Velocity:

From reference calculations (taken from ISO 10780):

$$\bar{v} = KC \sqrt{\frac{T_s \Delta p}{p_e M_s}}$$

\bar{v} = Average velocity (m/s)

C = velocity calculation constant = 129

T_s = Average stack temperature (K)

M_s = Molar mass of gas; assume 29 kg/kmol unless the molar mass is < 27 kg/kmol or > 31 g/kmol

K = Pitot calibration coefficient

p_e = Absolute gas pressure (kPa)

Δp = Average pitot tube pressure differential (kPa)

Volume flow rate

From reference calculations (taken from ISO 10780):

$$q_{va} = \bar{v} A$$

q_{va} = Average flow rate (m³/s)

\bar{v} = Average velocity (m/s)

A = Stack cross-sectional area (m²)

Volume flow rate corrected for moisture

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(100 - H_a)}{(100 - H_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

H_a = Moisture at actual conditions (%volume)

H_m = Reference moisture (%volume)

Volume flow rate corrected for temperature and pressure

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(T_m p_a)}{(T_a p_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

T_a = Temperature at actual conditions (K)

T_m = Reference Temperature (K)

p_a = Absolute gas pressure at actual conditions (kPa)

p_m = Reference pressure (kPa)

Volume flow rate corrected for oxygen

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(20.9 - O_{2,ref})}{(20.9 - O_{2,m})}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

$O_{2,m}$ = Actual oxygen concentration (%)

$O_{2,ref}$ = Reference oxygen concentration (%)

Concentration Calculations

Concentration:

From reference calculations (taken from BS EN 13284-1):

$$c = \frac{m}{V}$$

c = Concentration
 m = Mass of substance
 V = Volume sampled

Mass Emission

$$\text{Mass emission} = c \times q_m$$

c = Concentration
 q = Volume flow rate

Concentration corrected for oxygen:

From reference calculations (taken from BS ISO 9096):

$$c_m = c_a \times \frac{20.9 - O_{2,ref}}{20.9 - O_{2,a}}$$

c_m = Concentration at reference conditions
 c_a = Actual concentration
 $O_{2, ref}$ = Reference oxygen (%)
 $O_{2, a}$ = Actual Oxygen (%)

Concentration corrected for moisture:

From reference calculations (taken from BS ISO 9096):

Convert wet gas to dry gas

$$c_{dry} = c_{wet} \times \frac{100}{100 - H_a}$$

Convert dry gas to wet gas

$$c_{wet} = c_{dry} \times \frac{100 - H_a}{100}$$

c_{wet} = Concentration wet gas
 c_{dry} = Concentration dry gas
 H_a = Water vapour content (%vol)

Conversion of parts per million (ppm) to mg/m³

From reference calculations (taken from EA TGN M2):

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

When Converting TOC

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight of carbon in span gas}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

Calculation of Uncertainty Estimates - Instrumental Monitoring Techniques

Model equation

$$C_{ppm} = C_{reading} + Corr_{fit} + Corr_{0,dr} + Corr_{s,dr} + Corr_{rep} + Corr_{adj} + \sum_{i=1}^p Corr_{inf} + Corr_{int}$$

Where:

C_{ppm}	=	concentration in ppm	$Corr_{rep}$	=	correction of repeatability of measurement
$C_{NO,reading}$	=	concentration given by analyser	$Corr_{adj}$	=	correction of adjustment
$Corr_{fit}$	=	correction of lack of fit	$Corr_{inf}$	=	correction of influence quantities
$Corr_{0,dr}$	=	correction of zero drift	$Corr_{int}$	=	correction of interferences
$Corr_{s,dr}$	=	correction of span drift			

Calculation of partial uncertainties

$$u(Corr_{fit}) = \frac{\left(\frac{X_{fit,max}}{100 \times range} \right)}{\sqrt{3}} \quad \text{Where: } X_{fit,max} \text{ is the maximum allowable deviation from linearity}$$

Expressed as % of the range and calculated by applying a rectangular probability distribution

$$u(Corr_{0,dr}) = \frac{X_{0,dr}}{\sqrt{3}} \quad u(Corr_{s,dr}) = \frac{X_{s,dr}}{\sqrt{3}}$$

$$u(Corr_{rep}) = \max(S_{0,rep}; S_{s,rep}) = S_{rep} \quad \text{Where: } S_{r,0} \text{ is the standard uncertainty at zero level}$$

$$S_{r,s} \text{ is the standard uncertainty at span level}$$

$$u(Corr_{adj}) = u(Corr_{loss}) + u(Corr_{cal}) \quad \text{Where: } u(Corr_{loss}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{loss}) = \frac{C_{j,loss}}{\sqrt{3}} \quad u(Corr_{cal}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{cal}) = \frac{U_{cal}}{2} \quad c_{j,loss} \text{ is the concentration of sample loss at span level}$$

$$U_{cal} \text{ is the expanded uncertainty of the calibration gas}$$

$$u(Corr_{inf}) = c_j \sqrt{\frac{(x_{j,max} - x_{j,adj})^2 + (x_{j,min} - x_{j,adj})^2 + (x_{j,max} - x_{j,adj})(x_{j,min} - x_{j,adj})}{3}}$$

Where:

- c_j is the sensitivity coefficient of the influence quantity
- $x_{j,min}$ is the minimum value of the influence quantity during monitoring
- $x_{j,max}$ is the maximum value of the influence quantity during monitoring
- $x_{j,adj}$ is the value of the influence quantity during adjustment

$$u(Corr_{int}) = \frac{c_j}{Int_{j,test}} \sqrt{\frac{Int_{j,max}^2 + Int_{j,min} \times Int_{j,max} + Int_{j,min}^2}{3}}$$

and

$$u(\Sigma Corr_{int}) = \max[S_{Int,p}; S_{Int,n}] \quad \text{Where: } c_j \text{ is the sensitivity coefficient of the interferent j}$$

- $Int_{j,test}$ is the concentration of the interferent j used to determine c_j
- $Int_{j,min}$ is the minimum value of the interferent j quantity during monitoring
- $Int_{j,max}$ is the maximum value of the interferent j quantity during monitoring
- $Int_{j,adj}$ is the concentration of the interferent j in the cal gas used to adjust the analyser
- $S_{Int,p}$ is the sum of interferences with positive impact
- $S_{Int,n}$ is the sum of interferences with negative impact

Combined uncertainty

$$u(C_{ppm}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2}$$

$$\text{Overall expanded uncertainty (k = 2)} \quad U(C_m) = u(C_m) \times k$$

Uncertainty of NOx measurements

$$u(C_{NOx,conv}) = \frac{C_{NOx} \times R \times \eta}{\sqrt{3}} \quad \text{Where: } C_{NOx} \text{ is the concentration of NOx measured by the analyser}$$

- R is the ratio of NO:Nox in the stack gas
- η is the NOx converter efficiency

Combined uncertainty NOx measurements

$$u(C_{NOx,stack}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + u^2(Corr_{NOx,conv})}$$

Uncertainty of mass concentration at oxygen reference concentration

$$u(C_{O_2,ref}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + \left(\frac{u^2(O_{2,meas,dry})}{(21 - O_{2,meas,dry})^2} \right)}$$

Where:

$u(C_{O_2,ref})$	=	uncertainty associated with the mass concentration at O ₂ ref. concentration	in	mg/m ³
$C_{O_2,ref}$	=	mass concentration at O ₂ reference concentration	in	mg/m ³
$O_{2,meas}$	=	O ₂ measured concentration	in	% volume
$u((O_{2,meas})_{dry})$	=	uncertainty associated to the measured O ₂ concentration	in	% (relative to O ₂ meas)

APPENDIX 4

Uncertainty Estimate For The Measurement Of Total Organic Carbon

Analysers Type/Model
Reference Oxygen %

Sick Maihak
0 (0 = No correction)

		Test 1	Test 2	Test 3
Limit value	mg/m ³	75	75	75
Limit value	ppm	46.7	46.7	46.7
Measured concentration	ppm	11.4	9.6	5.9
Measured concentration	mg/m ³	18.4	15.4	9.4

Calibration gas	ppm	76.6	76.6	76.6
Calibration gas	mg/m ³	123.1	123.1	123.1
Analysers range	ppm	9.3	9.3	9.3
Analysers range	mg/m ³	15.0	15.0	15.0

Correction of Lack of Fit				
Lack of fit	% range	2.0	2.0	2.0
	u(Corr _{fit})	0.11	0.11	0.11

Corrections of Zero and Span Drift (*All drift is calculated for ∴ the residual is assumed to be < 5% u(max))				
Zero Drift	% range	0.00	0.00	0.00
	u(Corr _{zero})	0.00	0.00	0.00
Span Drift	% range	0.00	0.00	0.00
	u(Corr _{span})	0.00	0.00	0.00

Correction of Repeatability of Measurement				
Repeatability SD at span level (Not reported)	% range	0.0	0.0	0.0
	u(Corr _{rep})	0.00	0.00	0.00

Correction of adjustment				
losses in the line	% range	1.31	1.31	1.31
	u(Corr _{loss})	0.09	0.07	0.04
Uncertainty of calibration gas	% range	2.0	2.0	2.0
	u(Corr _{cal})	0.11	0.10	0.06

Correction of Influence of Interferents				
N ₂ O	% range			
	u(Corr _{N2O})	0.00	0.00	0.00
CO ₂	% range			
	u(Corr _{CO2})	0.00	0.00	0.00
CH ₄	% range			
	u(Corr _{CH4})	0.00	0.00	0.00
Total of interferent influences $u(\Sigma Corr_{int}) = \max[S_{int,1}; S_{int,n}]$	% range	2.50	2.50	2.50
	u(ΣCorr _{int})	0.16	0.16	0.16

Correction of Influence Quantities				
Sensitivity to sample volume flow	% range	1.60	1.60	1.60
	u(Corr _{vol})	0.09	0.09	0.09
Sensitivity to atmospheric pressure (Not reported)	% range			
	u(Corr _{press})	0.00	0.00	0.00
Sensitivity to ambient temperature	% range	-2.40	-2.40	-2.40
	u(Corr _{temp})	-0.28	-0.28	-0.28
Sensitivity to electrical voltage (Not reported)	% range	0.50	0.50	0.50
	u(Corr _{volt})	0.10	0.10	0.10

Maximum standard uncertainty	u(Corr _{max})	0.11	0.11	0.11
5% of maximum standard uncertainty	u(Corr _{5%})	0.01	0.01	0.01

Interferent Concentration Variations	Minimum	Maximum	Value at cal	Performance	Units
CH ₄ range	0	10	0	50	mg/m ³
N ₂ O range	0	0	0	20	mg/m ³
CO ₂ range	8	12	0	15	mg/m ³
Oxygen effect variations	Minimum	Maximum	Value at cal	Performance	Units
Oxygen effect	0	20	0	2	mg/m ³

Influence Quantity Variations	Minimum	Maximum	Value at cal	Performance	Units
Sensitivity to sample volume flow	55	65	60	5	l/h
Sensitivity to atmospheric pressure	99	100	99	1	kPa
Sensitivity to ambient temperature	278	313	288	10	K
Sensitivity to electrical voltage	187	250	230	5	V

Measurement uncertainty				
Combined uncertainty	ppm	0.39	0.38	0.37
Combined uncertainty	mg/m ³	0.63	0.62	0.60

Expanded uncertainty expressed with a level of confidence of 95%, k=2

Overall uncertainty	ppm	0.8	0.8	0.7
Overall uncertainty	mg/m ³	1.3	1.2	1.2
Overall uncertainty relative to measured value	%	6.9	8.0	12.7
Overall uncertainty relative to range	%	8.4	8.2	8.0
Overall uncertainty relative to ELV	%	1.0	1.0	1.0

The uncertainty evaluation has been carried out in accordance with UKAS requirements.




Client Xaarjet Ltd
1 Hurricane Close
Ermine Business Park
Huntingdon
Cambridgeshire
PE29 6XX

Part 1: Executive Summary

Report for the Periodic Monitoring of Emissions to Air.

Site	Huntingdon
Plant	LEV 13
Sampling Date	28th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4

Report Approved by:	Sign		
	Print	Derek Myers	
	MCERTS No.	MM02 115	Level 2 TE: 1,2,3,4



1783

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Company Registration No SC070429

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Monitoring Objectives

The monitoring was undertaken to check compliance with authorised emission limits.

All monitoring procedures were carried out to the MCERTS requirements under the Exova (UK) Ltd quality system to ISO 17025: 2005.

Monitoring was undertaken for the listed emissions from the following sampling positions:

Sampling Location	Emission
LEV 13	Total volatile organic carbon

Special Monitoring Requirements

There were no special requirements for this monitoring campaign.

Summary of Methods

Emission	Method number	Method standard
Gas velocity and volume flow TOC	TPM/01A MM0002	BS EN ISO 16911-1:2013 BS EN 12619 : 2013

Summary Of Results

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 13	Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
	Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	28/01/16	15:53	17:23	9.1	75	1.2	0.2	166.3

* at reference conditions	Stack Gas Weight 29.00 Kg/kmol	0 °C 101.3 kPa	Without correction for moisture Oxygen No Correction %
---------------------------	-----------------------------------	-------------------	---

Where applicable

Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report:

* Reference conditions (see above)
** Analysis not required
ND Non detectable
s - Subcontracted laboratory analysis

Nm³ 273 K, 101.3 kPa
- UKAS accredited only
- Not Accredited
N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated.
Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Summary Of Results, Exhaust Gases

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 13		Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
		Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	Test 1	28/01/16	15:53	16:23	8.0	75	1.2	0.2	145.6
TOC	Test 2	28/01/16	16:23	16:53	9.5	75	1.2	0.2	173.6
TOC	Test 3	28/01/16	16:53	17:23	9.8	75	1.2	0.2	179.7

* at ref	Stack Gas Weight	0 °C	Without correction for moisture
Conditions	29.00 Kg/kmol	101.3 kPa	Oxygen No Correction %

Where applicable Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report: * Reference conditions (see above) Nm³ 273 K, 101.3 kPa
 ** Analysis not required # - UKAS accredited only
 ND Non detectable ## - Not Accredited
 s - Subcontracted laboratory analysis N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated. Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Operating Information

The table below shows details of the operating information on each sampling date for: **LEV 13**

Date	Process type	Process duration	Fuel	Feedstock	Abatement	Load
28/01/2016	Production and cleaning of inkjet cartridges	Continuous	N/A	N/A	N/A	Normal

No CEMs installed on the emission point.

Comments & Monitoring Deviations

A waste gas homogeneity test to BS EN 15259:2007 (MID) is not required:-

The homogeneity test is not applicable to non-combustion processes.

The homogeneity test is not applicable to duct areas less than 1m².

The homogeneity test is not usually applicable to pollutant emissions that are less than 30% of the ELV.

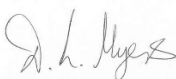
All monitoring was performed in accordance with the relevant procedures.



Part 2: Supporting Information

Report for the Periodic Monitoring of Emissions to Air.

Client	Xaarjet Ltd
Site	Huntingdon
Plant	LEV 13
Sampling Date	28th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4
Report Approved by:	Sign		
	Print	Derek Myers	
	MCERTS No.	MM02 115	Level 2 TE: 1,2,3,4



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APPENDIX 1

Emission Monitoring Procedures And Instrumentation

Gas velocity and temperature

Documented in-house procedure TPM01/A to the main procedural requirements of BS EN ISO 16911-1:2013
Velocity and temperature measurements are performed using a calibrated Pitot tube, a calibrated pressure differential reading device and a calibrated thermocouple. Velocity and possible flow deviation measurements are carried out at selected, representative points in the gas stream.

Total organic carbon

Documented in-house procedure MM0002 to the main procedural requirements of BS EN 12619:2013.
Continuous analysis using probe, sample line and multi range Flame Ionisation Detector (FID) analyser. The analyser is calibrated before and during the tests using certified gas mixtures of nitrogen, oxygen and propane. Sampling points are selected in accordance with the findings of any BS EN 15259 assessment.

Sampling Project Personnel Competency And Expiry Dates

		MCERTS No	Level 1	Level 2	TE1	TE2	TE3	TE4
Report prepared by:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Report authorised by:	Derek Myers	MM02 115	-	30/09/2017	31/05/2018	30/11/2018	30/11/2018	30/11/2018
Team leader:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Team leader:	Harpreet Badwal	MM03 149	-	30/09/2018	30/09/2018	30/04/2019	31/10/2019	31/10/2019

Equipment References

Equipment	Reference Number
FID	AQ270
Heated Line	HL33
Stack Thermocouple	PTTS97
Timer / Stopwatch	ST41
Barometer	WS03
Pitot	PT97
Thermometer	TK24
Manometer	PI03

APPENDIX 2

Date	28/01/2016
Time	10:30
Pitot Cp	0.79

Barometric pressure	101.6	kPa
Duct static pressure	0.20	kPa
Stack Area	0.785	m ²

Stack Diameter (circular)	1.00	m
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Traverse	Traverse	Depth	ΔP	T	Angle	velocity	Traverse	Depth	ΔP	T	Angle	velocity
Point	Line	cm	mmH ₂ O	°C	°	m/s	Line	cm	mmH ₂ O	°C	°	m/s
1	A	5.0	2.9	25	<15	5.4	B					
2	A	6.7	3.8	25	<15	6.2	B					
3	A	11.8	3.4	25	<15	5.9	B					
4	A	17.7	4.3	25	<15	6.6	B					
5	A	25.0	5.5	25	<15	7.5	B					
6	A	35.6	5.1	25	<15	7.2	B					
7	A	64.4	6.1	25	<15	7.9	B					
8	A	75.0	5.9	25	<15	7.8	B					
9	A	82.3	5.8	25	<15	7.7	B					
10	A	88.2	5.4	25	<15	7.5	B					
11	A	93.3	5.1	25	<15	7.2	B					
12	A	95.0	5.0	25	<15	7.2	B					

Average Pitot DP	4.79	mmH ₂ O
Average Temperature	297.7	K
Average Velocity	7.0	m/s
Average volumetric flow rate	5.51	m ³ /s at stack conditions
Average volumetric flow rate	5.08	m ³ /s (wet STP)

Sampling plane requirements Re: BS EN 13284-1:2001 5.2

a	Angle of gas flow less than 15° with regard to duct axis	YES
b	No local negative flow	YES
c	Minimum pitot greater than 5Pa	YES
d	Ratio of highest to lowest local gas velocity less than 3:1	YES
	Minimum local gas velocity	5.4
	Maximum local gas velocity	7.9
	Ratio of highest to lowest local gas velocity	1.46

Preliminary Velocity Traverse Data

Date 28/01/2016

From 15:53 to 16:23 30 minute mean

Volatile organic compounds	vppm, wet	4.95	mg/m ³ *	7.96
----------------------------	-----------	------	---------------------	------

From 16:23 to 16:53 30 minute mean

Volatile organic compounds	vppm, wet	5.90	mg/m ³ *	9.49
----------------------------	-----------	------	---------------------	------

From 16:53 to 17:23 30 minute mean

Volatile organic compounds	vppm, wet	6.11	mg/m ³ *	9.82
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Sampling Detection Limits

Volatile organic compounds	vppm	0.10	mg/m ³ *	0.16
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Reference Gas Details

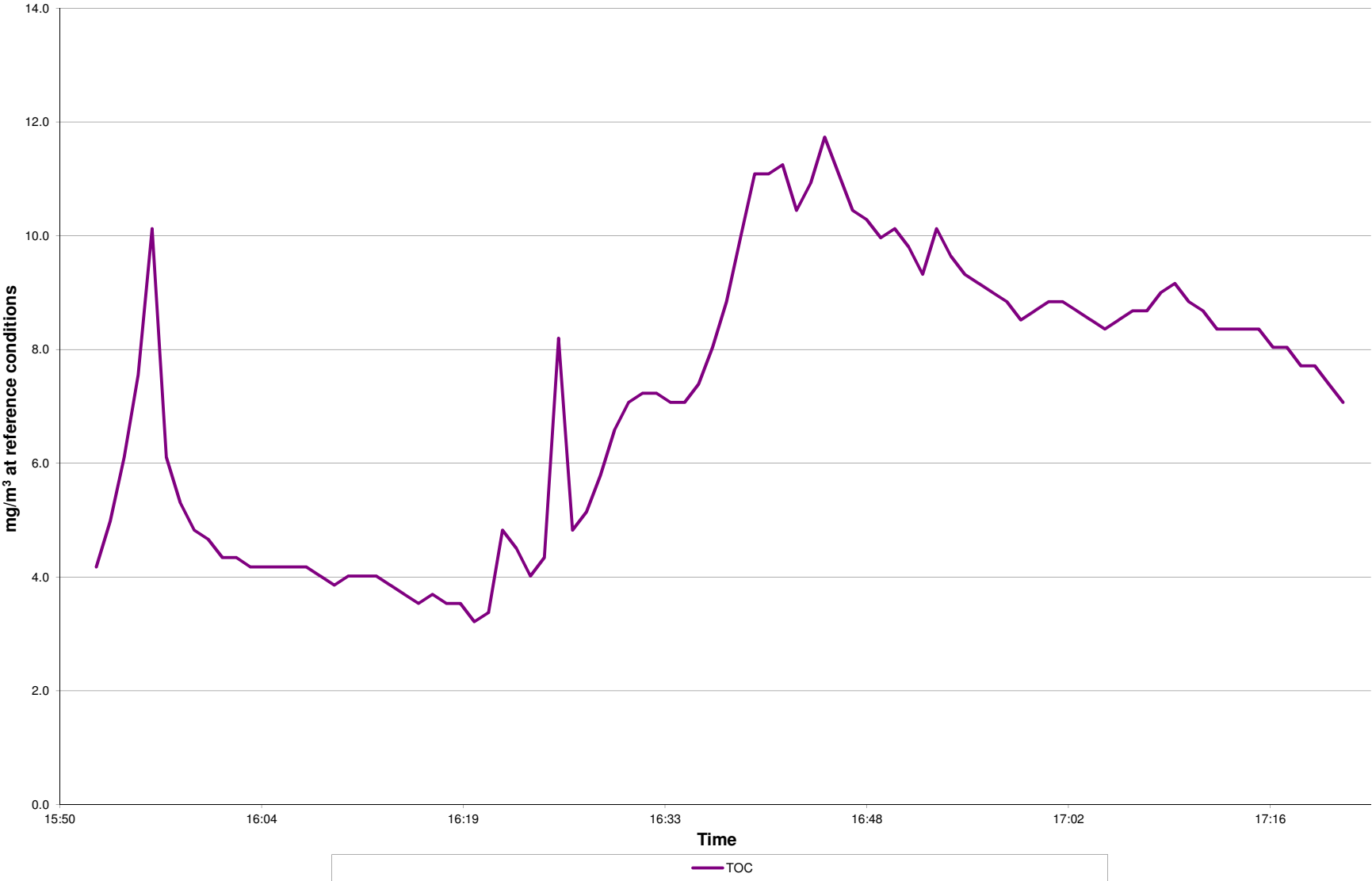
Species	Units	Value	Cylinder Reference	Analyser Range	Uncertainty <i>k</i> = 2
Nitrogen	%	99.999	VC80548	-	± 2
Volatile organic compounds	vppm	76.6	VCD500681	100	± 2

Zero And Span Gas Details

Species	units	Initial Time	11:40	Final Time	17:26
		Initial Zero	Initial Span	Final Zero	Final Span
Volatile organic compounds	vppm	0.0	76.6	-0.8	75.6

Exhaust Gases - Continuous Analysis Data

Chart 1 - Exhaust Gases - Xaarjet Ltd, Huntingdon, LEV 13, 28/01/16



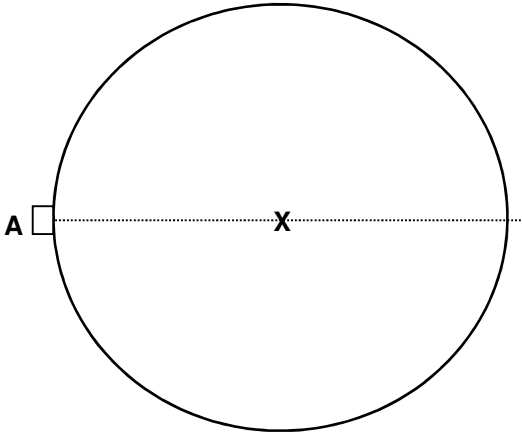
APPENDIX 3

Diagram Of The Sampling Location

Diagram of sampling points across the cross section of the duct (not to scale).

Traverse length = 1.00 m

Point	% of D	Location cm
1	50.0	50.0



LEV 13 – Room
extract

General Calculations

Stack area:

$$\text{Area of a circle} = \frac{\pi \cdot D^2}{4}$$

D = Diameter (m)

π = 3.142

Pressure conversion:

1mmH₂O = 0.00980665 kPa

1mmH₂O = 9.80665 Pa

1 mar = 0.1 kPa

Water vapour concentration:

From reference calculations (taken from BS EN 14790):

$$V_{WC(\%)} = \frac{\frac{m_{WC} \cdot V_{mol(std)}}{M_w}}{\frac{m_{WC} \cdot V_{mol(std)}}{M_w} + V_{m(std)}} \times 100$$

WVC (%) = Water vapour content on wet basis, in volume % (m³ of water vapour in m³ of wet gas)

V_{m(std)} = Dry gas volume measured, corrected to standard conditions (m³)

m_{WC} = Mass of water collected in the impingers (g)

M_w = Molecular weight of water, 18.01534 rounded to 18 (g/mol)

V_{mol(std)} = Molar volume of water at standard conditions = 0.0224 (m³/mol)

Gas meter volume at standard conditions (STP)

From reference calculations (taken from BS EN 14790):

$$V_{m(std)} = y_d \times (V_2 - V_1) \times \frac{T_{std}}{T_m} \times \frac{p_m}{p_{std}}$$

V_{m(std)} = Dry gas meter volume at standard conditions (m³)

y_d = Gas meter calibration coefficient

(V₂-V₁) = Dry gas meter volume at actual conditions (m³)

T_m = Actual Temperature (K)

T_{std} = Standard temperature (273 K)

p_m = Absolute pressure at the gas meter (kPa)

p_{std} = Standard gas pressure (101.3 kPa)

Isokenetic Ratio (%):

From reference calculations (taken from EA TGN M2):

$$\text{IsokineticRatio}(\%) = \frac{\text{Velocity at the sampling nozzle}}{\text{Velocity of the stack gas}} \times 100$$

Estimating Measurement Uncertainty

Uncertainty estimates are calculated using the general rule of uncertainty propagation. Guidance is taken from publications including UKAS document M3003 and ISO 20988:2007.

Flow Calculations

Velocity:

From reference calculations (taken from ISO 10780):

$$\bar{v} = KC \sqrt{\frac{T_s \Delta p}{p_e M_s}}$$

\bar{v} = Average velocity (m/s)

C = velocity calculation constant = 129

T_s = Average stack temperature (K)

M_s = Molar mass of gas; assume 29 kg/kmol unless the molar mass is < 27 kg/kmol or > 31 g/kmol

K = Pitot calibration coefficient

p_e = Absolute gas pressure (kPa)

Δp = Average pitot tube pressure differential (kPa)

Volume flow rate

From reference calculations (taken from ISO 10780):

$$q_{va} = \bar{v}A$$

q_{va} = Average flow rate (m³/s)

\bar{v} = Average velocity (m/s)

A = Stack cross-sectional area (m²)

Volume flow rate corrected for moisture

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(100 - H_a)}{(100 - H_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

H_a = Moisture at actual conditions (%volume)

H_m = Reference moisture (%volume)

Volume flow rate corrected for temperature and pressure

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(T_m p_a)}{(T_a p_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

T_a = Temperature at actual conditions (K)

T_m = Reference Temperature (K)

p_a = Absolute gas pressure at actual conditions (kPa)

p_m = Reference pressure (kPa)

Volume flow rate corrected for oxygen

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(20.9 - O_{2,ref})}{(20.9 - O_{2,m})}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

$O_{2,m}$ = Actual oxygen concentration (%)

$O_{2,ref}$ = Reference oxygen concentration (%)

Concentration Calculations

Concentration:

From reference calculations (taken from BS EN 13284-1):

$$c = \frac{m}{V}$$

c = Concentration
 m = Mass of substance
 V = Volume sampled

Mass Emission

$$\text{Mass emission} = c \times q_m$$

c = Concentration
 q = Volume flow rate

Concentration corrected for oxygen:

From reference calculations (taken from BS ISO 9096):

$$c_m = c_a \times \frac{20.9 - O_{2,ref}}{20.9 - O_{2,a}}$$

c_m = Concentration at reference conditions
 c_a = Actual concentration
 $O_{2,ref}$ = Reference oxygen (%)
 $O_{2,a}$ = Actual Oxygen (%)

Concentration corrected for moisture:

From reference calculations (taken from BS ISO 9096):

Convert wet gas to dry gas

$$c_{dry} = c_{wet} \times \frac{100}{100 - H_a}$$

Convert dry gas to wet gas

$$c_{wet} = c_{dry} \times \frac{100 - H_a}{100}$$

c_{wet} = Concentration wet gas
 c_{dry} = Concentration dry gas
 H_a = Water vapour content (%vol)

Conversion of parts per million (ppm) to mg/m³

From reference calculations (taken from EA TGN M2):

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

When Converting TOC

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight of carbon in span gas}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

Calculation of Uncertainty Estimates - Instrumental Monitoring Techniques

Model equation

$$C_{ppm} = C_{reading} + Corr_{fit} + Corr_{0,dr} + Corr_{s,dr} + Corr_{rep} + Corr_{adj} + \sum_{i=1}^p Corr_{inf} + Corr_{int}$$

Where:

C_{ppm}	=	concentration in ppm	$Corr_{rep}$	=	correction of repeatability of measurement
$C_{NO,reading}$	=	concentration given by analyser	$Corr_{adj}$	=	correction of adjustment
$Corr_{fit}$	=	correction of lack of fit	$Corr_{inf}$	=	correction of influence quantities
$Corr_{0,dr}$	=	correction of zero drift	$Corr_{int}$	=	correction of interferences
$Corr_{s,dr}$	=	correction of span drift			

Calculation of partial uncertainties

$$u(Corr_{fit}) = \frac{\left(\frac{X_{fit,max}}{100 \times range} \right)}{\sqrt{3}} \quad \text{Where: } X_{fit,max} \text{ is the maximum allowable deviation from linearity}$$

Expressed as % of the range and calculated by applying a rectangular probability distribution

$$u(Corr_{0,dr}) = \frac{X_{0,dr}}{\sqrt{3}} \quad u(Corr_{s,dr}) = \frac{X_{s,dr}}{\sqrt{3}}$$

$$u(Corr_{rep}) = \max(S_{0,rep}; S_{s,rep}) = S_{rep} \quad \text{Where: } S_{r,0} \text{ is the standard uncertainty at zero level}$$

$$S_{r,s} \text{ is the standard uncertainty at span level}$$

$$u(Corr_{adj}) = u(Corr_{loss}) + u(Corr_{cal}) \quad \text{Where: } u(Corr_{loss}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{loss}) = \frac{C_{j,loss}}{\sqrt{3}} \quad u(Corr_{cal}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{cal}) = \frac{U_{cal}}{2} \quad c_{j,loss} \text{ is the concentration of sample loss at span level}$$

$$U_{cal} \text{ is the expanded uncertainty of the calibration gas}$$

$$u(Corr_{inf}) = c_j \sqrt{\frac{(x_{j,max} - x_{j,adj})^2 + (x_{j,min} - x_{j,adj})^2 + (x_{j,max} - x_{j,adj})(x_{j,min} - x_{j,adj})}{3}}$$

Where:

- c_j is the sensitivity coefficient of the influence quantity
- $x_{j,min}$ is the minimum value of the influence quantity during monitoring
- $x_{j,max}$ is the maximum value of the influence quantity during monitoring
- $x_{j,adj}$ is the value of the influence quantity during adjustment

$$u(Corr_{int}) = \frac{c_j}{Int_{j,test}} \sqrt{\frac{Int_{j,max}^2 + Int_{j,min} \times Int_{j,max} + Int_{j,min}^2}{3}}$$

and

$$u(\Sigma Corr_{int}) = \max[S_{Int,p}; S_{Int,n}] \quad \text{Where: } c_j \text{ is the sensitivity coefficient of the interferent j}$$

- $Int_{j,test}$ is the concentration of the interferent j used to determine c_j
- $Int_{j,min}$ is the minimum value of the interferent j quantity during monitoring
- $Int_{j,max}$ is the maximum value of the interferent j quantity during monitoring
- $Int_{j,adj}$ is the concentration of the interferent j in the cal gas used to adjust the analyser
- $S_{Int,p}$ is the sum of interferences with positive impact
- $S_{Int,n}$ is the sum of interferences with negative impact

Combined uncertainty

$$u(C_{ppm}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2}$$

$$\text{Overall expanded uncertainty (k = 2)} \quad U(C_m) = u(C_m) \times k$$

Uncertainty of NOx measurements

$$u(C_{NOx,conv}) = \frac{C_{NOx} \times R \times \eta}{\sqrt{3}} \quad \text{Where: } C_{NOx} \text{ is the concentration of NOx measured by the analyser}$$

- R is the ratio of NO:Nox in the stack gas
- η is the NOx converter efficiency

Combined uncertainty NOx measurements

$$u(C_{NOx,stack}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + u^2(Corr_{NOx,conv})}$$

Uncertainty of mass concentration at oxygen reference concentration

$$u(C_{O_2,ref}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + \left(\frac{u^2(O_{2,meas,dry})}{(21 - O_{2,meas,dry})^2} \right)}$$

Where:

$u(C_{O_2,ref})$	=	uncertainty associated with the mass concentration at O ₂ ref. concentration	in	mg/m ³
$C_{O_2,ref}$	=	mass concentration at O ₂ reference concentration	in	mg/m ³
$O_{2,meas}$	=	O ₂ measured concentration	in	% volume
$u((O_{2,meas})_{dry})$	=	uncertainty associated to the measured O ₂ concentration	in	% (relative to O ₂ meas)

APPENDIX 4

Uncertainty Estimate For The Measurement Of Total Organic Carbon

Analysers Type/Model
Reference Oxygen %

Sick Maihak
0 (0 = No correction)

		Test 1	Test 2	Test 3
Limit value	mg/m ³	75	75	75
Limit value	ppm	46.7	46.7	46.7
Measured concentration	ppm	5.0	5.9	6.1
Measured concentration	mg/m ³	8.0	9.5	9.8

Calibration gas	ppm	76.6	76.6	76.6
Calibration gas	mg/m ³	123.1	123.1	123.1
Analysers range	ppm	9.3	9.3	9.3
Analysers range	mg/m ³	15.0	15.0	15.0

Correction of Lack of Fit				
Lack of fit	% range	2.0	2.0	2.0
	u(Corr _{fit})	0.11	0.11	0.11

Corrections of Zero and Span Drift (*All drift is calculated for ∴ the residual is assumed to be < 5% u(max))				
Zero Drift	% range	0.00	0.00	0.00
	u(Corr _{zdr})	0.00	0.00	0.00
Span Drift	% range	0.00	0.00	0.00
	u(Corr _{spd})	0.00	0.00	0.00

Correction of Repeatability of Measurement				
Repeatability SD at span level (Not reported)	% range	0.0	0.0	0.0
	u(Corr _{rep})	0.00	0.00	0.00

Correction of adjustment				
losses in the line	% range	1.31	1.31	1.31
	u(Corr _{loss})	0.04	0.04	0.05
Uncertainty of calibration gas	% range	2.0	2.0	2.0
	u(Corr _{cal})	0.05	0.06	0.06

Correction of Influence of Interferents				
N ₂ O	% range			
	u(Corr _{N2O})	0.00	0.00	0.00
CO ₂	% range			
	u(Corr _{CO2})	0.00	0.00	0.00
CH ₄	% range			
	u(Corr _{CH4})	0.00	0.00	0.00
Total of interferent influences $u(\Sigma Corr_{int}) = \max[S_{int,1}, S_{int,2}]$	% range	2.50	2.50	2.50
	u(ΣCorr _{int})	0.16	0.16	0.16

Correction of Influence Quantities				
Sensitivity to sample volume flow	% range	1.60	1.60	1.60
	u(Corr _{vol})	0.09	0.09	0.09
Sensitivity to atmospheric pressure (Not reported)	% range			
	u(Corr _{press})	0.00	0.00	0.00
Sensitivity to ambient temperature	% range	-2.40	-2.40	-2.40
	u(Corr _{temp})	-0.28	-0.28	-0.28
Sensitivity to electrical voltage (Not reported)	% range	0.50	0.50	0.50
	u(Corr _{volt})	0.10	0.10	0.10

Maximum standard uncertainty	u(Corr _{max})	0.11	0.11	0.11
5% of maximum standard uncertainty	u(Corr _{5%})	0.01	0.01	0.01

Interferent Concentration Variations	Minimum	Maximum	Value at cal	Performance	Units
CH ₄ range	0	10	0	50	mg/m ³
N ₂ O range	0	0	0	20	mg/m ³
CO ₂ range	8	12	0	15	mg/m ³
Oxygen effect variations	Minimum	Maximum	Value at cal	Performance	Units
Oxygen effect	0	20	0	2	mg/m ³

Influence Quantity Variations	Minimum	Maximum	Value at cal	Performance	Units
Sensitivity to sample volume flow	55	65	60	5	l/h
Sensitivity to atmospheric pressure	99	100	99	1	kPa
Sensitivity to ambient temperature	278	313	288	10	K
Sensitivity to electrical voltage	187	250	230	5	V

Measurement uncertainty		Test 1	Test 2	Test 3
Combined uncertainty	ppm	0.37	0.37	0.37
Combined uncertainty	mg/m ³	0.59	0.60	0.60

Expanded uncertainty expressed with a level of confidence of 95%, k=2				
Overall uncertainty	ppm	0.7	0.7	0.7
Overall uncertainty	mg/m ³	1.2	1.2	1.2
Overall uncertainty relative to measured value	%	14.9	12.6	12.2
Overall uncertainty relative to range	%	7.9	8.0	8.0
Overall uncertainty relative to ELV	%	1.0	1.0	1.0

The uncertainty evaluation has been carried out in accordance with UKAS requirements.



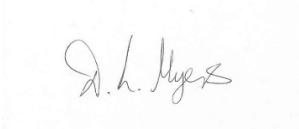
Client Xaarjet Ltd
1 Hurricane Close
Ermine Business Park
Huntingdon
Cambridgeshire
PE29 6XX

Part 1: Executive Summary

Report for the Periodic Monitoring of Emissions to Air.

Site	Huntingdon
Plant	LEV 14
Sampling Date	29th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4

Report Approved by:	Sign		
	Print	Derek Myers	
	MCERTS No.	MM02 115	Level 2 TE: 1,2,3,4



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Company Registration No SC070429

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Monitoring Objectives

The monitoring was undertaken to check compliance with authorised emission limits.

All monitoring procedures were carried out to the MCERTS requirements under the Exova (UK) Ltd quality system to ISO 17025: 2005.

Monitoring was undertaken for the listed emissions from the following sampling positions:

Sampling Location	Emission
LEV 14	Total volatile organic carbon

Special Monitoring Requirements

There were no special requirements for this monitoring campaign.

Summary of Methods

Emission	Method number	Method standard
Gas velocity and volume flow TOC	TPM/01A MM0002	BS EN ISO 16911-1:2013 BS EN 12619 : 2013

Summary Of Results

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 14	Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
	Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	29/01/16	09:45	11:15	9.1	75	1.2	0.2	16.4

* at reference conditions	Stack Gas Weight 29.00 Kg/kmol	0 °C 101.3 kPa	Without correction for moisture Oxygen No Correction %
---------------------------	-----------------------------------	-------------------	---

Where applicable

Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report:

* Reference conditions (see above)
** Analysis not required
ND Non detectable
s - Subcontracted laboratory analysis

Nm³ 273 K, 101.3 kPa
- UKAS accredited only
- Not Accredited
N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated.
Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Summary Of Results, Exhaust Gases

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 14		Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
		Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	Test 1	29/01/16	09:45	10:15	9.2	75	1.2	0.2	16.5
TOC	Test 2	29/01/16	10:15	10:45	8.1	75	1.2	0.2	14.6
TOC	Test 3	29/01/16	10:45	11:15	10.0	75	1.2	0.2	18.1

* at ref	Stack Gas Weight	0 °C	Without correction for moisture
Conditions	29.00 Kg/kmol	101.3 kPa	Oxygen No Correction %

Where applicable Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report: * Reference conditions (see above) Nm³ 273 K, 101.3 kPa
 ** Analysis not required # - UKAS accredited only
 ND Non detectable ## - Not Accredited
 s - Subcontracted laboratory analysis N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated. Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Operating Information

The table below shows details of the operating information on each sampling date for: **LEV 14**

Date	Process type	Process duration	Fuel	Feedstock	Abatement	Load
29/01/2016	Production and cleaning of inkjet cartridges	Continuous	N/A	N/A	N/A	Normal

No CEMs installed on the emission point.

Comments & Monitoring Deviations

A waste gas homogeneity test to BS EN 15259:2007 (MID) is not required:-

The homogeneity test is not applicable to non-combustion processes.

The homogeneity test is not applicable to duct areas less than 1m².

The homogeneity test is not usually applicable to pollutant emissions that are less than 30% of the ELV.

All monitoring was performed in accordance with the relevant procedures.



Part 2: Supporting Information

Report for the Periodic Monitoring of Emissions to Air.

Client	Xaarjet Ltd
Site	Huntingdon
Plant	LEV 14
Sampling Date	29th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by: **Print** Rob Jones

MCERTS No. MM08 984 **Level 2 TE: 1,2,3,4**

Report Approved by: **Sign**

Print Derek Myers

MCERTS No. MM02 115 **Level 2 TE: 1,2,3,4**



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APPENDIX 1

Emission Monitoring Procedures And Instrumentation

Gas velocity and temperature

Documented in-house procedure TPM01/A to the main procedural requirements of BS EN ISO 16911-1:2013
Velocity and temperature measurements are performed using a calibrated Pitot tube, a calibrated pressure differential reading device and a calibrated thermocouple. Velocity and possible flow deviation measurements are carried out at selected, representative points in the gas stream.

Total organic carbon

Documented in-house procedure MM0002 to the main procedural requirements of BS EN 12619:2013.
Continuous analysis using probe, sample line and multi range Flame Ionisation Detector (FID) analyser. The analyser is calibrated before and during the tests using certified gas mixtures of nitrogen, oxygen and propane. Sampling points are selected in accordance with the findings of any BS EN 15259 assessment.

Sampling Project Personnel Competency And Expiry Dates

		MCERTS No	Level 1	Level 2	TE1	TE2	TE3	TE4
Report prepared by:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Report authorised by:	Derek Myers	MM02 115	-	30/09/2017	31/05/2018	30/11/2018	30/11/2018	30/11/2018
Team leader:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Team leader:	Harpreet Badwal	MM03 149	-	30/09/2018	30/09/2018	30/04/2019	31/10/2019	31/10/2019

Equipment References

Equipment	Reference Number
FID	AQ271
Heated Line	HL40
Stack Thermocouple	PTTS97
Timer / Stopwatch	ST41
Barometer	WS03
Pitot	PT97
Thermometer	TK24
Manometer	PI03

APPENDIX 2

Date	29/01/2016
Time	09:08
Pitot Cp	0.79

Barometric pressure	101.6	kPa
Duct static pressure	0.04	kPa
Stack Area	0.159	m ²

Stack Diameter (circular)	0.45	m
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Traverse Point	Traverse Line	Depth cm	ΔP mmH ₂ O	T °C	Angle °	velocity m/s	Traverse Line	Depth cm	ΔP mmH ₂ O	T °C	Angle °	velocity m/s
1	A						B					
2	A	5.0	1.8	26	<15	4.4	B	5.0	2.4	26	<15	5.0
3	A	5.3	1.0	26	<15	3.2	B	5.3	1.9	26	<15	4.5
4	A	8.0	0.8	26	<15	2.9	B	8.0	1.5	26	<15	4.0
5	A	11.3	0.7	26	<15	2.7	B	11.3	1.7	26	<15	4.2
6	A	16.0	0.8	26	<15	2.9	B	16.0	1.1	26	<15	3.4
7	A	29.0	0.8	26	<15	2.9	B	29.0	0.8	26	<15	2.9
8	A	33.8	0.9	26	<15	3.1	B	33.8	0.6	26	<15	2.5
9	A	37.0	1.5	26	<15	4.0	B	37.0	0.6	26	<15	2.5
10	A	39.7	1.6	26	<15	4.1	B	39.7	0.8	26	<15	2.9
11	A	40.0	1.0	26	<15	3.2	B	40.0	1.2	26	<15	3.6
12	A						B					

Average Pitot DP	1.15	mmH ₂ O
Average Temperature	299.2	K
Average Velocity	3.4	m/s
Average volumetric flow rate	0.55	m ³ /s at stack conditions
Average volumetric flow rate	0.50	m ³ /s (wet STP)

Sampling plane requirements Re: BS EN 13284-1:2001 5.2

a	Angle of gas flow less than 15° with regard to duct axis	YES
b	No local negative flow	YES
c	Minimum pitot greater than 5Pa	YES
d	Ratio of highest to lowest local gas velocity less than 3:1	YES
	Minimum local gas velocity	2.5
	Maximum local gas velocity	5.0
	Ratio of highest to lowest local gas velocity	2.00

Preliminary Velocity Traverse Data

Date 29/01/2016

From 09:45 to 10:15 30 minute mean

Volatile organic compounds	vppm, wet	5.69	mg/m ³ *	9.15
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From 10:15 to 10:45 30 minute mean

Volatile organic compounds	vppm, wet	5.02	mg/m ³ *	8.06
----------------------------	-----------	------	---------------------	------

From 10:45 to 11:15 30 minute mean

Volatile organic compounds	vppm, wet	6.24	mg/m ³ *	10.03
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Sampling Detection Limits

Volatile organic compounds	vppm	0.10	mg/m ³ *	0.16
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Reference Gas Details

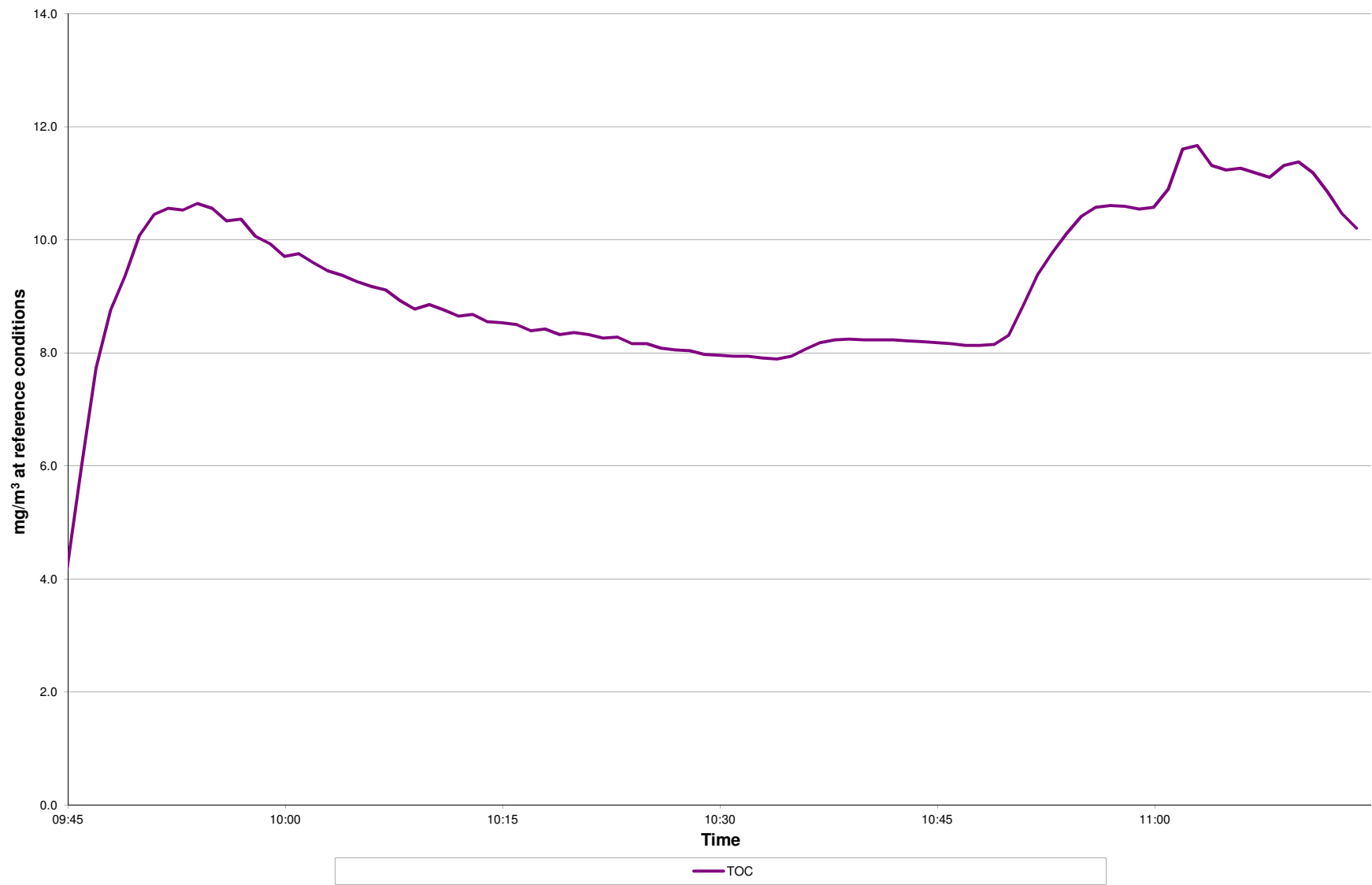
Species	Units	Value	Cylinder Reference	Analyser Range	Uncertainty <i>k</i> = 2
Nitrogen	%	99.999	VCK01959	-	± 2
Volatile organic compounds	vppm	75.50	VCSMG3066	10	± 2

Zero And Span Gas Details

Species	units	Initial Time	09:35	Final Time	11:26
		Initial Zero	Initial Span	Final Zero	Final Span
Volatile organic compounds	vppm	0.00	75.50	0.14	75.66

Exhaust Gases - Continuous Analysis Data

Chart 1 - Exhaust Gases - Xaarjet Ltd, Huntingdon, LEV 14, 29/01/16



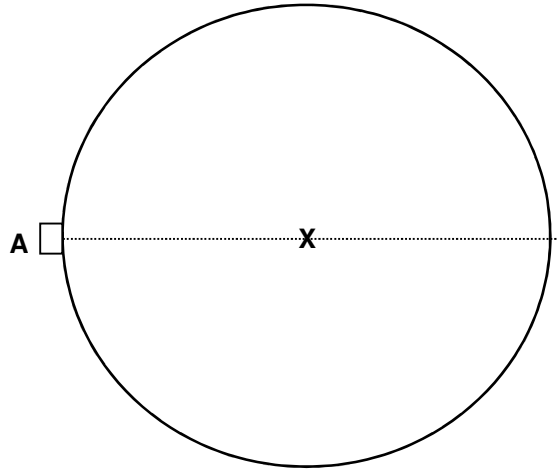
APPENDIX 3

Diagram Of The Sampling Location

Diagram of sampling points across the cross section of the duct (not to scale).

Traverse length = 0.45 m

Point	% of D	Location cm
1	50.0	22.5



Backend Assembly VOC

LEV 14
Room extract

General Calculations

Stack area:

$$\text{Area of a circle} = \frac{\pi \cdot D^2}{4}$$

D = Diameter (m)

π = 3.142

Pressure conversion:

1mmH₂O = 0.00980665 kPa

1mmH₂O = 9.80665 Pa

1 mar = 0.1 kPa

Water vapour concentration:

From reference calculations (taken from BS EN 14790):

$$V_{WC(\%)} = \frac{\frac{m_{WC} \cdot V_{mol(std)}}{M_w}}{\frac{m_{WC} \cdot V_{mol(std)}}{M_w} + V_{m(std)}} \times 100$$

WVC (%) = Water vapour content on wet basis, in volume % (m³ of water vapour in m³ of wet gas)

V_{m(std)} = Dry gas volume measured, corrected to standard conditions (m³)

m_{WC} = Mass of water collected in the impingers (g)

M_w = Molecular weight of water, 18.01534 rounded to 18 (g/mol)

V_{mol(std)} = Molar volume of water at standard conditions = 0.0224 (m³/mol)

Gas meter volume at standard conditions (STP)

From reference calculations (taken from BS EN 14790):

$$V_{m(std)} = y_d \times (V_2 - V_1) \times \frac{T_{std}}{T_m} \times \frac{p_m}{p_{std}}$$

V_{m(std)} = Dry gas meter volume at standard conditions (m³)

y_d = Gas meter calibration coefficient

(V₂-V₁) = Dry gas meter volume at actual conditions (m³)

T_m = Actual Temperature (K)

T_{std} = Standard temperature (273 K)

p_m = Absolute pressure at the gas meter (kPa)

p_{std} = Standard gas pressure (101.3 kPa)

Isokenetic Ratio (%):

From reference calculations (taken from EA TGN M2):

$$\text{IsokineticRatio}(\%) = \frac{\text{Velocity at the sampling nozzle}}{\text{Velocity of the stack gas}} \times 100$$

Estimating Measurement Uncertainty

Uncertainty estimates are calculated using the general rule of uncertainty propagation. Guidance is taken from publications including UKAS document M3003 and ISO 20988:2007.

Flow Calculations

Velocity:

From reference calculations (taken from ISO 10780):

$$\bar{v} = KC \sqrt{\frac{T_s \Delta p}{p_e M_s}}$$

\bar{v} = Average velocity (m/s)

C = velocity calculation constant = 129

T_s = Average stack temperature (K)

M_s = Molar mass of gas; assume 29 kg/kmol unless the molar mass is < 27 kg/kmol or > 31 g/kmol

K = Pitot calibration coefficient

p_e = Absolute gas pressure (kPa)

Δp = Average pitot tube pressure differential (kPa)

Volume flow rate

From reference calculations (taken from ISO 10780):

$$q_{va} = \bar{v} A$$

q_{va} = Average flow rate (m³/s)

\bar{v} = Average velocity (m/s)

A = Stack cross-sectional area (m²)

Volume flow rate corrected for moisture

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(100 - H_a)}{(100 - H_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

H_a = Moisture at actual conditions (%volume)

H_m = Reference moisture (%volume)

Volume flow rate corrected for temperature and pressure

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(T_m p_a)}{(T_a p_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

T_a = Temperature at actual conditions (K)

T_m = Reference Temperature (K)

p_a = Absolute gas pressure at actual conditions (kPa)

p_m = Reference pressure (kPa)

Volume flow rate corrected for oxygen

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(20.9 - O_{2,ref})}{(20.9 - O_{2,m})}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

$O_{2,m}$ = Actual oxygen concentration (%)

$O_{2,ref}$ = Reference oxygen concentration (%)

Concentration Calculations

Concentration:

From reference calculations (taken from BS EN 13284-1):

$$c = \frac{m}{V}$$

c = Concentration
 m = Mass of substance
 V = Volume sampled

Mass Emission

$$\text{Mass emission} = c \times q_m$$

c = Concentration
 q = Volume flow rate

Concentration corrected for oxygen:

From reference calculations (taken from BS ISO 9096):

$$c_m = c_a \times \frac{20.9 - O_{2,ref}}{20.9 - O_{2,a}}$$

cm = Concentration at reference conditions
 ca = Actual concentration
 $O_{2, ref}$ = Reference oxygen (%)
 $O_{2, a}$ = Actual Oxygen (%)

Concentration corrected for moisture:

From reference calculations (taken from BS ISO 9096):

Convert wet gas to dry gas

$$c_{dry} = c_{wet} \times \frac{100}{100 - H_a}$$

Convert dry gas to wet gas

$$c_{wet} = c_{dry} \times \frac{100 - H_a}{100}$$

c_{wet} = Concentration wet gas
 c_{dry} = Concentration dry gas
 H_a = Water vapour content (%vol)

Conversion of parts per million (ppm) to mg/m³

From reference calculations (taken from EA TGN M2):

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

When Converting TOC

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight of carbon in span gas}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

Calculation of Uncertainty Estimates - Instrumental Monitoring Techniques

Model equation

$$C_{ppm} = C_{reading} + Corr_{fit} + Corr_{0,dr} + Corr_{s,dr} + Corr_{rep} + Corr_{adj} + \sum_{i=1}^p Corr_{inf} + Corr_{int}$$

Where:

C_{ppm}	=	concentration in ppm	$Corr_{rep}$	=	correction of repeatability of measurement
$C_{NO,reading}$	=	concentration given by analyser	$Corr_{adj}$	=	correction of adjustment
$Corr_{fit}$	=	correction of lack of fit	$Corr_{inf}$	=	correction of influence quantities
$Corr_{0,dr}$	=	correction of zero drift	$Corr_{int}$	=	correction of interferences
$Corr_{s,dr}$	=	correction of span drift			

Calculation of partial uncertainties

$$u(Corr_{fit}) = \frac{\left(\frac{X_{fit,max}}{100 \times range} \right)}{\sqrt{3}} \quad \text{Where: } X_{fit,max} \text{ is the maximum allowable deviation from linearity}$$

Expressed as % of the range and calculated by applying a rectangular probability distribution

$$u(Corr_{0,dr}) = \frac{X_{0,dr}}{\sqrt{3}} \quad u(Corr_{s,dr}) = \frac{X_{s,dr}}{\sqrt{3}}$$

$$u(Corr_{rep}) = \max(S_{0,rep}; S_{s,rep}) = S_{rep} \quad \text{Where: } S_{r,0} \text{ is the standard uncertainty at zero level}$$

$$S_{r,s} \text{ is the standard uncertainty at span level}$$

$$u(Corr_{adj}) = u(Corr_{loss}) + u(Corr_{cal}) \quad \text{Where: } u(Corr_{loss}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{loss}) = \frac{C_{j,loss}}{\sqrt{3}} \quad u(Corr_{cal}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{cal}) = \frac{U_{cal}}{2} \quad c_{j,loss} \text{ is the concentration of sample loss at span level}$$

$$U_{cal} \text{ is the expanded uncertainty of the calibration gas}$$

$$u(Corr_{inf}) = c_j \sqrt{\frac{(x_{j,max} - x_{j,adj})^2 + (x_{j,min} - x_{j,adj})^2 + (x_{j,max} - x_{j,adj})(x_{j,min} - x_{j,adj})}{3}}$$

Where:

- c_j is the sensitivity coefficient of the influence quantity
- $x_{j,min}$ is the minimum value of the influence quantity during monitoring
- $x_{j,max}$ is the maximum value of the influence quantity during monitoring
- $x_{j,adj}$ is the value of the influence quantity during adjustment

$$u(Corr_{int}) = \frac{c_j}{Int_{j,test}} \sqrt{\frac{Int_{j,max}^2 + Int_{j,min} \times Int_{j,max} + Int_{j,min}^2}{3}}$$

and

$$u(\Sigma Corr_{int}) = \max[S_{Int,p}; S_{Int,n}] \quad \text{Where: } c_j \text{ is the sensitivity coefficient of the interferent j}$$

- $Int_{j,test}$ is the concentration of the interferent j used to determine c_j
- $Int_{j,min}$ is the minimum value of the interferent j quantity during monitoring
- $Int_{j,max}$ is the maximum value of the interferent j quantity during monitoring
- $Int_{j,adj}$ is the concentration of the interferent j in the cal gas used to adjust the analyser
- $S_{Int,p}$ is the sum of interferences with positive impact
- $S_{Int,n}$ is the sum of interferences with negative impact

Combined uncertainty

$$u(C_{ppm}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2}$$

$$\text{Overall expanded uncertainty (k = 2)} \quad U(C_m) = u(C_m) \times k$$

Uncertainty of NOx measurements

$$u(C_{NOx,conv}) = \frac{C_{NOx} \times R \times \eta}{\sqrt{3}} \quad \text{Where: } C_{NOx} \text{ is the concentration of NOx measured by the analyser}$$

- R is the ratio of NO:Nox in the stack gas
- η is the NOx converter efficiency

Combined uncertainty NOx measurements

$$u(C_{NOx,stack}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + u^2(Corr_{NOx,conv})}$$

Uncertainty of mass concentration at oxygen reference concentration

$$u(C_{O_2,ref}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + \left(\frac{u^2(O_{2,meas,dry})}{(21 - O_{2,meas,dry})^2} \right)}$$

Where:

$u(C_{O_2,ref})$	=	uncertainty associated with the mass concentration at O ₂ ref. concentration	in	mg/m ³
$C_{O_2,ref}$	=	mass concentration at O ₂ reference concentration	in	mg/m ³
$O_{2,meas}$	=	O ₂ measured concentration	in	% volume
$u((O_{2,meas})_{dry})$	=	uncertainty associated to the measured O ₂ concentration	in	% (relative to O ₂ meas)

APPENDIX 4

Uncertainty Estimate For The Measurement Of Total Organic Carbon

Analyser Type/Model

Sick Maihak

Reference Oxygen %

0

(0 = No correction)

		Test 1	Test 2	Test 3
Limit value	mg/m ³	75	75	75
Limit value	ppm	46.7	46.7	46.7
Measured concentration	ppm	5.7	5.0	6.2
Measured concentration	mg/m ³	9.2	8.1	10.0

Calibration gas	ppm	75.5	75.5	75.5
Calibration gas	mg/m ³	121.3	121.3	121.3
Analyser range	ppm	9.3	9.3	9.3
Analyser range	mg/m ³	15.0	15.0	15.0

Correction of Lack of Fit

Lack of fit	% range	2.0	2.0	2.0
	$u(\text{Corr}_{\text{lof}})$	0.11	0.11	0.11

Corrections of Zero and Span Drift

(* All drift is calculated for \therefore the residual is assumed to be < 5% $u(\text{max})$)

Zero Drift	% range	0.00	0.00	0.00
	$u(\text{Corr}_{\text{zdr}})$	0.00	0.00	0.00
Span Drift	% range	0.00	0.00	0.00
	$u(\text{Corr}_{\text{spr}})$	0.00	0.00	0.00

Correction of Repeatability of Measurement

Repeatability SD at span level (Not reported)	% range	0.0	0.0	0.0
	$u(\text{Corr}_{\text{rep}})$	0.00	0.00	0.00

Correction of adjustment

losses in the line	% range	0.21	0.21	0.21
	$u(\text{Corr}_{\text{loss}})$	0.01	0.01	0.01
Uncertainty of calibration gas	% range	2.0	2.0	2.0
	$u(\text{Corr}_{\text{cga}})$	0.06	0.05	0.06

Correction of Influence of Interferents

N ₂ O	% range			
	$u(\text{Corr}_{\text{N2O}})$	0.00	0.00	0.00
CO ₂	% range			
	$u(\text{Corr}_{\text{CO2}})$	0.00	0.00	0.00
CH ₄	% range			
	$u(\text{Corr}_{\text{CH4}})$	0.00	0.00	0.00
Total of interferent influences $u(\Sigma \text{Corr}_{\text{int}}) = \max[S_{\text{int},p}; S_{\text{int},n}]$	% range	2.50	2.50	2.50
	$u(\Sigma \text{Corr}_{\text{int}})$	0.16	0.16	0.16

Correction of Influence Quantities

Sensitivity to sample volume flow	% range	1.60	1.60	1.60
	$u(\text{Corr}_{\text{scv}})$	0.09	0.09	0.09
Sensitivity to atmospheric pressure (Not reported)	% range			
	$u(\text{Corr}_{\text{press}})$	0.00	0.00	0.00
Sensitivity to ambient temperature	% range	-2.40	-2.40	-2.40
	$u(\text{Corr}_{\text{temp}})$	-0.28	-0.28	-0.28
Sensitivity to electrical voltage (Not reported)	% range	0.50	0.50	0.50
	$u(\text{Corr}_{\text{voltage}})$	0.10	0.10	0.10

Maximum standard uncertainty	$u(\text{Corr}_{\text{max}})$	0.11	0.11	0.11
5% of maximum standard uncertainty	$u(\text{Corr}_{\text{5\%}})$	0.01	0.01	0.01

Interferent Concentration Variations	Minimum	Maximum	Value at cal	Performance	Units
CH ₄ range	0	10	0	50	mg/m ³
N ₂ O range	0	0	0	20	mg/m ³
CO ₂ range	8	12	0	15	mg/m ³
Oxygen effect variations	Minimum	Maximum	Value at cal	Performance	Units
Oxygen effect	0	20	0	2	mg/m ³

Influence Quantity Variations

	Minimum	Maximum	Value at cal	Performance	Units
Sensitivity to sample volume flow	55	65	60	5	l/h
Sensitivity to atmospheric pressure	99	100	99	1	kPa
Sensitivity to ambient temperature	278	313	288	10	K
Sensitivity to electrical voltage	187	250	230	5	V

Measurement uncertainty		Test 1	Test 2	Test 3
Combined uncertainty	ppm	0.37	0.37	0.37
Combined uncertainty	mg/m ³	0.59	0.59	0.59

Expanded uncertainty expressed with a level of confidence of 95%, k=2

Overall uncertainty	ppm	0.7	0.7	0.7
Overall uncertainty	mg/m ³	1.2	1.2	1.2
Overall uncertainty relative to measured value	%	13.0	14.7	11.9
Overall uncertainty relative to range	%	7.9	7.9	7.9
Overall uncertainty relative to ELV	%	1.0	1.0	1.0

The uncertainty evaluation has been carried out in accordance with UKAS requirements.



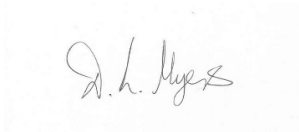
Client Xaarjet Ltd
1 Hurricane Close
Ermine Business Park
Huntingdon
Cambridgeshire
PE29 6XX

Part 1: Executive Summary

Report for the Periodic Monitoring of Emissions to Air.

Site	Huntingdon
Plant	LEV 17
Sampling Date	29th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4

Report Approved by:	Sign		
	Print	Derek Myers	
	MCERTS No.	MM02 115	Level 2 TE: 1,2,3,4



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Company Registration No SC070429

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Monitoring Objectives

The monitoring was undertaken to check compliance with authorised emission limits.

All monitoring procedures were carried out to the MCERTS requirements under the Exova (UK) Ltd quality system to ISO 17025: 2005.

Monitoring was undertaken for the listed emissions from the following sampling positions:

Sampling Location	Emission
LEV 17	Total volatile organic carbon

Special Monitoring Requirements

There were no special requirements for this monitoring campaign.

Summary of Methods

Emission	Method number	Method standard
Gas velocity and volume flow TOC	TPM/01A MM0002	BS EN ISO 16911-1:2013 BS EN 12619 : 2013

Summary Of Results

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 17	Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
	Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	29/01/16	10:05	11:35	10.3	75	1.2	0.2	5.1

* at reference conditions	Stack Gas Weight 29.00 Kg/kmol	0 °C 101.3 kPa	Without correction for moisture Oxygen No Correction %
---------------------------	-----------------------------------	-------------------	---

Where applicable

Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report:

* Reference conditions (see above)
** Analysis not required
ND Non detectable
s - Subcontracted laboratory analysis

Nm³ 273 K, 101.3 kPa
- UKAS accredited only
- Not Accredited
N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated.
Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Summary Of Results, Exhaust Gases

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 17		Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
		Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	Test 1	29/01/16	10:05	10:35	9.1	75	1.2	0.2	4.6
TOC	Test 2	29/01/16	10:35	11:05	13.4	75	1.2	0.2	6.7
TOC	Test 3	29/01/16	11:05	11:35	8.2	75	1.2	0.2	4.1

* at ref	Stack Gas Weight	0 °C	Without correction for moisture
Conditions	29.00 Kg/kmol	101.3 kPa	Oxygen No Correction %

Where applicable Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report: * Reference conditions (see above) Nm³ 273 K, 101.3 kPa
 ** Analysis not required # - UKAS accredited only
 ND Non detectable ## - Not Accredited
 s - Subcontracted laboratory analysis N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated. Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Operating Information

The table below shows details of the operating information on each sampling date for: **LEV 17**

Date	Process type	Process duration	Fuel	Feedstock	Abatement	Load
29/01/2016	Production and cleaning of inkjet cartridges	Continuous	N/A	N/A	N/A	Normal

No CEMs installed on the emission point.

Comments & Monitoring Deviations

A waste gas homogeneity test to BS EN 15259:2007 (MID) is not required:-

The homogeneity test is not applicable to non-combustion processes.

The homogeneity test is not applicable to duct areas less than 1m².

The homogeneity test is not usually applicable to pollutant emissions that are less than 30% of the ELV.

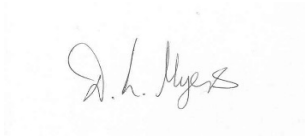
All monitoring was performed in accordance with the relevant procedures.



Part 2: Supporting Information

Report for the Periodic Monitoring of Emissions to Air.

Client	Xaarjet Ltd
Site	Huntingdon
Plant	LEV 17
Sampling Date	29th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4
Report Approved by:	Sign		
	Print	Derek Myers	
	MCERTS No.	MM02 115	Level 2 TE: 1,2,3,4



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APPENDIX 1

Emission Monitoring Procedures And Instrumentation

Gas velocity and temperature

Documented in-house procedure TPM01/A to the main procedural requirements of BS EN ISO 16911-1:2013
Velocity and temperature measurements are performed using a calibrated Pitot tube, a calibrated pressure differential reading device and a calibrated thermocouple. Velocity and possible flow deviation measurements are carried out at selected, representative points in the gas stream.

Total organic carbon

Documented in-house procedure MM0002 to the main procedural requirements of BS EN 12619:2013.
Continuous analysis using probe, sample line and multi range Flame Ionisation Detector (FID) analyser. The analyser is calibrated before and during the tests using certified gas mixtures of nitrogen, oxygen and propane. Sampling points are selected in accordance with the findings of any BS EN 15259 assessment.

Sampling Project Personnel Competency And Expiry Dates

		MCERTS No	Level 1	Level 2	TE1	TE2	TE3	TE4
Report prepared by:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Report authorised by:	Derek Myers	MM02 115	-	30/09/2017	31/05/2018	30/11/2018	30/11/2018	30/11/2018
Team leader:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Team leader:	Harpreet Badwal	MM03 149	-	30/09/2018	30/09/2018	30/04/2019	31/10/2019	31/10/2019

Equipment References

Equipment	Reference Number
FID	AQ270
Heated Line	HL33
Stack Thermocouple	PTTS97
Timer / Stopwatch	ST41
Barometer	WS03
Pitot	PT97
Thermometer	TK24
Manometer	PI03

APPENDIX 2

Date	29/01/2016
Time	12:05
Pitot Cp	0.79

Barometric pressure	101.6	kPa
Duct static pressure	0.14	kPa
Stack Area	0.049	m ²

Stack Diameter (circular)	0.25	m
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Traverse	Traverse	Depth	ΔP	T	Angle	velocity	Traverse	Depth	ΔP	T	Angle	velocity
Point	Line	cm	mmH ₂ O	°C	°	m/s	Line	cm	mmH ₂ O	°C	°	m/s
1	A						B					
2	A						B					
3	A						B					
4	A	5.0	0.6	19	>15	2.5	B	5.0	0.6	19	>15	2.5
5	A	6.3	0.9	19	<15	3.0	B	6.3	0.8	19	<15	2.9
6	A	8.9	1.0	19	<15	3.2	B	8.9	0.9	19	<15	3.0
7	A	16.1	1.4	19	<15	3.8	B	16.1	1.0	19	<15	3.2
8	A	18.8	1.0	19	<15	3.2	B	18.8	1.2	19	<15	3.5
9	A	20.0	0.7	19	<15	2.7	B	20.0	0.8	19	<15	2.9
10	A						B					
11	A						B					
12	A						B					

Average Pitot DP	0.91	mmH ₂ O
Average Temperature	294.7	K
Average Velocity	3.0	m/s
Average volumetric flow rate	0.15	m ³ /s at stack conditions
Average volumetric flow rate	0.14	m ³ /s (wet STP)

Sampling plane requirements Re: BS EN 13284-1:2001 5.2

a	Angle of gas flow less than 15° with regard to duct axis	YES
b	No local negative flow	YES
c	Minimum pitot greater than 5Pa	YES
d	Ratio of highest to lowest local gas velocity less than 3:1	YES
	Minimum local gas velocity	2.5
	Maximum local gas velocity	3.8
	Ratio of highest to lowest local gas velocity	1.53

Preliminary Velocity Traverse Data

Date 29/01/2016

From 10:05 to 10:35 30 minute mean

Volatile organic compounds	vppm, wet	5.67	mg/m ³ *	9.11
----------------------------	-----------	------	---------------------	------

From 10:35 to 11:05 30 minute mean

Volatile organic compounds	vppm, wet	8.36	mg/m ³ *	13.44
----------------------------	-----------	------	---------------------	-------

From 11:05 to 11:35 30 minute mean

Volatile organic compounds	vppm, wet	5.13	mg/m ³ *	8.24
----------------------------	-----------	------	---------------------	------

Sampling Detection Limits

Volatile organic compounds	vppm	0.10	mg/m ³ *	0.16
----------------------------	------	------	---------------------	------

Reference Gas Details

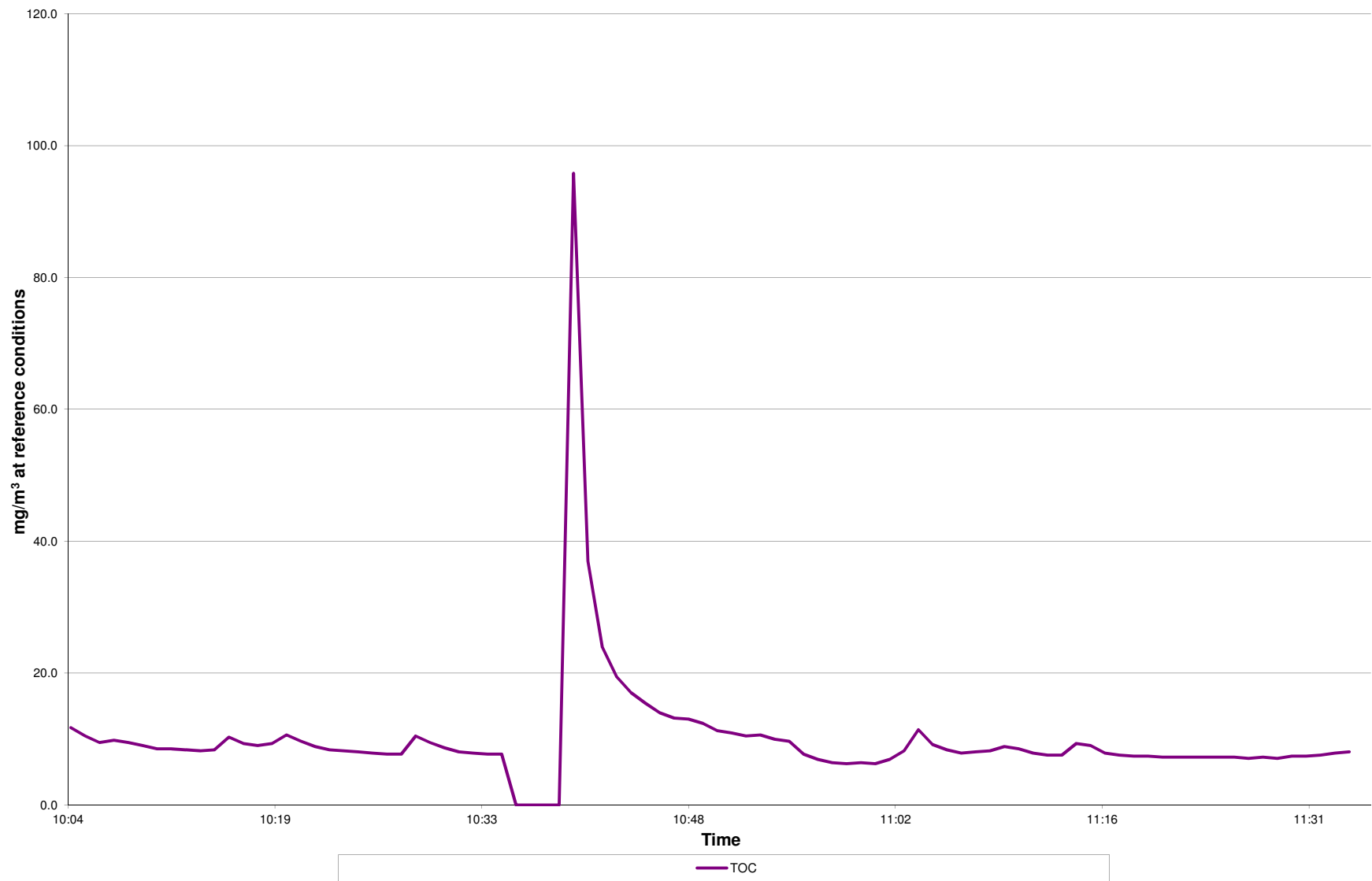
Species	Units	Value	Cylinder Reference	Analyser Range	Uncertainty <i>k</i> = 2
Nitrogen	%	99.999	VC80548	-	± 2
Volatile organic compounds	vppm	76.6	VCD500681	100	± 2

Zero And Span Gas Details

Species	units	Initial Time	09:54	Final Time	11:57
		Initial Zero	Initial Span	Final Zero	Final Span
Volatile organic compounds	vppm	0.0	76.6	-0.4	76.1

Exhaust Gases - Continuous Analysis Data

Chart 1 - Exhaust Gases - Xaarjet Ltd, Huntingdon, LEV 17, 29/01/16



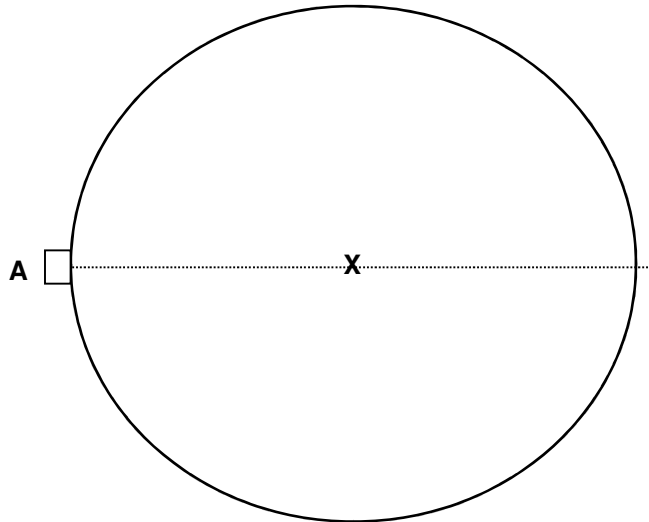
APPENDIX 3

Diagram Of The Sampling Location

Diagram of sampling points across the cross section of the duct (not to scale).

Traverse length = 0.25 m

Point	% of D	Location cm
1	50.0	12.5



General Calculations

Stack area:

$$\text{Area of a circle} = \frac{\pi \cdot D^2}{4}$$

D = Diameter (m)

π = 3.142

Pressure conversion:

1mmH₂O = 0.00980665 kPa

1mmH₂O = 9.80665 Pa

1 mar = 0.1 kPa

Water vapour concentration:

From reference calculations (taken from BS EN 14790):

$$V_{WC(\%)} = \frac{\frac{m_{WC} \cdot V_{mol(std)}}{M_w}}{\frac{m_{WC} \cdot V_{mol(std)}}{M_w} + V_{m(std)}} \times 100$$

WVC (%) = Water vapour content on wet basis, in volume % (m³ of water vapour in m³ of wet gas)

V_{m(std)} = Dry gas volume measured, corrected to standard conditions (m³)

m_{WC} = Mass of water collected in the impingers (g)

M_w = Molecular weight of water, 18.01534 rounded to 18 (g/mol)

V_{mol(std)} = Molar volume of water at standard conditions = 0.0224 (m³/mol)

Gas meter volume at standard conditions (STP)

From reference calculations (taken from BS EN 14790):

$$V_{m(std)} = y_d \times (V_2 - V_1) \times \frac{T_{std}}{T_m} \times \frac{p_m}{p_{std}}$$

V_{m(std)} = Dry gas meter volume at standard conditions (m³)

y_d = Gas meter calibration coefficient

(V₂-V₁) = Dry gas meter volume at actual conditions (m³)

T_m = Actual Temperature (K)

T_{std} = Standard temperature (273 K)

p_m = Absolute pressure at the gas meter (kPa)

p_{std} = Standard gas pressure (101.3 kPa)

Isokenetic Ratio (%):

From reference calculations (taken from EA TGN M2):

$$\text{IsokineticRatio}(\%) = \frac{\text{Velocity at the sampling nozzle}}{\text{Velocity of the stack gas}} \times 100$$

Estimating Measurement Uncertainty

Uncertainty estimates are calculated using the general rule of uncertainty propagation. Guidance is taken from publications including UKAS document M3003 and ISO 20988:2007.

Flow Calculations

Velocity:

From reference calculations (taken from ISO 10780):

$$\bar{v} = KC \sqrt{\frac{T_s \Delta p}{p_e M_s}}$$

\bar{v} = Average velocity (m/s)

C = velocity calculation constant = 129

T_s = Average stack temperature (K)

M_s = Molar mass of gas; assume 29 kg/kmol unless the molar mass is < 27 kg/kmol or > 31 g/kmol

K = Pitot calibration coefficient

p_e = Absolute gas pressure (kPa)

Δp = Average pitot tube pressure differential (kPa)

Volume flow rate

From reference calculations (taken from ISO 10780):

$$q_{va} = \bar{v} A$$

q_{va} = Average flow rate (m³/s)

\bar{v} = Average velocity (m/s)

A = Stack cross-sectional area (m²)

Volume flow rate corrected for moisture

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(100 - H_a)}{(100 - H_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

H_a = Moisture at actual conditions (%volume)

H_m = Reference moisture (%volume)

Volume flow rate corrected for temperature and pressure

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(T_m p_a)}{(T_a p_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

T_a = Temperature at actual conditions (K)

T_m = Reference Temperature (K)

p_a = Absolute gas pressure at actual conditions (kPa)

p_m = Reference pressure (kPa)

Volume flow rate corrected for oxygen

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(20.9 - O_{2,ref})}{(20.9 - O_{2,m})}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

$O_{2,m}$ = Actual oxygen concentration (%)

$O_{2,ref}$ = Reference oxygen concentration (%)

Concentration Calculations

Concentration:

From reference calculations (taken from BS EN 13284-1):

$$c = \frac{m}{V}$$

c = Concentration
 m = Mass of substance
 V = Volume sampled

Mass Emission

$$\text{Mass emission} = c \times q_m$$

c = Concentration
 q = Volume flow rate

Concentration corrected for oxygen:

From reference calculations (taken from BS ISO 9096):

$$c_m = c_a \times \frac{20.9 - O_{2,ref}}{20.9 - O_{2,a}}$$

cm = Concentration at reference conditions
 ca = Actual concentration
 $O_{2, ref}$ = Reference oxygen (%)
 $O_{2, a}$ = Actual Oxygen (%)

Concentration corrected for moisture:

From reference calculations (taken from BS ISO 9096):

Convert wet gas to dry gas

$$c_{dry} = c_{wet} \times \frac{100}{100 - H_a}$$

Convert dry gas to wet gas

$$c_{wet} = c_{dry} \times \frac{100 - H_a}{100}$$

c_{wet} = Concentration wet gas
 c_{dry} = Concentration dry gas
 H_a = Water vapour content (%vol)

Conversion of parts per million (ppm) to mg/m³

From reference calculations (taken from EA TGN M2):

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

When Converting TOC

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight of carbon in span gas}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

Calculation of Uncertainty Estimates - Instrumental Monitoring Techniques

Model equation

$$C_{ppm} = C_{reading} + Corr_{fit} + Corr_{0,dr} + Corr_{s,dr} + Corr_{rep} + Corr_{adj} + \sum_{i=1}^p Corr_{inf} + Corr_{int}$$

Where:

C_{ppm}	=	concentration in ppm	$Corr_{rep}$	=	correction of repeatability of measurement
$C_{NO,reading}$	=	concentration given by analyser	$Corr_{adj}$	=	correction of adjustment
$Corr_{fit}$	=	correction of lack of fit	$Corr_{inf}$	=	correction of influence quantities
$Corr_{0,dr}$	=	correction of zero drift	$Corr_{int}$	=	correction of interferences
$Corr_{s,dr}$	=	correction of span drift			

Calculation of partial uncertainties

$$u(Corr_{fit}) = \frac{\left(\frac{X_{fit,max}}{100 \times range} \right)}{\sqrt{3}} \quad \text{Where: } X_{fit,max} \text{ is the maximum allowable deviation from linearity}$$

Expressed as % of the range and calculated by applying a rectangular probability distribution

$$u(Corr_{0,dr}) = \frac{X_{0,dr}}{\sqrt{3}} \quad u(Corr_{s,dr}) = \frac{X_{s,dr}}{\sqrt{3}}$$

$$u(Corr_{rep}) = \max(S_{0,rep}; S_{s,rep}) = S_{rep} \quad \text{Where: } S_{r,0} \text{ is the standard uncertainty at zero level}$$

$$S_{r,s} \text{ is the standard uncertainty at span level}$$

$$u(Corr_{adj}) = u(Corr_{loss}) + u(Corr_{cal}) \quad \text{Where: } u(Corr_{loss}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{loss}) = \frac{C_{j,loss}}{\sqrt{3}} \quad u(Corr_{cal}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{cal}) = \frac{U_{cal}}{2} \quad c_{j,loss} \text{ is the concentration of sample loss at span level}$$

$$U_{cal} \text{ is the expanded uncertainty of the calibration gas}$$

$$u(Corr_{int}) = c_j \sqrt{\frac{(x_{j,max} - x_{j,adj})^2 + (x_{j,min} - x_{j,adj})^2 + (x_{j,max} - x_{j,adj})(x_{j,min} - x_{j,adj})}{3}}$$

Where:

- c_j is the sensitivity coefficient of the influence quantity
- $x_{j,min}$ is the minimum value of the influence quantity during monitoring
- $x_{j,max}$ is the maximum value of the influence quantity during monitoring
- $x_{j,adj}$ is the value of the influence quantity during adjustment

$$u(Corr_{int}) = \frac{c_j}{Int_{j,test}} \sqrt{\frac{Int_{j,max}^2 + Int_{j,min} \times Int_{j,max} + Int_{j,min}^2}{3}}$$

and

$$u(\Sigma Corr_{int}) = \max[S_{Int,p}; S_{Int,n}] \quad \text{Where: } c_j \text{ is the sensitivity coefficient of the interferent j}$$

- $Int_{j,test}$ is the concentration of the interferent j used to determine c_j
- $Int_{j,min}$ is the minimum value of the interferent j quantity during monitoring
- $Int_{j,max}$ is the maximum value of the interferent j quantity during monitoring
- $Int_{j,adj}$ is the concentration of the interferent j in the cal gas used to adjust the analyser
- $S_{Int,p}$ is the sum of interferences with positive impact
- $S_{Int,n}$ is the sum of interferences with negative impact

Combined uncertainty

$$u(C_{ppm}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2}$$

$$\text{Overall expanded uncertainty (k = 2)} \quad U(C_m) = u(C_m) \times k$$

Uncertainty of NOx measurements

$$u(C_{NOx,conv}) = \frac{C_{NOx} \times R \times \eta}{\sqrt{3}} \quad \text{Where: } C_{NOx} \text{ is the concentration of NOx measured by the analyser}$$

- R is the ratio of NO:Nox in the stack gas
- η is the NOx converter efficiency

Combined uncertainty NOx measurements

$$u(C_{NOx,stack}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + u^2(Corr_{NOx,conv})}$$

Uncertainty of mass concentration at oxygen reference concentration

$$u(C_{O_2,ref}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + \left(\frac{u^2(O_{2,meas,dry})}{(21 - O_{2,meas,dry})^2} \right)}$$

Where:

$u(C_{O_2,ref})$	=	uncertainty associated with the mass concentration at O ₂ ref. concentration	in	mg/m ³
$C_{O_2,ref}$	=	mass concentration at O ₂ reference concentration	in	mg/m ³
$O_{2,meas}$	=	O ₂ measured concentration	in	% volume
$u((O_{2,meas})_{dry})$	=	uncertainty associated to the measured O ₂ concentration	in	% (relative to O ₂ meas)

APPENDIX 4

Uncertainty Estimate For The Measurement Of Total Organic Carbon

Analysers Type/Model
Reference Oxygen %

Sick Maihak
0 (0 = No correction)

		Test 1	Test 2	Test 3
Limit value	mg/m ³	75	75	75
Limit value	ppm	46.7	46.7	46.7
Measured concentration	ppm	5.7	8.4	5.1
Measured concentration	mg/m ³	9.1	13.4	8.2

Calibration gas	ppm	76.6	76.6	76.6
Calibration gas	mg/m ³	123.1	123.1	123.1
Analysers range	ppm	9.3	9.3	9.3
Analysers range	mg/m ³	15.0	15.0	15.0

Correction of Lack of Fit				
Lack of fit	% range	2.0	2.0	2.0
	u(Corr _{fit})	0.11	0.11	0.11

Corrections of Zero and Span Drift (*All drift is calculated for ∴ the residual is assumed to be < 5% u(max))				
Zero Drift	% range	0.00	0.00	0.00
	u(Corr _{zero})	0.00	0.00	0.00
Span Drift	% range	0.00	0.00	0.00
	u(Corr _{span})	0.00	0.00	0.00

Correction of Repeatability of Measurement				
Repeatability SD at span level (Not reported)	% range	0.0	0.0	0.0
	u(Corr _{rep})	0.00	0.00	0.00

Correction of adjustment				
losses in the line	% range	0.65	0.65	0.65
	u(Corr _{loss})	0.02	0.03	0.02
Uncertainty of calibration gas	% range	2.0	2.0	2.0
	u(Corr _{cal})	0.06	0.08	0.05

Correction of Influence of Interferents				
N ₂ O	% range			
	u(Corr _{N2O})	0.00	0.00	0.00
CO ₂	% range			
	u(Corr _{CO2})	0.00	0.00	0.00
CH ₄	% range			
	u(Corr _{CH4})	0.00	0.00	0.00
Total of interferent influences	% range	2.50	2.50	2.50
u(ΣCorr _{int}) = max[S _{int,1} ; S _{int,2}]	u(ΣCorr _{int})	0.16	0.16	0.16

Correction of Influence Quantities				
Sensitivity to sample volume flow	% range	1.60	1.60	1.60
	u(Corr _{vol})	0.09	0.09	0.09
Sensitivity to atmospheric pressure (Not reported)	% range			
	u(Corr _{press})	0.00	0.00	0.00
Sensitivity to ambient temperature	% range	-2.40	-2.40	-2.40
	u(Corr _{temp})	-0.28	-0.28	-0.28
Sensitivity to electrical voltage (Not reported)	% range	0.50	0.50	0.50
	u(Corr _{volt})	0.10	0.10	0.10

Maximum standard uncertainty	u(Corr _{max})	0.11	0.11	0.11
5% of maximum standard uncertainty	u(Corr _{5%})	0.01	0.01	0.01

Interferent Concentration Variations	Minimum	Maximum	Value at cal	Performance	Units
CH ₄ range	0	10	0	50	mg/m ³
N ₂ O range	0	0	0	20	mg/m ³
CO ₂ range	8	12	0	15	mg/m ³
Oxygen effect variations	Minimum	Maximum	Value at cal	Performance	Units
Oxygen effect	0	20	0	2	mg/m ³

Influence Quantity Variations	Minimum	Maximum	Value at cal	Performance	Units
Sensitivity to sample volume flow	55	65	60	5	l/h
Sensitivity to atmospheric pressure	99	100	99	1	kPa
Sensitivity to ambient temperature	278	313	288	10	K
Sensitivity to electrical voltage	187	250	230	5	V

Measurement uncertainty				
		Test 1	Test 2	Test 3
Combined uncertainty	ppm	0.37	0.38	0.37
Combined uncertainty	mg/m ³	0.59	0.60	0.59

Expanded uncertainty expressed with a level of confidence of 95%, k=2

Overall uncertainty	ppm	0.7	0.8	0.7
Overall uncertainty	mg/m ³	1.2	1.2	1.2
Overall uncertainty relative to measured value	%	13.1	9.0	14.4
Overall uncertainty relative to range	%	7.9	8.0	7.9
Overall uncertainty relative to ELV	%	1.0	1.0	1.0

The uncertainty evaluation has been carried out in accordance with UKAS requirements.



Client
 Xaarjet Ltd
 1 Hurricane Close
 Ermine Business Park
 Huntingdon
 Cambridgeshire
 PE29 6XX

Part 1: Executive Summary

Report for the Periodic Monitoring of Emissions to Air.

Site	Huntingdon
Plant	LEV 19
Sampling Date	28th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4

Report Approved by:	Sign		
	Print	Derek Myers	
	MCERTS No.	MM02 115	Level 2 TE: 1,2,3,4



1783

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 Company Registration No SC070429

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Monitoring Objectives

The monitoring was undertaken to check compliance with authorised emission limits.

All monitoring procedures were carried out to the MCERTS requirements under the Exova (UK) Ltd quality system to ISO 17025: 2005.

Monitoring was undertaken for the listed emissions from the following sampling positions:

Sampling Location	Emission
LEV 19	Total volatile organic carbon

Special Monitoring Requirements

There were no special requirements for this monitoring campaign.

Summary of Methods

Emission	Method number	Method standard
Gas velocity and volume flow TOC	TPM/01A MM0002	BS EN ISO 16911-1:2013 BS EN 12619 : 2013

Summary Of Results

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 19	Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
	Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	28/01/16	13:54	15:24	8.8	75	1.2	0.2	31.7

* at reference conditions	Stack Gas Weight 29.00 Kg/kmol	0 °C 101.3 kPa	Without correction for moisture Oxygen No Correction %
---------------------------	-----------------------------------	-------------------	---

Where applicable

Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report:

* Reference conditions (see above)
** Analysis not required
ND Non detectable
s - Subcontracted laboratory analysis

Nm³ 273 K, 101.3 kPa
- UKAS accredited only
- Not Accredited
N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated.
Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Summary Of Results, Exhaust Gases

The table presents the atmospheric emissions from the tests undertaken on behalf of **Xaarjet Ltd**
The results were measured from the sample positions downstream of the arrestment plant.

Emission at Huntingdon LEV 19		Sampling Time			Emission Result	Authorised Limit	Uncertainty +/-	Detection Limit	Mass Emission
		Date	Start	End	mg/m ³ *	mg/m ³ *	mg/m ³ *	mg/m ³ *	g/h
TOC	Test 1	28/01/16	13:54	14:24	5.1	75	1.2	0.2	18.3
TOC	Test 2	28/01/16	14:24	14:54	8.2	75	1.2	0.2	29.4
TOC	Test 3	28/01/16	14:54	15:24	13.1	75	1.2	0.2	47.3

* at ref	Stack Gas Weight	0 °C	Without correction for moisture
Conditions	29.00 Kg/kmol	101.3 kPa	Oxygen No Correction %

Where applicable Oxides of nitrogen results are expressed as nitrogen dioxide
TOC results are expressed as total carbon

Throughout Report: * Reference conditions (see above) Nm³ 273 K, 101.3 kPa
 ** Analysis not required # - UKAS accredited only
 ND Non detectable ## - Not Accredited
 s - Subcontracted laboratory analysis N/A Not applicable

The reported expanded uncertainty is based on a standard uncertainty multiplied by a coverage factor k=2, providing a 95% confidence level. The uncertainty evaluation has been carried out in accordance with UKAS requirements.



All tests included in this report are accredited under UKAS and MCERTS accreditation schemes unless otherwise stated. Opinions and interpretations expressed herein are outside the scope of MCERTS and UKAS accreditation.



Operating Information

The table below shows details of the operating information on each sampling date for: **LEV 19**

Date	Process type	Process duration	Fuel	Feedstock	Abatement	Load
28/01/2016	Production and cleaning of inkjet cartridges	Continuous	N/A	N/A	N/A	Normal

No CEMs installed on the emission point.

Comments & Monitoring Deviations

A waste gas homogeneity test to BS EN 15259:2007 (MID) is not required:-

The homogeneity test is not applicable to non-combustion processes.

The homogeneity test is not applicable to duct areas less than 1m².

The homogeneity test is not usually applicable to pollutant emissions that are less than 30% of the ELV.

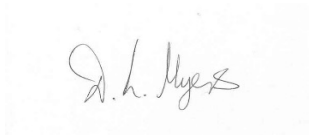
All monitoring was performed in accordance with the relevant procedures.



Part 2: Supporting Information

Report for the Periodic Monitoring of Emissions to Air.

Client	Xaarjet Ltd
Site	Huntingdon
Plant	LEV 19
Sampling Date	28th January 2016
Report Date	25th February 2016
Job Number	EM-2708
Permit Number	B22/11

Report Prepared by:	Print	Rob Jones	
	MCERTS No.	MM08 984	Level 2 TE: 1,2,3,4
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APPENDIX 1

Emission Monitoring Procedures And Instrumentation

Gas velocity and temperature

Documented in-house procedure TPM01/A to the main procedural requirements of BS EN ISO 16911-1:2013. Velocity and temperature measurements are performed using a calibrated Pitot tube, a calibrated pressure differential reading device and a calibrated thermocouple. Velocity and possible flow deviation measurements are carried out at selected, representative points in the gas stream.

Total organic carbon

Documented in-house procedure MM0002 to the main procedural requirements of BS EN 12619:2013. Continuous analysis using probe, sample line and multi range Flame Ionisation Detector (FID) analyser. The analyser is calibrated before and during the tests using certified gas mixtures of nitrogen, oxygen and propane. Sampling points are selected in accordance with the findings of any BS EN 15259 assessment.

Sampling Project Personnel Competency And Expiry Dates

		MCERTS No	Level 1	Level 2	TE1	TE2	TE3	TE4
Report prepared by:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Report authorised by:	Derek Myers	MM02 115	-	30/09/2017	31/05/2018	30/11/2018	30/11/2018	30/11/2018
Team leader:	Rob Jones	MM08 984	-	31/03/2016	31/03/2020	31/03/2016	30/09/2016	31/12/2020
Team leader:	Harpreet Badwal	MM03 149	-	30/09/2018	30/09/2018	30/04/2019	31/10/2019	31/10/2019

Equipment References

Equipment	Reference Number
FID	AQ270
Heated Line	HL33
Stack Thermocouple	PTTS97
Timer / Stopwatch	ST41
Barometer	WS03
Pitot	PT97
Thermometer	TK24
Manometer	PI03

APPENDIX 2

Date	28/01/2016
Time	12:15
Pitot Cp	0.79

Barometric pressure	101.6	kPa
Duct static pressure	-1.10	kPa
Stack Area	0.096	m ²

Stack Diameter (circular)	0.35	m
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Traverse Point	Traverse Line	Depth cm	ΔP mmH ₂ O	T °C	Angle °	velocity m/s	Traverse Line	Depth cm	ΔP mmH ₂ O	T °C	Angle °	velocity m/s
1	A						B					
2	A						B					
3	A	5.0	13.5	20	<15	11.7	B	5.0	12.5	20	<15	11.3
4	A	6.2	13.5	20	<15	11.7	B	6.2	13.0	20	<15	11.6
5	A	8.8	12.1	20	<15	11.1	B	8.8	13.8	20	<15	11.9
6	A	12.5	10.8	20	<15	10.5	B	12.5	13.1	20	<15	11.6
7	A	22.5	12.2	20	<15	11.2	B	22.5	12.7	20	<15	11.4
8	A	26.3	12.7	20	<15	11.4	B	26.3	11.7	20	<15	11.0
9	A	28.8	12.3	20	<15	11.2	B	28.8	11.4	20	<15	10.8
10	A	30.0	12.2	20	<15	11.2	B	30.0	10.5	20	<15	10.4
11	A						B					
12	A						B					

Average Pitot DP	12.37	mmH ₂ O
Average Temperature	293.2	K
Average Velocity	11.3	m/s
Average volumetric flow rate	1.08	m ³ /s at stack conditions
Average volumetric flow rate	1.00	m ³ /s (wet STP)

Sampling plane requirements Re: BS EN 13284-1:2001 5.2

a	Angle of gas flow less than 15° with regard to duct axis	YES
b	No local negative flow	YES
c	Minimum pitot greater than 5Pa	YES
d	Ratio of highest to lowest local gas velocity less than 3:1	YES
	Minimum local gas velocity	10.4
	Maximum local gas velocity	11.9
	Ratio of highest to lowest local gas velocity	1.14

Preliminary Velocity Traverse Data

Date 28/01/2016

From 13:54 to 14:24 30 minute mean

Volatile organic compounds	vppm, wet	3.16	mg/m ³ *	5.08
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From 14:24 to 14:54 30 minute mean

Volatile organic compounds	vppm, wet	5.08	mg/m ³ *	8.16
----------------------------	-----------	------	---------------------	------

From 14:54 to 15:24 30 minute mean

Volatile organic compounds	vppm, wet	8.16	mg/m ³ *	13.11
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Sampling Detection Limits

Volatile organic compounds	vppm	0.10	mg/m ³ *	0.16
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Reference Gas Details

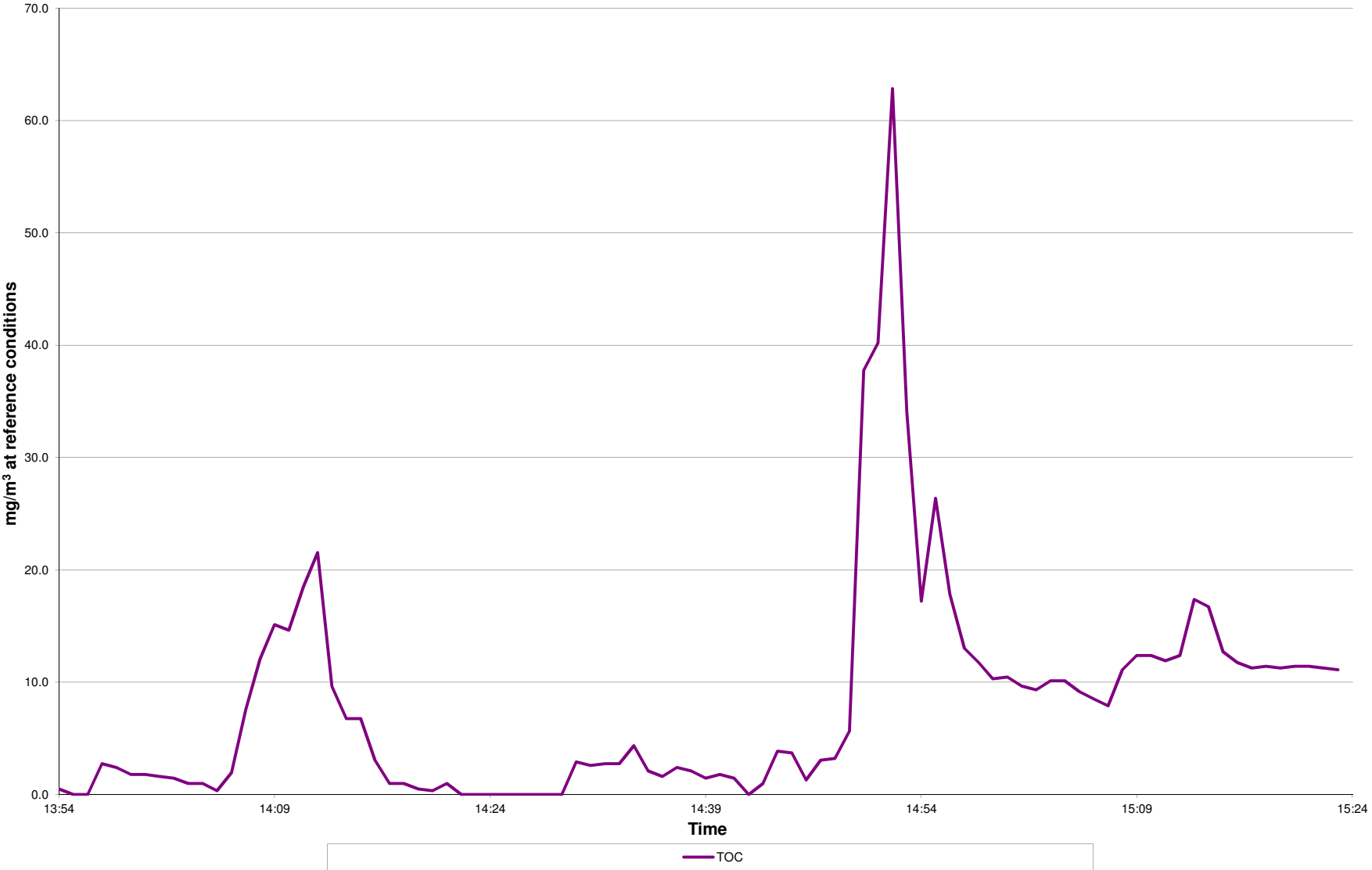
Species	Units	Value	Cylinder Reference	Analyser Range	Uncertainty <i>k</i> = 2
Nitrogen	%	99.999	VC80548	-	± 2
Volatile organic compounds	vppm	76.6	VCD500681	100	± 2

Zero And Span Gas Details

Species	units	Initial Time	11:40	Final Time	17:26
		Initial Zero	Initial Span	Final Zero	Final Span
Volatile organic compounds	vppm	0.0	76.6	-0.8	75.6

Exhaust Gases - Continuous Analysis Data

Chart 1 - Exhaust Gases - Xaarjet Ltd, Huntingdon, LEV 19, 28/01/16



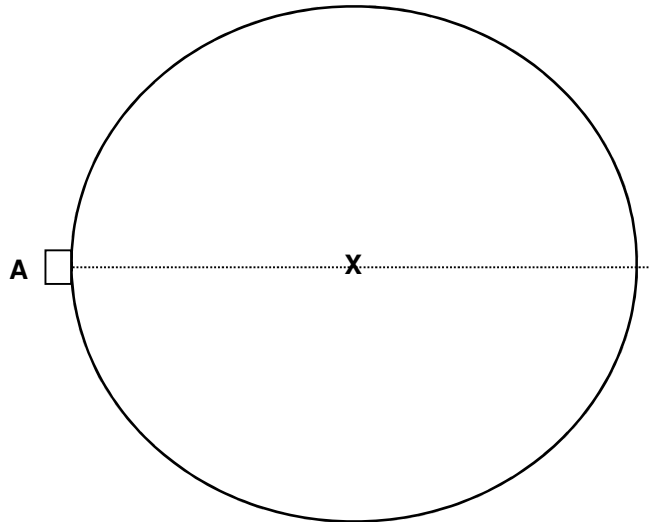
APPENDIX 3

Diagram Of The Sampling Location

Diagram of sampling points across the cross section of the duct (not to scale).

Traverse length = 0.35 m

Point	% of D	Location cm
1	50.0	17.5



General Calculations

Stack area:

$$\text{Area of a circle} = \frac{\pi \cdot D^2}{4}$$

D = Diameter (m)

π = 3.142

Pressure conversion:

1mmH₂O = 0.00980665 kPa

1mmH₂O = 9.80665 Pa

1 mar = 0.1 kPa

Water vapour concentration:

From reference calculations (taken from BS EN 14790):

$$V_{WC(\%)} = \frac{\frac{m_{WC} \cdot V_{mol(std)}}{M_w}}{\frac{m_{WC} \cdot V_{mol(std)}}{M_w} + V_{m(std)}} \times 100$$

WVC (%) = Water vapour content on wet basis, in volume % (m³ of water vapour in m³ of wet gas)

V_{m(std)} = Dry gas volume measured, corrected to standard conditions (m³)

m_{WC} = Mass of water collected in the impingers (g)

M_w = Molecular weight of water, 18.01534 rounded to 18 (g/mol)

V_{mol(std)} = Molar volume of water at standard conditions = 0.0224 (m³/mol)

Gas meter volume at standard conditions (STP)

From reference calculations (taken from BS EN 14790):

$$V_{m(std)} = y_d \times (V_2 - V_1) \times \frac{T_{std}}{T_m} \times \frac{p_m}{p_{std}}$$

V_{m(std)} = Dry gas meter volume at standard conditions (m³)

y_d = Gas meter calibration coefficient

(V₂-V₁) = Dry gas meter volume at actual conditions (m³)

T_m = Actual Temperature (K)

T_{std} = Standard temperature (273 K)

p_m = Absolute pressure at the gas meter (kPa)

p_{std} = Standard gas pressure (101.3 kPa)

Isokenetic Ratio (%):

From reference calculations (taken from EA TGN M2):

$$\text{IsokineticRatio}(\%) = \frac{\text{Velocity at the sampling nozzle}}{\text{Velocity of the stack gas}} \times 100$$

Estimating Measurement Uncertainty

Uncertainty estimates are calculated using the general rule of uncertainty propagation. Guidance is taken from publications including UKAS document M3003 and ISO 20988:2007.

Flow Calculations

Velocity:

From reference calculations (taken from ISO 10780):

$$\bar{v} = KC \sqrt{\frac{T_s \Delta p}{p_e M_s}}$$

\bar{v} = Average velocity (m/s)

C = velocity calculation constant = 129

T_s = Average stack temperature (K)

M_s = Molar mass of gas; assume 29 kg/kmol unless the molar mass is < 27 kg/kmol or > 31 g/kmol

K = Pitot calibration coefficient

p_e = Absolute gas pressure (kPa)

Δp = Average pitot tube pressure differential (kPa)

Volume flow rate

From reference calculations (taken from ISO 10780):

$$q_{va} = \bar{v} A$$

q_{va} = Average flow rate (m³/s)

\bar{v} = Average velocity (m/s)

A = Stack cross-sectional area (m²)

Volume flow rate corrected for moisture

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(100 - H_a)}{(100 - H_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

H_a = Moisture at actual conditions (%volume)

H_m = Reference moisture (%volume)

Volume flow rate corrected for temperature and pressure

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(T_m p_a)}{(T_a p_m)}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

T_a = Temperature at actual conditions (K)

T_m = Reference Temperature (K)

p_a = Absolute gas pressure at actual conditions (kPa)

p_m = Reference pressure (kPa)

Volume flow rate corrected for oxygen

From reference calculations (taken from BS ISO 9096):

$$q_m = q_{va} \frac{(20.9 - O_{2,ref})}{(20.9 - O_{2,m})}$$

q_m = Corrected volume flowrate (m³/s)

q_{va} = Volume flow rate at actual conditions (m³/s)

$O_{2,m}$ = Actual oxygen concentration (%)

$O_{2,ref}$ = Reference oxygen concentration (%)

Concentration Calculations

Concentration:

From reference calculations (taken from BS EN 13284-1):

$$c = \frac{m}{V}$$

c = Concentration
 m = Mass of substance
 V = Volume sampled

Mass Emission

$$\text{Mass emission} = c \times q_m$$

c = Concentration
 q = Volume flow rate

Concentration corrected for oxygen:

From reference calculations (taken from BS ISO 9096):

$$c_m = c_a \times \frac{20.9 - O_{2,ref}}{20.9 - O_{2,a}}$$

cm = Concentration at reference conditions
 ca = Actual concentration
 $O_{2, ref}$ = Reference oxygen (%)
 $O_{2, a}$ = Actual Oxygen (%)

Concentration corrected for moisture:

From reference calculations (taken from BS ISO 9096):

Convert wet gas to dry gas

$$c_{dry} = c_{wet} \times \frac{100}{100 - H_a}$$

Convert dry gas to wet gas

$$c_{wet} = c_{dry} \times \frac{100 - H_a}{100}$$

c_{wet} = Concentration wet gas
 c_{dry} = Concentration dry gas
 H_a = Water vapour content (%vol)

Conversion of parts per million (ppm) to mg/m³

From reference calculations (taken from EA TGN M2):

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

When Converting TOC

$$\text{Concentration}(\text{mg} / \text{m}^3) = \frac{\text{Concentration}(\text{ppm}) \times \text{molecular weight of carbon in span gas}(\text{g})}{\text{molar volume}(\text{l}) \text{ at a given temperature}}$$

molar volume at 273K = 22.4 litres

Calculation of Uncertainty Estimates - Instrumental Monitoring Techniques

Model equation

$$C_{ppm} = C_{reading} + Corr_{fit} + Corr_{0,dr} + Corr_{s,dr} + Corr_{rep} + Corr_{adj} + \sum_{i=1}^p Corr_{inf} + Corr_{int}$$

Where:

C_{ppm}	=	concentration in ppm	$Corr_{rep}$	=	correction of repeatability of measurement
$C_{NO,reading}$	=	concentration given by analyser	$Corr_{adj}$	=	correction of adjustment
$Corr_{fit}$	=	correction of lack of fit	$Corr_{inf}$	=	correction of influence quantities
$Corr_{0,dr}$	=	correction of zero drift	$Corr_{int}$	=	correction of interferences
$Corr_{s,dr}$	=	correction of span drift			

Calculation of partial uncertainties

$$u(Corr_{fit}) = \frac{\left(\frac{X_{fit,max}}{100 \times range} \right)}{\sqrt{3}} \quad \text{Where: } X_{fit,max} \text{ is the maximum allowable deviation from linearity}$$

Expressed as % of the range and calculated by applying a rectangular probability distribution

$$u(Corr_{0,dr}) = \frac{X_{0,dr}}{\sqrt{3}} \quad u(Corr_{s,dr}) = \frac{X_{s,dr}}{\sqrt{3}}$$

$$u(Corr_{rep}) = \max(S_{0,rep}; S_{s,rep}) = S_{rep} \quad \text{Where: } S_{r,0} \text{ is the standard uncertainty at zero level}$$

$$S_{r,s} \text{ is the standard uncertainty at span level}$$

$$u(Corr_{adj}) = u(Corr_{loss}) + u(Corr_{cal}) \quad \text{Where: } u(Corr_{loss}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{loss}) = \frac{C_{j,loss}}{\sqrt{3}} \quad u(Corr_{cal}) \text{ is the uncertainty due to losses in sample line}$$

$$u(Corr_{cal}) = \frac{U_{cal}}{2} \quad c_{j,loss} \text{ is the concentration of sample loss at span level}$$

$$U_{cal} \text{ is the expanded uncertainty of the calibration gas}$$

$$u(Corr_{inf}) = c_j \sqrt{\frac{(x_{j,max} - x_{j,adj})^2 + (x_{j,min} - x_{j,adj})^2 + (x_{j,max} - x_{j,adj})(x_{j,min} - x_{j,adj})}{3}}$$

Where:

- c_j is the sensitivity coefficient of the influence quantity
- $x_{j,min}$ is the minimum value of the influence quantity during monitoring
- $x_{j,max}$ is the maximum value of the influence quantity during monitoring
- $x_{j,adj}$ is the value of the influence quantity during adjustment

$$u(Corr_{int}) = \frac{c_j}{Int_{j,test}} \sqrt{\frac{Int_{j,max}^2 + Int_{j,min} \times Int_{j,max} + Int_{j,min}^2}{3}}$$

and

$$u(\Sigma Corr_{int}) = \max[S_{Int,p}; S_{Int,n}] \quad \text{Where: } c_j \text{ is the sensitivity coefficient of the interferent j}$$

- $Int_{j,test}$ is the concentration of the interferent j used to determine c_j
- $Int_{j,min}$ is the minimum value of the interferent j quantity during monitoring
- $Int_{j,max}$ is the maximum value of the interferent j quantity during monitoring
- $Int_{j,adj}$ is the concentration of the interferent j in the cal gas used to adjust the analyser
- $S_{Int,p}$ is the sum of interferences with positive impact
- $S_{Int,n}$ is the sum of interferences with negative impact

Combined uncertainty

$$u(C_{ppm}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2}$$

$$\text{Overall expanded uncertainty (k = 2)} \quad U(C_m) = u(C_m) \times k$$

Uncertainty of NOx measurements

$$u(C_{NOx,conv}) = \frac{C_{NOx} \times R \times \eta}{\sqrt{3}} \quad \text{Where: } C_{NOx} \text{ is the concentration of NOx measured by the analyser}$$

- R is the ratio of NO:Nox in the stack gas
- η is the NOx converter efficiency

Combined uncertainty NOx measurements

$$u(C_{NOx,stack}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + u^2(Corr_{NOx,conv})}$$

Uncertainty of mass concentration at oxygen reference concentration

$$u(C_{O_2,ref}) = \sqrt{u^2(Corr_{fit}) + u^2(Corr_{0,dr}) + u^2(Corr_{s,dr}) + u^2(Corr_{rep}) + u^2(Corr_{s,vf}) + u^2(Corr_{a,press}) + u^2(Corr_{temp}) + u^2(Corr_{volt}) + u^2(Corr_{adj}) + S_{Int}^2 + \left(\frac{u^2(O_{2,meas,dry})}{(21 - O_{2,meas,dry})^2} \right)}$$

Where:

$u(C_{O_2,ref})$	=	uncertainty associated with the mass concentration at O ₂ ref. concentration	in	mg/m ³
$C_{O_2,ref}$	=	mass concentration at O ₂ reference concentration	in	mg/m ³
$O_{2,meas}$	=	O ₂ measured concentration	in	% volume
$u((O_{2,meas})_{dry})$	=	uncertainty associated to the measured O ₂ concentration	in	% (relative to O ₂ meas)

APPENDIX 4

Uncertainty Estimate For The Measurement Of Total Organic Carbon

Analysers Type/Model
Reference Oxygen %

Sick Maihak
0 (0 = No correction)

		Test 1	Test 2	Test 3
Limit value	mg/m ³	75	75	75
Limit value	ppm	46.7	46.7	46.7
Measured concentration	ppm	3.2	5.1	8.2
Measured concentration	mg/m ³	5.1	8.2	13.1

Calibration gas	ppm	76.6	76.6	76.6
Calibration gas	mg/m ³	123.1	123.1	123.1
Analysers range	ppm	9.3	9.3	9.3
Analysers range	mg/m ³	15.0	15.0	15.0

Correction of Lack of Fit				
Lack of fit	% range	2.0	2.0	2.0
	u(Corr _{fit})	0.11	0.11	0.11

Corrections of Zero and Span Drift (*All drift is calculated for ∴ the residual is assumed to be < 5% u(max))				
Zero Drift	% range	0.00	0.00	0.00
	u(Corr _{zero})	0.00	0.00	0.00
Span Drift	% range	0.00	0.00	0.00
	u(Corr _{span})	0.00	0.00	0.00

Correction of Repeatability of Measurement				
Repeatability SD at span level (Not reported)	% range	0.0	0.0	0.0
	u(Corr _{rep})	0.00	0.00	0.00

Correction of adjustment				
losses in the line	% range	1.31	1.31	1.31
	u(Corr _{loss})	0.02	0.04	0.06
Uncertainty of calibration gas	% range	2.0	2.0	2.0
	u(Corr _{cal})	0.03	0.05	0.08

Correction of Influence of Interferents				
N ₂ O	% range			
	u(Corr _{N2O})	0.00	0.00	0.00
CO ₂	% range			
	u(Corr _{CO2})	0.00	0.00	0.00
CH ₄	% range			
	u(Corr _{CH4})	0.00	0.00	0.00
Total of interferent influences	% range	2.50	2.50	2.50
u(ΣCorr _{int}) = max[S _{int,1} ; S _{int,2}]	u(ΣCorr _{int})	0.16	0.16	0.16

Correction of Influence Quantities				
Sensitivity to sample volume flow	% range	1.60	1.60	1.60
	u(Corr _{vol})	0.09	0.09	0.09
Sensitivity to atmospheric pressure (Not reported)	% range			
	u(Corr _{press})	0.00	0.00	0.00
Sensitivity to ambient temperature	% range	-2.40	-2.40	-2.40
	u(Corr _{temp})	-0.28	-0.28	-0.28
Sensitivity to electrical voltage (Not reported)	% range	0.50	0.50	0.50
	u(Corr _{volt})	0.10	0.10	0.10

Maximum standard uncertainty	u(Corr _{max})	0.11	0.11	0.11
5% of maximum standard uncertainty	u(Corr _{5%})	0.01	0.01	0.01

Interferent Concentration Variations	Minimum	Maximum	Value at cal	Performance	Units
CH ₄ range	0	10	0	50	mg/m ³
N ₂ O range	0	0	0	20	mg/m ³
CO ₂ range	8	12	0	15	mg/m ³
Oxygen effect variations	Minimum	Maximum	Value at cal	Performance	Units
Oxygen effect	0	20	0	2	mg/m ³

Influence Quantity Variations	Minimum	Maximum	Value at cal	Performance	Units
Sensitivity to sample volume flow	55	65	60	5	l/h
Sensitivity to atmospheric pressure	99	100	99	1	kPa
Sensitivity to ambient temperature	278	313	288	10	K
Sensitivity to electrical voltage	187	250	230	5	V

Measurement uncertainty				
Combined uncertainty	ppm	0.37	0.37	0.38
Combined uncertainty	mg/m ³	0.59	0.60	0.61

Expanded uncertainty expressed with a level of confidence of 95%, k=2

Overall uncertainty	ppm	0.7	0.7	0.8
Overall uncertainty	mg/m ³	1.2	1.2	1.2
Overall uncertainty relative to measured value	%	23.2	14.6	9.3
Overall uncertainty relative to range	%	7.9	7.9	8.1
Overall uncertainty relative to ELV	%	1.0	1.0	1.0

The uncertainty evaluation has been carried out in accordance with UKAS requirements.