

GRINDLE HOUSE,  
CHURCH LANE,  
CLYST ST MARY,  
EXETER, DEVON EX5 1AB  
TEL 01392 877770  
FAX 01392 874041



**PARTICULATE EMISSION MONITORING  
AGGREGATE INDUSTRIES UK LTD.  
BARDON CONTRACTING  
SITE AT AVEN INDUSTRIAL PARK  
MALTBY  
SOUTH YORKSHIRE**



REPORT ON PARTICULATE EMISSION MONITORING

to

DETERMINE THE LEVELS OF PARTICULATE EMISSION

from the

HOT ASPHALT RECYCLER

at

AGGREGATE INDUSTRIES UK LTD.  
BARDON CONTRACTING  
SITE AT AVEN INDUSTRIAL PARK  
MALTBY  
SOUTH YORKSHIRE

**Report Submitted To:**

AGGREGATE INDUSTRIES UK LTD.  
BARDON CONTRACTING  
SITE AT AVEN INDUSTRIAL PARK  
MALTBY  
SOUTH YORKSHIRE

**Report Prepared by:**

K Gough  
Company Principal

A Yelland  
Associate

Date: 18.04.12



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## SUMMARY INFORMATION

| Determined                      | Units              | Results | Limit |
|---------------------------------|--------------------|---------|-------|
| Particulate Concentration (STP) | mg/m <sup>3</sup>  | 9.2     | 50    |
| Mass Emission (STP)             | kg/hr              | 0.04    | -     |
| Stack Temperature               | °C                 | 255     | -     |
| Gas Velocity                    | m/s                | 29.82   | -     |
| Stack Volume Flow Rate (Actual) | m <sup>3</sup> /hr | 7339    | -     |
| Stack Volume Flow Rate (STP)    | m <sup>3</sup> /hr | 3830    | -     |

All results are reported at reference conditions of 273K, 101.3kPa, wet gas.



## **1. INTRODUCTION**

On 18 April 2012, particulate emission testing was undertaken by Advance Environmental, on the hot asphalt recycling plant at Aggregate Industries UK Limited, Maltby.

The purpose of the emission testing was to ensure compliance with the requirements of the permit issued by the Local Authority under The Environmental Permitting (England and Wales) Regulations 2010.



## **2. BACKGROUND INFORMATION**

The environmental Permitting (England and Wales) Regulations 2010 (EPR), came into force on 6 April 2010. The regulations combine Pollution Prevention and Control and Waste Management Licensing.

Environmental Permits automatically replaced previously issued Pollution Prevention and Control permits (PPC) permits with effect from April 2010. As with PPC permits, to continue operations, all sites operating scheduled processes must obtain an EPA permit from their Local Authority and comply with the conditions contained therein. The conditions will include a requirement to monitor emissions to air both periodically and continuously in accordance with relevant clauses of following process guidance note:-

\* Process Guidance Note PG3/15a(04) Secretary of State's Guidance for Roadstone Coating Processes.



### **3. MONITORING CONTRACTOR**

The emission monitoring was co-ordinated by Mr K Gough, Company Principal, Advance Environmental. Mr Gough has 22 years experience of undertaking particulate emission testing on plant used in the quarrying and allied industries.

The lead engineer managing the on site testing is MCERTS Level 2 accredited.



## **4. MONITORING PROTOCOL**

### **4.1 Test Method and references**

Isokinetic sampling of the contained emission sources was undertaken using the APEX Instruments Inc Method Five isokinetic sampling apparatus in accordance with the main procedural requirements within the following British Standards and Technical Guidance Notes:-

- \* BS ISO 9096:2003 - Stationary source emissions. Manual Determination of mass concentration of particulate matter.
- \* Environment Agency - Technical Guidance Document (Monitoring) M1 Sampling requirements for monitoring stack emissions to air from industrial installations; and
- \* Environment Agency - Technical Guidance Document (Monitoring) M2 Monitoring of Stack Emissions to Air.

### **4.2 Sampling Procedure**

The work carried out was, as far as was reasonably practical, in accordance with BS ISO 9096.

Isokinetic flow means that sample gases laden with particulates are drawn off at the same velocity as the free stream velocity in the flue. Isokinetic sampling thus avoids possible inertial effects of particulates approaching the vicinity of the inlet nozzle which may result in significant error.

The Apex Instruments test equipment was designed to meet the sampling requirements of US EPA Method 5 and with a modified nozzle design, meets the sampling requirements of BS ISO 9096.





The principle of the standard is to draw a known volume of dust laden gas isokinetically through a filter. The weight gain on the filter, after sampling, divided by the gas sample volume equates to the particulate concentration, which in turn can be used to calculate a mass emission.

### 4.3 Sampling equipment

The test equipment is inspected prior to use and its calibration status observed. This includes:-

- \* *Pitot Tube* - All pitot tubes are checked for damage, alignment and that there are no blockages;
- \* *Manometer* - Check of oil levels, connectors and orientation level;
- \* *Thermocouple* - Temperature is measured using k type thermocouples. Each thermocouple is inspected for calibration and damage. Digital temperature meters are used in conjunction with k type thermocouples which are also checked for calibration dates;
- \* *Gas meter* - The calibration of the gas meter is checked before and after sampling using a critical orifice.
- \* *Nozzles* - All nozzles used have been constructed in accordance with BS ISO 9096. Each nozzle is checked for damaged and measured using a vernier caliper on at least 3 planes. Non conforming nozzles will be rejected.
- \* *Balance* - A Mettler Toledo balance is used to weigh filters. It is calibrated yearly by the manufacturer and checked daily by in-house weights.
- \* *Filters* - Pall quartz membrane filters with a collection efficiency of >99.5% at 0.3microns.



## **4.4 Preparation for sampling**

### **4.4.1 Filter Preparation**

Filters are pre-conditioned before arrival on site. The filters are dried in an oven at 180°C for a period of at least one hour and then placed to cool in a dessicator for at least four hours. The filters are then weighed on a five figure balance and placed in individual transport containers. Spare Filters are prepared to obtain blank values.

### **4.4.2 Sampling Location**

No site visit was undertaken prior to undertaking the sampling procedure, as monitoring had previously been undertaken at the site, during which time the sampling position, working platform, sampling ports, access and safety precautions were found to be satisfactory.

The internal dimension of the flue was known from previous monitoring undertaken. However, further measurements were taken to check that the internal diameter had not changed.

Prior to sampling a pressure and temperature survey, using a pitot static tube, a micromanometer, a digital thermometer and a nickel-chromium/nickel-aluminium thermocouple, is carried out to check whether the flow conditions meet with the requirements of BS ISO 9096. From this initial survey sample locations, isokinetic flow rates, nozzle size, and sample period can be worked out.

## **4.5 Sample Collection**

A leak check is carried out before and after sampling to confirm all the suction is drawn through the nozzle.



With the required isokinetic flow rates known the sample probe is inserted into the stack at 90° to the gas flow, this is to stop any particulate matter impinging on the filter before

The filter head and probe were allowed to obtain the stack gas temperature.

The initial gas meter reading was noted and the suction device and timer started. The correct flow rate for isokinetic sampling was set and the nozzle positioned to face parallel to the gas flow.

Sampling was then carried out for the planned duration and number of sample points, recording all the necessary data for final calculations. On completion, the suction device and timer were stopped and the final gas meter volume recorded.

The probe was removed from the process stack and a further leak test carried out prior to removal of the filter, which was subsequently removed and placed in a storage container.

Any residual particulates upstream of the filter was washed with acetone into an appropriate beaker.

At all times during the sampling procedure the sampling technicians were in contact with the process operator to ensure that the plant was in full production and there were no changes in the process that might affect the representative nature of the samples collected.

#### **4.6 Analysis of samples**

On returning to the laboratory, the used filters were dried in an oven at 160°C for a minimum of one hour and then desiccated and weighed as before. The water/acetone washings are first evaporated, without boiling, then dried and weighed as above. The total particulate mass is the sum of the differential filter weight added to the differential water/acetone rinsings component.



#### **4.7 Calculation of results**

The calculations were made using the formula specified in BS ISO 9096.

The recorded filter weights, velocity, temperature, sampling duration and internal flue dimensions were then used to calculate:-

- \* the mass rate of solids emission in kg/hr; and
- \* the solids concentration in  $\text{mg/m}^3$ .

#### **4.8 Sampling Results**

A particulate emission test was carried out, under continuous operating conditions, to assess the emission concentration in the exhaust gases. The sample time of the test was 32 minutes.

At the time of sampling, a particulate matter of  $9.2\text{mg/m}^3$  at reference conditions was measured. It can be concluded, therefore, that the emission from this plant was found to comply with the emission limit currently imposed.

#### **4.9 Comments**

Full test data demonstrating procedural compliance with BS ISO 9096 for total particulate monitoring is provided in following sections.



## **5. SAMPLING RECORDS**



## 5.1 Process Conditions

|                      |                                       |
|----------------------|---------------------------------------|
| Arrestment Plant:    | None                                  |
| Particulate Type:    | Sand                                  |
| Plant Loading:       | 10 tonne batch process @ 40mins/batch |
| Appearance of plume: | Steam                                 |



## 5.2 Sampling Results

|  |                 |
|--|-----------------|
|  | Test Run No. 1. |
| Time of Test:  | 11.05 - 11.37   |
| Sampling Duration:<br>(mins)   | 32              |
| Gas Temperature<br>(°C)  | 255             |
| Mean Velocity at<br>Sampling Points: (m/s)                           | 31.23           |
| Gas Flow Rate<br>at STP (1): (m <sup>3</sup> /min)                   | 65.0            |
| Particulate Loading<br>at STP (1): (mg/m <sup>3</sup> )              | 9.22            |
| Particulate at<br>Normalised Conditions<br>(2): (mg/m <sup>3</sup> ) | -----           |

(1) Particulate stated at 273K, 101.3kPa without correction for water vapour.

(2) State normalised conditions (eg 11% O<sub>2</sub>, etc).



### 5.3 - Calculations Sample Run No. 1

#### On-site measurements

$$\begin{aligned} \text{O}_2 &= 13.4 \% & \text{CO}_2 &= 4.2 \% & \text{N}_2 &= 82.4 \% \\ \text{Bws} &= 0.04 & \text{Ps} &= 102.3 \text{ kPa} & \text{Ts} &= 528.0 \text{ K} \\ \text{Md} &= \text{Molecular weight of gas at DGM (g/g mole)} \\ \text{Md} &= (0.44 \times \% \text{CO}_2) + (0.32 \times \% \text{O}_2) + (0.28 \times \% \text{N}_2) \\ &= 29.21 \text{ g/g mole} \\ \text{Ms} &= \text{Molecular weight of gas wet (g/g mole)} \\ &= 28.76 \text{ g/g mole} \end{aligned}$$

#### Stack gas velocity at sample points

$$\begin{aligned} V &= K_p \times C_p \times \ddot{O}(\text{Ts.DP/Ps.Ms}) \\ &= 31.23 \text{ m/s} \end{aligned}$$
$$\begin{aligned} K_p &= 4.07 \\ \text{DP} &= 330.0 \text{ av. Dp at sample plane} \\ C_p &= 1.00 \text{ pitot tube coefficient} \end{aligned}$$

#### Stack gas volume at sample points

$$\begin{aligned} Q &= V \times A \times 60 \\ &= 128.1 \text{ m}^3/\text{min} \end{aligned}$$
$$A = 0.07 \text{ area of stack m}^2$$

#### Volume of water vapour collected, standard conditions (m<sup>3</sup>)

$$\begin{aligned} \text{Vwstd} &= 0.00124 \times \text{Vlc} \\ &= 0.0177 \text{ m}^3 \end{aligned}$$
$$\text{Vlc} = 14 \text{ ml}$$

#### Volume of gas metered, standard conditions (m<sup>3</sup>)

$$\begin{aligned} \text{Vmstd} &= \frac{2.695 \times \text{Vm} \times (\text{Pa} + (\text{DH}/102)) \times \text{Yd}}{(\text{T} + \text{Tm})} \\ &= 0.6117 \text{ m}^3 \end{aligned}$$
$$\begin{aligned} \text{Tm} &= 8 \text{ }^\circ\text{C} \\ \text{Vm} &= 0.6217 \text{ m}^3 \\ \text{Pa} &= 102.10 \text{ kPa} \\ \text{DH} &= 38.7 \text{ mm H}_2\text{O} \\ \text{Yd} &= 1.001 \end{aligned}$$

#### Moisture content

$$\begin{aligned} \text{Bwo} &= \text{Vwstd}/(\text{Vwstd} + \text{Vmstd}) \\ &= 0.0282 \end{aligned}$$

#### Dry total flow of stack gas, standard conditions (m<sup>3</sup>/min)

$$\begin{aligned} \text{Qstd} &= \frac{Q \times \text{Ps}(2.695)(1 - \text{Bwo})}{\text{Ts} + 273} \\ &= 65 \text{ m}^3/\text{min} \end{aligned}$$
$$\begin{aligned} \text{Ts} &= 255.0 \text{ }^\circ\text{C} \\ \text{Ps} &= 102.3 \text{ kPa} \end{aligned}$$

#### Percent isokinetic

$$\begin{aligned} \%I &= \frac{(6.184 \times 10^5)(\text{Ts} + 273) \times \text{Vmstd}}{\text{Ps} \times V \times \text{Aa} \times t \times (1 - \text{Bwo})} \\ &= 102.4 \% \end{aligned}$$
$$\text{Aa} = 19.6 \text{ area of nozzle m}^2$$





### 5.3 - Calculations Sample Run No. 1 Cont.

#### Filter & rinsing weights sample no. 1

weight gain on filters = 5.64 mg  
weight of acetone wash = mg  
total weight gain (M) = 5.64 mg

#### Particulate concentration (mg/m<sup>3</sup>)

$$\begin{aligned} C &= M/V_{mstd} \\ &= 9.22 \text{ mg/m}^3 \end{aligned}$$

$$M = 5.64 \text{ mg}$$

#### Particulate emission rate (kg/hr)

$$\begin{aligned} E &= (C \times Q_{std} \times 60)/1000 \\ &= 0.04 \text{ kg/hr} \end{aligned}$$



## 5.4 - Sample Blank

An overall sample blank was taken after the measurement series, following the sampling procedure in the methodology without starting the suction device and keeping the blank in the duct for 15 minutes with the sampling nozzle 180° from the direction of flow. This leads to an estimation of the dispersion of results related to the whole procedure.

weight gain on filters = 0.00003 mg  
weight of acetone wash = mg  
total weight gain (M) = 0.00003 mg

### Particulate concentration (mg/m<sup>3</sup>)

$$\begin{aligned} C &= M/V_{mstd} \\ &= 0.05 \text{ mg/m}^3 \end{aligned}$$

$$M = 0.03 \text{ mg}$$



## 5.5 - On Site Velocity and Flow Data

|           |                              |                        |       |                |
|-----------|------------------------------|------------------------|-------|----------------|
| Company   | AGGREGATE INDUSTRIES UK LTD. | Stack Diameter         | 0.30  | m              |
| Site      | BARDON CONTRACTING           | Area                   | 0.07  | m <sup>2</sup> |
| Location  | HOT ASPHALT RECYCLER         | Barometric Pressure    | 102.1 | kPa            |
| Job No    | 439                          | Stack Pressure         | 0.16  | kPa            |
| Operators | AJY/MJR                      | Pitot Tube Coefficient | 0.997 |                |

| Preliminary readings taken before sampling |           |            |           |            |
|--|-----------|------------|-----------|------------|
| Pitot Traverse B                           |           |            |           |            |
| Pitot Settings                             | D P<br>pa | Temp<br>°C | D P<br>pa | Temp<br>°C |
| 1  | 98        | 255        | 98        | 255        |
| 2  | 132       | 255        | 132       | 255        |
| 3  | 187       | 255        | 187       | 255        |
| 4  | 201       | 255        | 201       | 255        |
| 5  | 225       | 255        | 225       | 255        |
| 6  | 289       | 255        | 289       | 255        |
| 7  | 363       | 255        | 363       | 255        |
| 8  | 475       | 255        | 475       | 255        |
| 9  | 584       | 255        | 584       | 255        |
| 10   | 682       | 255        | 682       | 255        |

|   |     |
|---|-----|
| av temp (K)=((average temp traverse A+average temp traverse B)/2)+273 | 528 |
| av press (Pa)=((average press traverse A+average press traverse B)/2) | 324 |

| Suitability of sampling positions & Required No. of sample points | Actual Stack Conditions |
|---|-------------------------|
| Permitted highest to lowest pressure range = 9:1                  | 7.0 : 1                 |
| Negative pressure   | Not permitted           |
| Differential pressure minimum > 5 Pa                              | 98                      |
| No. of sampling points  | 1                       |





## 5.7 - Weighing Results

The below filters and acetone rinsings were weighed on a balance in a temperature

| Sample<br>Run No.1.    | Ref No. | Weight<br>gms |         |           | Sample<br>time at each<br>point (mins) | %<br>weight<br>gain |
|------------------------|---------|---------------|---------|-----------|--|---------------------|
|                        |         | Before        | After   | Collected |  |                     |
| Filter                 | 16      | 0.05447       | 0.06011 | 0.00564   | 32.0                                   | 10.4%               |
| Acetone                |         |               |         |           |  |                     |
| Total weight = 0.00564 |         |               |         |           |  |                     |
| Sample<br>Blank        | Ref No. | Weight<br>gms |         |           | Sample<br>time at each<br>point (mins) |                     |
|                        |         | Before        | After   | Collected |  |                     |
| Filter                 | 17      | 0.05462       | 0.05465 | 0.00003   | n/a                                    | 0.1%                |
| Acetone                |         |               |         |           |  |                     |
| Total weight = 0.00003 |         |               |         |           |  |                     |



## 5.8 - Main conditions for compliance with BS ISO 9096:2003

The following requirements must be met:

### Preliminary Velocity Survey

|  |  | Pass | Fail |
|--|--|------|------|
|  | No negative flow at sampling points                            | *    |      |
|  | Direction of gas flow within 15° of flue axis                  | *    |      |
|  | Pitot-static pressure differential greater than 5 Pa ( 3m/s )  | *    |      |
|  | Ratio of highest to lowest pitot-static readings less than 9:1 | *    |      |

### Sampling procedure

|  |   |   |  |
|--|---|---|--|
|  | Sampling plane was corectly positioned              | * |  |
|  | Sampling centroids of equal area                    | * |  |
|  | Nozzle was facing upstream to within $\pm 10^\circ$ | * |  |
|  | Leak check performed                                | * |  |
|  | Constant 'at' during cumulative sampling            | * |  |

### Post Sampling Operations

|  |                                 |   |  |
|--|---------------------------------|---|--|
|  | Leak test performed             | * |  |
|  | Isokinetic rate 95 % to 115 %   | * |  |
|  | Samples achieved stable weights | * |  |

Note :

A single tick in the "fail" column indicates that this test does not comply with the full provisions of BS ISO 9096:2003. Due to site/sampling locations it is not always practically possible for all the conditions to be met. Best practical means are employed to try and achieve a representative result.

