

Part D

Solvent/Product Analysis: 2012 (Base Data for VOC Calculation)

Solvent Analysis

Solvent	Op. Bal.	Receipts	Cl. Bal.	Usage		
ACETONE	2069	8538	3494	7113		
ISOPROPANOL	1356	19700	2881	18175	18541	
N-PROPANOL	150	330	114	367		
HEPTANES	0	6606	0	6606		
HEXANES	26053	105060	2811	128302	2500382	1250191
CYCLOHEXANE	0	5005	1251	3754		
HYDROCARBON	10596	2411090	53359	2368327		
ETHANOL (IMS)	650	2370	119	2901		
TOTAL	40874	2558698	64029	2535543	1,730,963	40.57%

Production Analysis

Production Volume Jan - Dec 2011					
Product	Tanker	IBC	Drum	Poly	Total
SLC 100A	124,280	59,945	2,158,475	-	2,342,700
SLC 160	-	-	925,440	-	925,440
SLC 235	168,520	-	323,680	32	492,232
SLC 239G	-	-	11,020	-	11,020
SLC 9291ES	-	-	72,864	-	72,864
	-	-	-	-	0
SOLV 1E	-	-	8,576	-	8,576
SOLV 3	-	-	1,120	-	1,120
NDF 20/27T DF	-	-	27,650	702	28,352
SP 1427	56,640	160,500	157,320	247	374,707
DL	-	-	571	3,654	4,225
LF	-	-	-	-	-
NW	-	-	1,260	1,920	3,180
CSF	-	-	-	2,090	2,090
DREM	-	-	-	-	-
Total	349,440	220,445	3,687,976	8,645	4,266,506

Vent Measurements: May 14th 2012

Mass Emission is calculated from Ideal Gas Law

mass emission mg/min = ppm x flow rate x molecular weight x P /RT

$n = PV/RT$

V = measured flow rate (m3/min)	
P = 101325 Pa (760 mm Mercury)	101325
T = 293 K	293
R = molar gas constant 8.314 (m3Pa/mol K)	8.314
Molecular weight for solvent = 90	90
R x T	2436.002
P/RxT	41.595

		Solvent Tank to Mixer	Homogenisation Tank to Tank	Mixer to Buk Tank
		ST2 toMM	BT1 to BT4	MM to BT5
Mean ppm	ppm	0.00	5.42	0.74
Flow Volume	m3/min	3.20	3.20	3.20
Emission rate	gm/min	0.00000	0.06501	0.00888
Emission Rate MR	kg/min	0.00000	0.00007	0.00001
Prebalanced Rate (PBR)	kg/min	0.18000	0.18000	0.04400
MR/PBR		0.00000	0.00036	0.00020
Efficiency 1-MR/PBR		1.00000	0.99964	0.99980
EFFICIENCY PERCENT	%	100.000	99.964	99.980

Vent Measurements: October 16th 2012

Mass Emission is calculated from Ideal Gas Law

mass emission mg/min = ppm x flow rate x molecular weight x P /RT

$n = PV/RT$

V = measured flow rate (m3/min)	
P = 101325 Pa (760 mm Mercury)	101325
T = 293 K	293
R = molar gas constant 8.314 (m3Pa/mol K)	8.314
Molecular weight for solvent = 90	90
R x T	2436.002
P/RxT	41.595

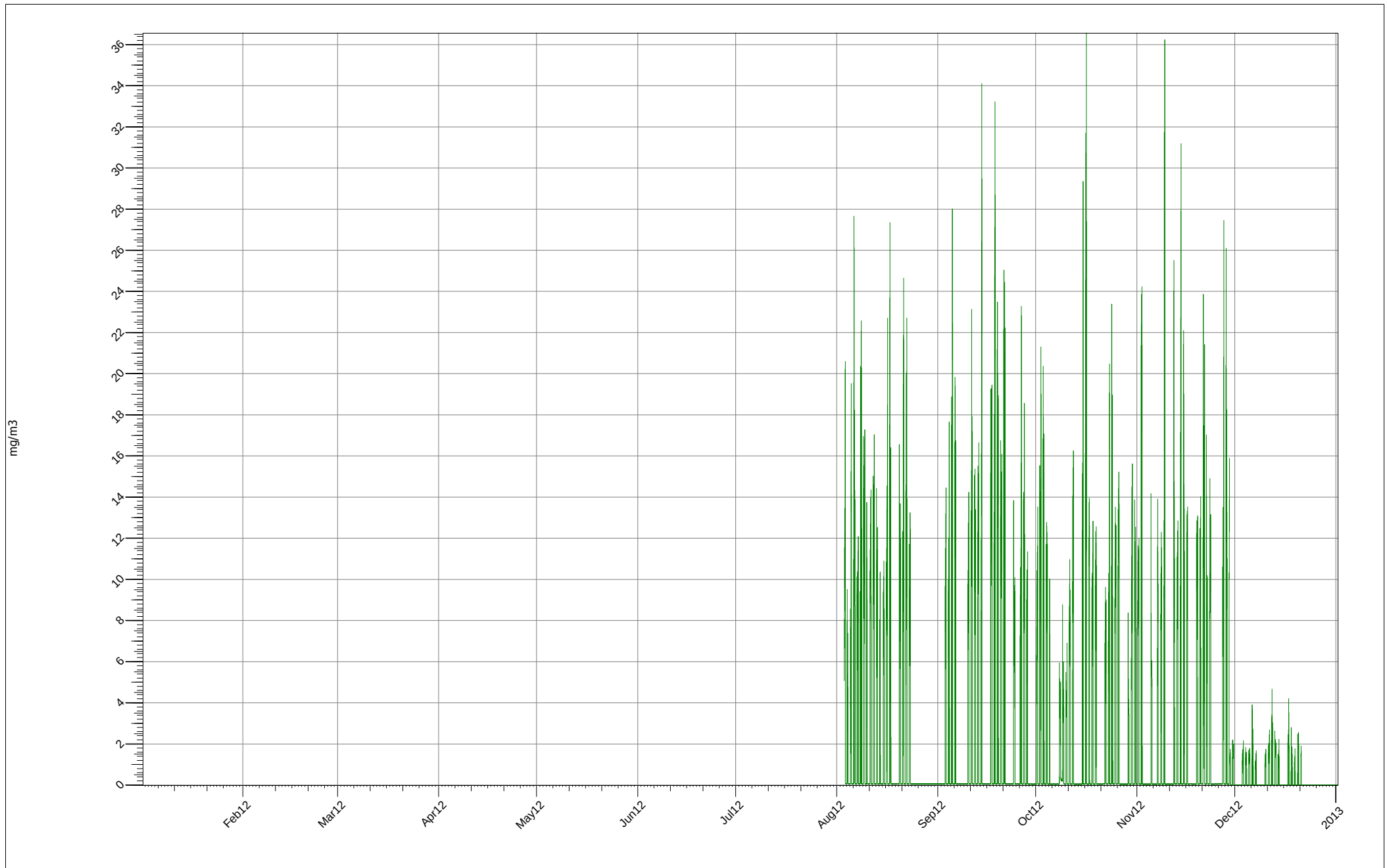
		Solvent Tank to Mixer	Homogenisation Tank to Tank	Mixer to Buk Tank
		ST2 toMM	BT1 to BT4	MM to BT5
Mean ppm	ppm	0.00	0.00	6.49
Flow Volume	m3/min	3.20	3.20	3.20
Emission rate	gm/min	0.00000	0.00000	0.07782
Emission Rate MR	kg/min	0.00000	0.00000	0.00008
Prebalanced Rate (PBR)	kg/min	0.18000	0.18000	0.04400
MR/PBR		0.00000	0.00000	0.00177
Efficiency 1-MR/PBR		1.00000	1.00000	0.99823
EFFICIENCY PERCENT	%	100.000	100.000	99.823

Emission Report

Company:DAREX UK LTD Contact

From:01 Jan 12 09:15:00 To:01 Jan 13 15:15:00

Device 1 : Stack1 Banbury Cal Factor: WARNING CAL FACTOR IS NOT CONSTANT Average:2.110 Averaging Period:15 mins Maximum:36.57



Emission Report

Company:DAREX UK LTD Contact

From:01 Jan 12 09:15:00 To:01 Jan 13 15:15:00

Device 1 : Stack2 Conveyor Cal Factor: 1.00 (constant) Average:0.122 Averaging Period:15 mins Maximum:3.040

