

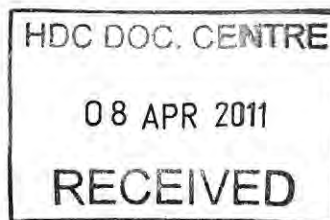


timber engineering specialists

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PE29 3TN

Ref : LA-PPC Compliance Monitoring

6th April 2011



Dear Mr Bass

Further the Emission Monitoring of the Boiler Plant carried out on 11th March 2011, we are pleased to be able to enclose the results.

Yours Sincerely

Simon Wadsworth
Director



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HE 11 / 7839

LA-PPC/EPR Compliance Monitoring

at

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for

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Study Period; - 11th March 2011

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23rd March 2011

FAO: Mr C Franklin - Director

REPORT REF: - HE 11 / 7839

LA-PPC/EPR COMPLIANCE MONITORING OF THE WIESS UNIT AT DAVID SMITH, ST IVES, CAMBRIDGESHIRE.

1.1 INTRODUCTION

This study was undertaken to determine data as detailed by David Smith St Ives Limited's Local Authority Pollution Prevention and Control (LA-PPC/EPR) permit provisions, as defined by Local Authority Environmental Services personnel, to assess the releases sourced from the operation of the site's Weiss wood burning boiler unit.

The report relates to monitoring studies undertaken on 11th March 2011 by Mr T Growcott, BSc (Hons) MRSC C Sci C Chem, of Halcyon Environmental in respect of the determination of Process Guidance Note PG 1/12 defined analytes.

In this study the wood burning unit system was fully operational, burning the wood feed stocks sourced from site manufacturing activities. Monitoring was undertaken continuously over a 3-hour period during which time RanHeat personnel were on site.

The author was formally trained in source testing via Clean Air Engineering (CAe) (1991), Casella (1992) and SGS (1991) and is STA registered (MM 03/314). Monitoring was undertaken over a continuous period to determine the results quoted and in accordance with the following Source Testing Association (STA) codes of practice; -

Document	Title
M 1054	STA Minimum Standards of Testing and Reporting
M 1055	STA Code of Practice
MIG001	Measurement of Specific Organic Compounds in Source Releases
QGN001	Guidance on Assessing Uncertainty in Stack Emission Monitoring



5 ANALYTICAL SEQUENCE AND RESULTS

The monitoring strategy was undertaken over one day.

An ongoing continuous assessment of emission clarity, colour and odour at the point of discharge were also undertaken. At no time during this study was there any indication of colouration by dense black smoke.

Periodic monitoring of O₂, water vapour, CO, SO_x, NO_x and VOC were undertaken.

TPM measurement was undertaken on 2 x 30 minute sampling schedules with the filters located outside of the stack.

5.1 ANALYTICAL RESULTS

Analytical mean result data is detailed below: -

Analyte	Test 1	Test 2	Mean	PG 1/12 Max Limit
1. Carbon Monoxide CO (mg/m ³)	240 samples (60 minutes at 15 second intervals)		246	250
2. TPM (mg/m ³)	159.4 1 x 30 mins sample	147.3 1 x 30 mins sample	153.35	200
3. VOC as C (mg/m ³)	240 samples (60 minutes at 15 second intervals)		6.412	20
4. Oxygen (%)	240 samples (60 minutes at 15 second intervals)		9.91	-
5. Water Vapour (%)	2 x 30 mins sample	2 x 30 mins sample	5.472	-
6. Oxides of Sulphur SO _x (mg/m ³)	240 samples (60 minutes at 15 second intervals)		1.04	-
7. Oxides of Nitrogen NO _x (mg/m ³)	240 samples (60 minutes at 15 second intervals)		78.0	-
8. Formaldehyde (mg/m ³)	1.14 (1 x 30 min sample)	0.72 (1 x 30 min sample)	0.93	-
9 Chlorides (as HCl) (mg/m ³)	1.19 (2 x 30 min sample)	-	1.19	-



2. Emission discharges have been assessed and found to be free from droplets as defined within PG 1/12 note provisions.
3. Flow and mean velocity determinations have established data for the wood burner's stack, which have indicated compliance above specified minimum efflux velocity requirements.

The Weiss unit's stack mean efflux velocity was determined to be 13.08 m/s its discharge temperature.

A copy of this report should be sent to Local Authority within 8 weeks of receipt.

Tim Growcott B Sc (Hons) MRSC C Chem C Sci MIMF
Senior Partner

RANH 7839 LAPPC REP



SECTION 2
SAMPLING AND MONITORING STRATEGIES



2 SAMPLING AND MONITORING STRATEGIES

2.1 SAMPLING STRATEGY

The main sampling and monitoring studies were completed following initial determination of the wood burner unit's stack thermal and flow profiles as detailed in ISO 9096:2003.

The data reported herein was compiled in accordance with the methodologies and procedures detailed in STA approved specifications, in addition to specific GC-MS methodologies and the use of approved Draeger tube methods and procedures.

The data reported herein was determined at the two stack portal locations, using the following instrumentation.

Velocity data was determined using a standard Airflow Developments model PVM 100 electronic micro-manometer, (HE 03-012) used in conjunction with a BS 1042 type 2.1 pitot system (HE 03-045), with in line thermocouple.

Calibrated flow, humidity, temperature and pressure measurement devices were also used in these procedures, using Huger-Sutronics and AGL instrumentation.

This procedure was based on US EPA Method 2, "The Determination of Stack Gas Velocity and Volumetric Flow Rates (Type S Pitot Tubes)", and EPA Method 3B "Gas Analysis for the Determination of Emission Rate Correction Factor or Excess Air".

2.2 SAMPLING EQUIPMENT

Sampling was undertaken using BMS high and low flow pumps as defined in the analytical methodology procedures detailed in the next section of this report.

Samples were obtained using convention Andersen probes located in the stack. These were connected to insulated transfer lines, of less than 0.5 m. length, to minimise condensation losses.

The port sealing system was tested prior to each run, and a leak rate of less than 0.02 % was recorded.

2.2.1 ISO 9096:2003 TOTAL PARTICULATE MATTER DETERMINATION

The procedure employed was that detailed in ISO 9096:2003.

Air was extracted from the main stack isokinetically over 2 x 60 minute sampling periods and via a purpose built stack-sampling train located directly in the duct portals to minimise condensation losses. The filters were retained for gravimetric measurement in post sampling analysis.

2.2.2 BS 12619 VOC DETERMINATION

Both direct reading and post sampling laboratory-based procedures were used to produce the data reported herein. Direct measurements were determined via a sampling train located adjacent to the main stack portals.

Direct reading measurements were made as detailed in BS 12619 using a Signal Instruments 3030PM instrument with FID calibrated for 20 ppm propane in air - ex Air Products.



Indirect measurements were made using composite Activated Charcoal and Tenax adsorption tubes, used in conjunction with low flow pumps.

The tubes were then analysed in laboratory based procedures using Gas Chromatography + Mass Spectroscopy by Halcyon personnel. This analysis detailed the VOC emissions as Carbon residues.

Further procedures were involved in the determination of free Formaldehyde using direct reading Draeger tubes.

2.2.3 GAS COMPONENT DETERMINATIONS

The gaseous components of the emission stream were also determined.

Analyses were undertaken for NO_x, SO_x, CO, CO₂ and Oxygen using a Eurotron series 3000 Professional Combustion Gas Analyser.

This instrument had its own probe system and operated by direct measurement of the stack emissions. These measurements were made via a number of on site analyses within the instrument using comparative assessments against pre conditioned calibrated internal standards.

The instrument had its own gas conditioning system and pre calibrated internal measurement standards.

This instrument was using for direct reading of the transfer duct emissions.

Water (moisture) content was determined in accordance with EPA Method 4 using Halcyon test equipment (HE 09-141).

2.2.4 CHLORIDES (as HCl) DETERMINATION

Total Chloride was determined in accordance with the latest standard method of determination, BS EN 1911-3. This methodology was supplied from the Source Testing Association as the most accurate procedure for the determination of HCl. The method provides procedures for isokinetic sampling, the suggest methodology when particulate matter is anticipated in the emission stream.

The procedure was adhered to in strict accordance with defined methodology other than in the use of a full heated sampling line due to space limitations. The sampling head was determined to be at temperatures in excess of 250 degrees C at the sampling tip, and in excess of 150 degrees C at the filter body. Simultaneous temperature measurements determined that the emission stream temp was in excess of 100 degrees C at the bubbler bottle and not less than 90 degrees C at both sampling pumps.

Chloride analyses were undertaken using the ion exchange chromatography procedure detailed in BS EN 1911-3. This procedure was considered to give identical results to the alternative mercuric thiocyanate methodology, and not have the significant interferences of the silver nitrate potentiometric methodology.

The ion exchange method is the only one of the three options, which also gives indicative distinction of the presence of volatile chlorides, which may be present in the sampling solutions.

Chloride determination was calculated using BS EN 1911 section 4.5 equations.



2.2.5 SAMPLING PROTOCOLS

All sampling and monitoring procedures were based on basic isokinetic sampling strategies, to assess process uniformity, with continuous on line assessment of flow rate and dynamic velocity measurements during unit operation.

All flow rate and velocity measurement instrumentation was calibrated prior to, during and after each sampling run.

All sampling planes and points of determination were corrected in accordance with isokinetic correction Ka coefficients as detailed in Source Testing Association protocols.

Monitoring was based on the Approved 1999 Code of Practice produced by the Source Testing Association.

Calculation of Velocity of Flow:

The basic formula for calculating velocity of flow from velocity pressure is:

$$\text{Velocity Pressure (Pv)} = \frac{1}{2} \rho V^2$$

Where:

Pv is Velocity Pressure in pascals.

ρ is the density of dry air (free of CO₂) at 1013mb, 273K in Kg/m³.

V is velocity in metres per second.

Dry air contains 78.1% Nitrogen (as N₂), 20.9% Oxygen (as O₂), 0.9% Argon (as Ar) and traces of CO₂ (0.03%), Ne, He, Kr, Xe, H₂, CH₄, N₂O, O₃, SO₂, NO₂, NH₃, CO, & I₂.

Atomic Weight of Nitrogen is 14, Oxygen is 16, and Argon is 40. Molecular Weight of Nitrogen (N₂) is 28, Oxygen (O₂) is 32 and Argon (Ar) is 40.

Molar Density of a complex gas mixture, such as air, can be calculated using the proportions of gas present, and the molecular weights of the component gases. Thus using the 3 principle components of dry air:

$$\begin{aligned} \text{Molar gas density} &= 0.781 \times 28 \text{ (for N}_2\text{)} + 0.209 \times 32 \text{ (for O}_2\text{)} + 0.009 \times 40 \text{ (for Ar)} \\ &= 28.916 \end{aligned}$$

When the figures are made more accurate, and all the other trace gases added into the equation, **Molar Gas Density of Air** works out to be **28.9644**. This is normally approximated to 29.

The following calculations can be utilised (in most cases), where molar gas density is in the range of 28-30, (see note on determination of flue gas density).

In some combustion stacks the density can be found to be outside this range, in which case the calculations need to be modified by substituting the actual value into the basic equation, and following the calculation through.

One mole of gas occupies 22.4136 litres at 273 K, 1013mb. (Normally approximated to 22.4). One mole of air occupies the same volume and weighs 28.9644 g. Thus the **Density of Dry Air** at 273 K, 1013 mb works out at 1.292 Kg /m³. The precise figure is 1.2928 Kg/m³.



If this figure is entered into the initial equation

$$P_v = \frac{1}{2} \rho V^2$$

It calculates out to; -

$$\text{Velocity (metres per second)} = 1.244 \sqrt{P_v} \quad (\text{at } 273 \text{ K, } 1013 \text{ mb})$$

or

$$\text{Velocity (metres per second)} = 1.280 \sqrt{P_v} \quad (\text{at ambient: } 289 \text{ K, } 1013 \text{ mb})$$

This equation can be applied at or near standard conditions. Where conditions vary significantly from standard, corrections can be made according to the following formula:

$$V = 1.280 \sqrt{\frac{1013 \times T \times 101300}{P_a \times 289 \times (101300 + P_s)}} \times P_v$$

This equation corrects for atmospheric pressure (Pa), expressed in millibars, Temperature expressed in Kelvin (T), and static pressure in the stack (Ps) in pascals. It multiplies out to give:

$$V = 762.7 \sqrt{\frac{T \times P_v}{P_a (101300 + P_s)}} \times P_v$$

Where:

V	=	Velocity of Flow on metres per second (ms^{-1})	
T	=	Temperature in Kelvin (Kelvin = ° Celsius + 273)	(K)
Pv	=	Velocity Pressure in pascals	(Pa)
Ps	=	Static Pressure in pascals	(Pa)
Pa	=	Atmospheric Pressure in millibars (1 millibars = 100 pascals)	(mb)

To apply this equation, Pv should be entered as the root mean square of all velocity pressure readings. Where the majority of the readings do not vary by more than 25% from the mean figure, the mean provides a satisfactory answer. The equation gives velocity of flow at temperature T, static pressure Ps, and atmospheric pressure Pa.

Measurement of Air Flow in Stacks:

Correct isokinetic sampling is dependent on accurate assessment of air velocity in the duct or flue. Because of the potentially hot, acid conditions found in flues, the instrument of choice for measuring flow is one that measures differential pressure, and does not insert an instrument with electronic or moving parts into the duct. There are several other types of instrument available for measuring airflow, but these should not, as a general rule, be used in flue stacks.

Pressure in Ducts:

There are 4 factors that affect the perceived pressure in a duct:

1. Movement of air produces a measurable Velocity Pressure (also known as Dynamic Pressure).
2. Static Pressure, is exerted in all directions, by the compression, expansion, or heating process that is moving the air.
3. Atmospheric (Barometric) Pressure
4. Temperature.



Micro manometer & Pitot Tube:

The pitot tube is the differential pressure probe, it is designed to create minimal turbulence in the flow. The British Standard design has an ellipsoidal nose, which is inserted to face the flow. The tube is very directional and needs to be accurately aligned into the flow, to produce the best result. Unfortunately the pressure bearing on the nose of the instrument is Velocity Pressure, but with the addition of static pressure.

To eliminate this problem, the pitot tube is made with a separate tapping to measure static pressure alone. The BS tube is made double, with tapings at right angles to the flow, whereas the American S type pitot consists of two separate tubes 180° opposed. The two types of pitot tube have different response factors (sometimes called the K factor), and this may require the use of a correction factor in calculating flow. The response factor for the BS type is 1.0 and for the S type is 0.85.

The original instrument for measuring air pressure is the U tube manometer. By attaching the two tapings of the pitot tube, one to each side of the manometer, Static pressure is applied to both sides, and its effect is eliminated, allowing a direct reading of Velocity pressure. The inclined manometer is an improvement on the U tube, because it allows for more accurate readings of pressure. However it does require careful leveling before use, and an electronic micro manometer is more user friendly.

With either type of instrument it is important that it is connected up with the Velocity pressure tapping bearing on the positive side of the instrument.

Calculating & Presentation of Results (Measurements & Corrections):

Particulate sampling is always assessed gravimetrically (by weight). Filter material of all types is pre weighed, exposed in the sampling line and re-weighed.

This procedure may require drying of the filter medium before re-weighing, if the sampling was conducted at a temperature below the dew point. In all circumstances, filters require careful handling to avoid loss particulate, and also loss of original fibrous material. Weight of particulate collected is thus derived from the difference of the two weights and is normally expressed in milligrams (g^{-3}) or micrograms (g^{-6}). The balance should be calibrated against a traceable standard before and after each batch of filters is weighed / re-weighed.

Volume of gas collected is normally determined either by multiplying sampling flow rate (litres/minute) by time elapsed (minutes) to get a final volume in litres, or by utilising a direct reading from a gas meter.

In both cases, volume calculated is at ambient temperature and pressure and requires correcting to standard conditions. The gas meter or flow meter should be regularly re-calibrated against a traceable standard, and this may impose an extra calibration factor on the results to obtain correct ambient volume.

If the sampling line, does not include a silica gel trap, but only a condensate trap, (as in the BCURA or CEGB Mk111A) the air passing to the meters can be assumed to be water saturated at ambient conditions, and this too required compensation.

Schedule A & B processes require presentation of results in milligrams per cubic metre, and / or parts per million, as standardised to the following conditions:

Temperature	273K (0° Celsius)
Barometric Pressure	101.3KPa, (1013mb)
Humidity	Dry
Oxygen	3%, 6%, 8%, 11%, 15%, 18% depending on combustion process



The various calculations and conversions are explained in the subsequent paragraphs.

Determination of Isokinetic Sampling Rate:

To obtain correct samples of particulates, turbulence caused by sampling must be minimised. This is achieved by making the velocity of flow into the sampling probe equal to the velocity flow moving along the duct or stack. This sampling technique is called isokinetic sampling, and its use enables the collection of representative samples, by eliminating the distortion of sample reliability caused by variation in proportion of light particulates collected.

Velocity of flow is determined by the use of pitot tube and micro manometer. This is normally calculated at the stack temperature. The gas volume measuring equipment is normally functioning at about ambient temperature (Gas moving along the sampling line rapidly cools to ambient).

To calculate isokinetic flow rate, first the gas velocity must be calculated as at ambient. This is done using the standard gas equation (See Calculation of Results).

$$\frac{\text{Pressure} \times \text{Volume}}{\text{Temperature}} = \text{Constant}$$

Thus for a stack of uniform width volume is proportional to velocity, hence:

$$\text{Velocity}_{\text{ambient}} = \frac{\text{pressure}_{\text{stack}} \times \text{Velocity}_{\text{stack}} \times \text{Temperature}_{\text{ambient}}}{\text{Temperature}_{\text{stack}} \times \text{Pressure}_{\text{ambient}}}$$

As atmospheric pressure remains equal this item cancels out of the equation.

Sampling rate (litres per minute) is a function of stack velocity (metres per second) and probe tip area (square centimetres), derived from πr^2 . The rationale is as below:

$$\text{Metres per second (m/s)} \times \frac{100}{60} = \text{centimetres per minute (cm/min)}$$

$$\text{Centimetres per minute (cm/min)} \times \text{Square centimetres (cm}^2\text{)} = \text{Cubic Centimetres per minute (cm}^3\text{/min)}$$

$$\frac{\text{Cubic Centimetres per minute (cm}^3\text{/min)}}{1000} = \text{Litres per minute (l/min)}$$

Thus:

$$\text{Sampling Rate (l/min)} = \frac{\text{Ambient Stack Flow (m/s)} \times \text{Tip area (cm}^2\text{)}}{600}$$

Determination of Flue Gas Density:

Stack gas density is determined by measuring the concentration of Carbon Dioxide, Carbon monoxide and Oxygen in the stack. This can be done using a combustion analyser.

The residual dry atmospheric gas is assumed for the purpose of this calculation to be Nitrogen. Nitrogen concentration is calculated as follows:

$$\% \text{ N}_2 = 100 - (\% \text{ CO}_2 + \% \text{ O}_2 + \% \text{ CO})$$



The proportion of each gas in the dry mixture can then be utilised to calculate the dry molar gas density as shown previously:

$$\text{Molar Dry Gas Density (Dd)} = \left(\frac{\% \text{CO}_2 \times 44}{100} \right) + \left(\frac{\% \text{O}_2 \times 32}{100} \right) + \left(\frac{\% \text{CO} + \% \text{N}_2 \times 28}{100} \right)$$

Flue gases however also contain water. The water is condensed out of the sampling line, (to protect the sampling pump), and is weighted.

The volume of gas occupied by the collected condensate water can be calculated from the volume occupied by 1 mole of standard gas (ie. 22.4 litres at 273K, 1013mb).

$$\text{Gas Phase Volume of Water (litres)} = \text{Weight of Water (grams)} \times \frac{22.4}{28}$$

Dry gas volume of the sample is measured by the gas meter in the sampling line. Total gas volume (wet) collected is therefore the sum of the calculated water volume above and the dry gas volume measured.

$$\text{Total (Wet) Gas Volume} = \text{Dry Gas Volume} + \text{Gas phase Water Volume}$$

Using the above relationship, the proportion of dry gas in the total volume collected, (Mole Fraction of Dry Gas), can be calculated as follows:

$$\text{Mole Fraction of dry gas (Md)} = \frac{\text{Dry gas volume}}{\text{Total gas volume}}$$

Mole fraction of wet gas can be calculated similarly, or as

$$\text{Mole fraction of wet gas (Mw)} = 1 - \text{Mole fraction of dry gas (Md)}$$

Density of stack gas can then be calculated from the density of dry stack gas calculated above, and the Mole Fractions calculated.

Thus:

Molar Density

$$\begin{aligned} & \text{of dry gas (Dd)} \times \text{Mole fraction of dry gas (Md)} + 18 (1 - \text{Md}) \\ & = \text{Molar Stack gas density (Ds)} \end{aligned}$$

This latter equation is identical in methodology to the earlier equation for deriving molar gas density of dry gas, but now includes an extra derived function for water

$$\text{Molar stack gas density (Ds)} = \text{Md} \left(\frac{\% \text{CO}_2 \times 44}{100} + \frac{\% \text{O}_2 \times 32}{100} + \frac{\% \text{N}_2 + \% \text{CO} \times 28}{100} \right) + \text{Mw} \left(\frac{\% \text{H}_2\text{O} \times 18}{100} \right)$$

In most cases the Molar stack gas density will work out as 29 ± 1 . In this case, the normal equation for stack flow will prove to be satisfactory.

Calculation of Volume Flow:

Volume flow is calculated from flow velocity and internal area of the stack or duct as follows:

$$\text{Volume flow (m}^3/\text{min)} = \text{Velocity (ms}^{-1}\text{)} \times \text{Internal Area of Duct (m}^2\text{)} \times 60$$



Internal area of duct is calculated as:

πr^2 for a circular duct,
or base x height for a square duct.

To convert $\text{m}^3\text{min}^{-1}$ to cubic feet per minute (cfm) multiply by 35.315

Oxygen Correction:

The principal behind the oxygen correction is that a complete combustion process would consume all the oxygen, releasing only Carbon Dioxide and Water. Thus the more efficient the combustion process, the less Oxygen is released.

Many processes however function less efficiently than they should, and many others are designed to operate with a large excess of air, or additions of cool air to facilitate the erection of less heat resistant stacks.

The oxygen correction is designed to recalculate the concentration of pollutant gases found, assuming that the process is functioning at a reasonable efficiency for its type.

Thus Gas & Oil fired combustion plant are corrected to 3% O_2 , Coal fired combustion plant at 6% O_2 , Clinical Waste Incinerators at 11% O_2 , and Gas Turbines at 15% O_2 . Other processes may be standardised to other Oxygen concentrations.

Oxygen makes up about 20.9% of normal air; this is used in the correction factor, which is as follows:

$$\text{Corrected Pollutant Concentration (mg/m}^3\text{)} = \frac{(20.9 - \text{Standard O}_2\%) \times \text{Measured Conc}^n}{(20.9 - \text{Measured O}_2\%)}$$

This means that where a combustion process is running more efficiently than required, the correction factor will effectively decrease the final corrected concentration of pollutant. Conversely, where the process is inefficient, the Oxygen correction can dramatically increase the final result.

The correction is only used in combustion processes, and is applied identically to all pollutant gases and particles.

Conversion Factors (mg/m^3 and ppm):

Final results of particulate concentrations in air are always presented as a weight by volume measure (e.g. milligrams per cubic metre).

Gases can be presented as a weight by volume, or as a volume measure (parts per million). Unfortunately, there is no standard methodology within the Process Guidance notes and both types of measure are used, often in the same note. It is thus, important to be able to change between the two methods of calculating gas concentration.

Hydrogen chloride will be used to illustrate the two methods as follows:

Hydrogen chloride has molecular weight of 36.5. 1 mole of HCl occupies 22.4 litres at s.t.p. 1 milli-mole of HCl occupies 22.4 millilitres at s.t.p. 1 millimole weighs 36.5 milligrams.

If 1 millimole of HCl is dispersed in 1 cubic metre of air then this is a concentration of 36.5 milligrams per cubic metre (mg/m^3) or 22.4 millimetres per cubic metre (parts per million) ppm.

So for HCl $36.5 \text{ mg/m}^3 = 22.4 \text{ ppm}$



Specifically for HCl $\text{ppm} \times \frac{36.5}{22.4} = \text{mg/m}^3$

In general $\text{ppm} \times \frac{\text{molecular weight}}{22.4} = \text{mg/m}^3$ at standard conditions
(273 K, 1013mb)

The concept of parts per million is particularly useful, because gas volumes expand and contract with temperature and pressure. Because all gases occupy the same volume, ppm does not change with temperature.

Thus a gas concentration recorded in ppm at high temperature, is still the same at low temperature, and at standard conditions, allowing a direct conversion to mg/m^3 without the worry of changing volumes.

In the case of Nitric Oxide (NO) and Nitrogen Dioxide (NO₂), NO exists at high temperature, as a breakdown product of NO₂. When combined emissions are released to atmosphere, the NO cools and re-oxidises to form NO₂. Thus the PG notes required presentation of Nitrogen oxides (NO_x) to be combined and expressed as NO₂.

Because both gases occupy the same volume the ppm concentrations can be directly added such that:

$$\text{ppm NO} + \text{ppm NO}_2 = \text{ppm NO}_x \text{ (as NO}_2\text{)}$$

The combined NO_x concentration as NO₂ can then be calculated as above using the molecular weight of NO₂ as the basis for the calculation.

Occasionally (for example in Occupational Hygiene applications), the conversion equation is presented as:

$$\text{mg/m}^3 = \text{ppm} \times \frac{\text{molecular weight}}{24}$$

This allows for the fact that 1 mole of gas at 20°C, 1013 mb, occupies 24 litres, and is correct for use at ambient conditions. It is not correct to use this equation at standard conditions.

Temperature and Pressure:

Assuming that stack gases obey the standard Gas Laws, then:

$$\frac{\text{Atmospheric Pressure (mb)} \times \text{Volume (m}^3\text{)}}{\text{Temperature (K)}} = \text{Molar Gas Content}$$

or $\frac{PV}{T} = K$

The Molar Gas Constant equals $8.3143 \text{ J K}^{-1} \text{ mol}^{-1}$

A more useful expression of the Gas Law is:

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$



This can be expressed to find an unknown as; -

$$V_1 = \frac{P_2 V_2}{T_2} \times \frac{T_1}{P_1}$$

The correction equation can therefore be expressed as:

$$\text{Standardised Volume} = \frac{\text{Recorded Pressure} \times \text{Std Temperature (273)} \times \text{Recorded Volume}}{\text{Std Pressure (1013)} \times \text{Recorded Temperature}}$$

For this correction to work, any unit of pressure can be utilised (inches of water, millimetres of mercury, millibars, kilopascals etc.) provided that the standard atmosphere is expressed in similar units. Temperature must however be worked in Absolute Units e.g. Kelvin ($K = ^\circ C + 273.15$) or Rankine ($^{\circ}R = ^\circ F + 459.67$)

2.2.6 INITIAL STACK PROFILE STUDY

As per the provisions ISO 9096:2003, a stack profile study was addressed prior to monitoring and sampling. This study was undertaken at ten points in two transaxial assessments at the sampling portal locations. Both temperature and velocity profiles were measured.

The study determined that the temperature variance across the two measured planes was less than 10 C, and that velocity variances were within method tolerance specification.

(Pre-test measurements determined that the sampling head was less than 10 % of the total stack cross sectional area as detailed in ISO 9096:2003).

2.2.7 CLIMACTIC CONDITIONS

The following climactic conditions were noted during the study; -

Ambient Temperature - K	274.8
Atmospheric Pressure - kPas	101.9
Relative Humidity - %	47
Wind Speed - kph	< 10
Wind Direction	ne
Visibility metres	> 1000
Weather	Bright and clear, becoming cloudy with light rain

2.2.8 QA - QC PROCEDURES

Halcyon operates QA - QC procedures following the guidelines of Halcyon QA.QC Doc 1.

Halcyon is a member of the Source Testing Association.



2.2.9 UNCERTAINTY MEASUREMENTS

Halcyon operates the measurement of uncertainty in accordance with; -

“Guidance on Assessing Uncertainty in Stack Emission Monitoring” Dr.J.Pullen STA Quality Task Group



SECTION 3
ANALYTICAL PROCEDURES



3 ANALYTICAL PROCEDURES AND METHODS

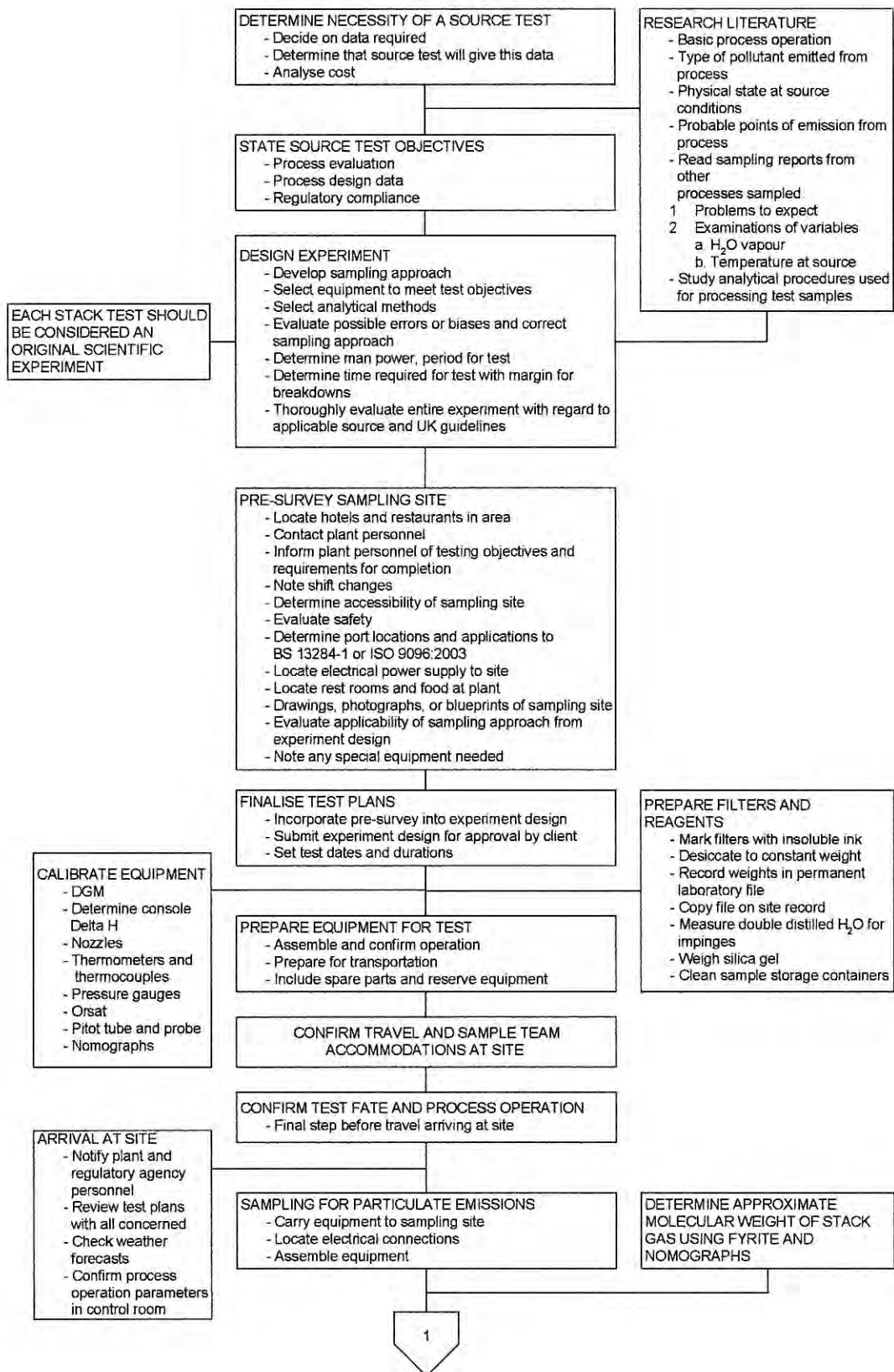
The following analytical methods were used to determine the data reported herein; -

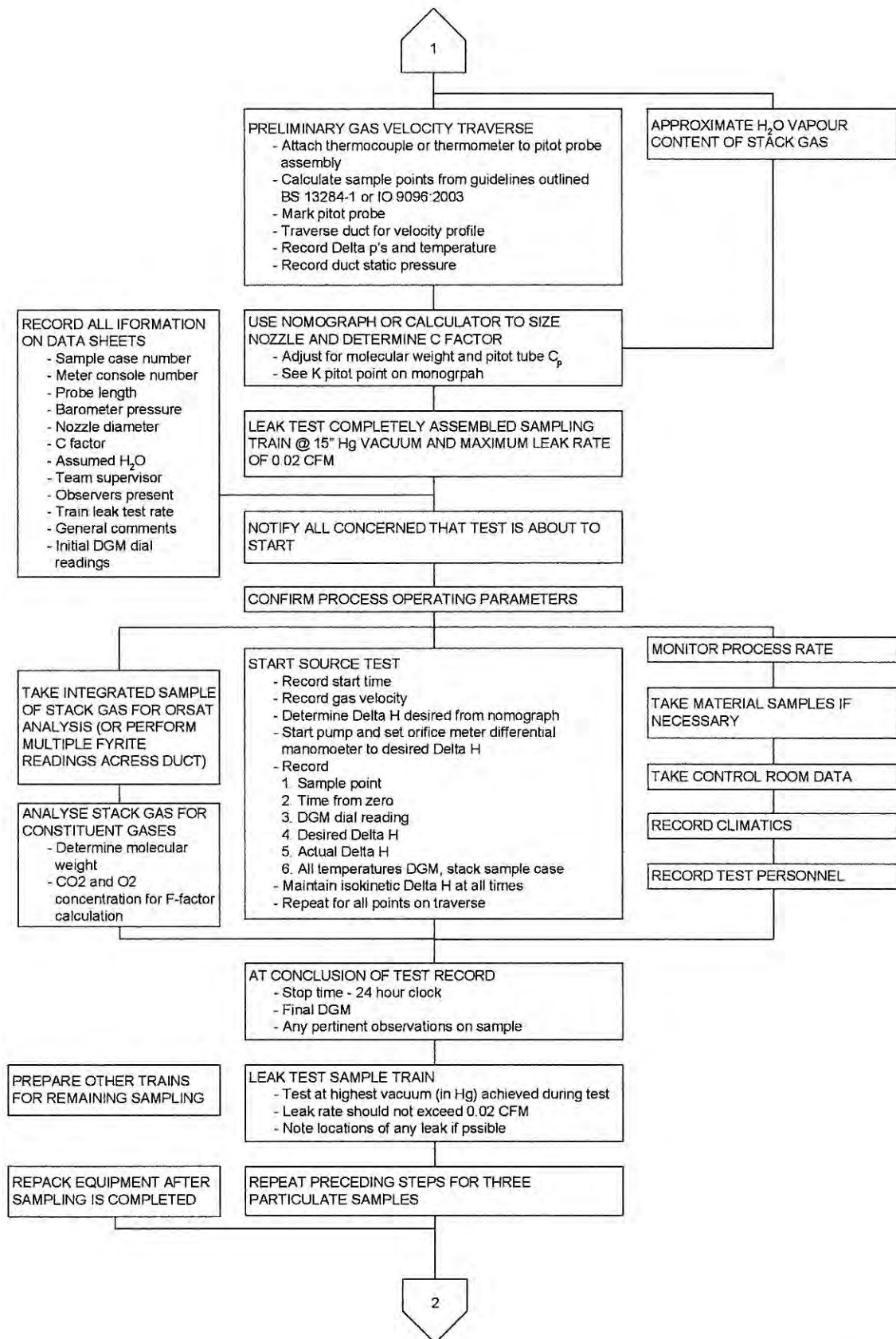
	Analyte	Method Reference
1	CO / CO ₂	**Direct reading EPA Methods 3/3B
2	Total Particulate Matter	ISO 9096:2003
3	VOC	BS 12619
4	VOC as Carbon	BS 12619
5	Water Content	EPA Method 4
6	Oxygen	**Direct reading
7	Free Formaldehyde	Halcyon Test Method HALC.EPA.HCHO 01 Impingers + automated dynamic titrimetry
8	Chlorides	BS 1911-3

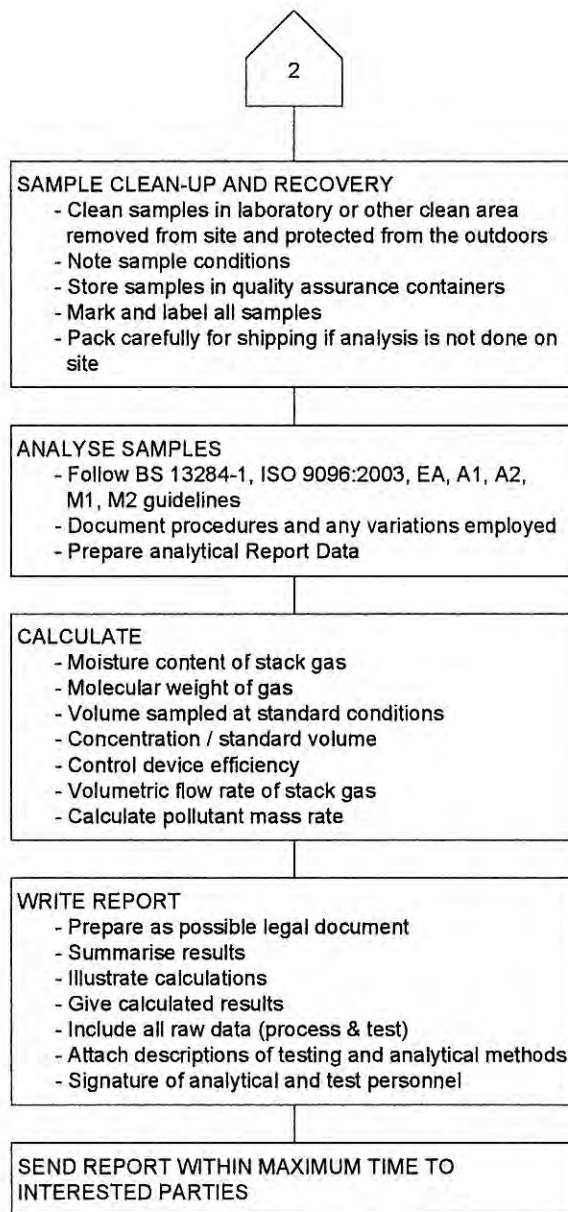
****Eurotron Combustion Gas Analyser instrument**



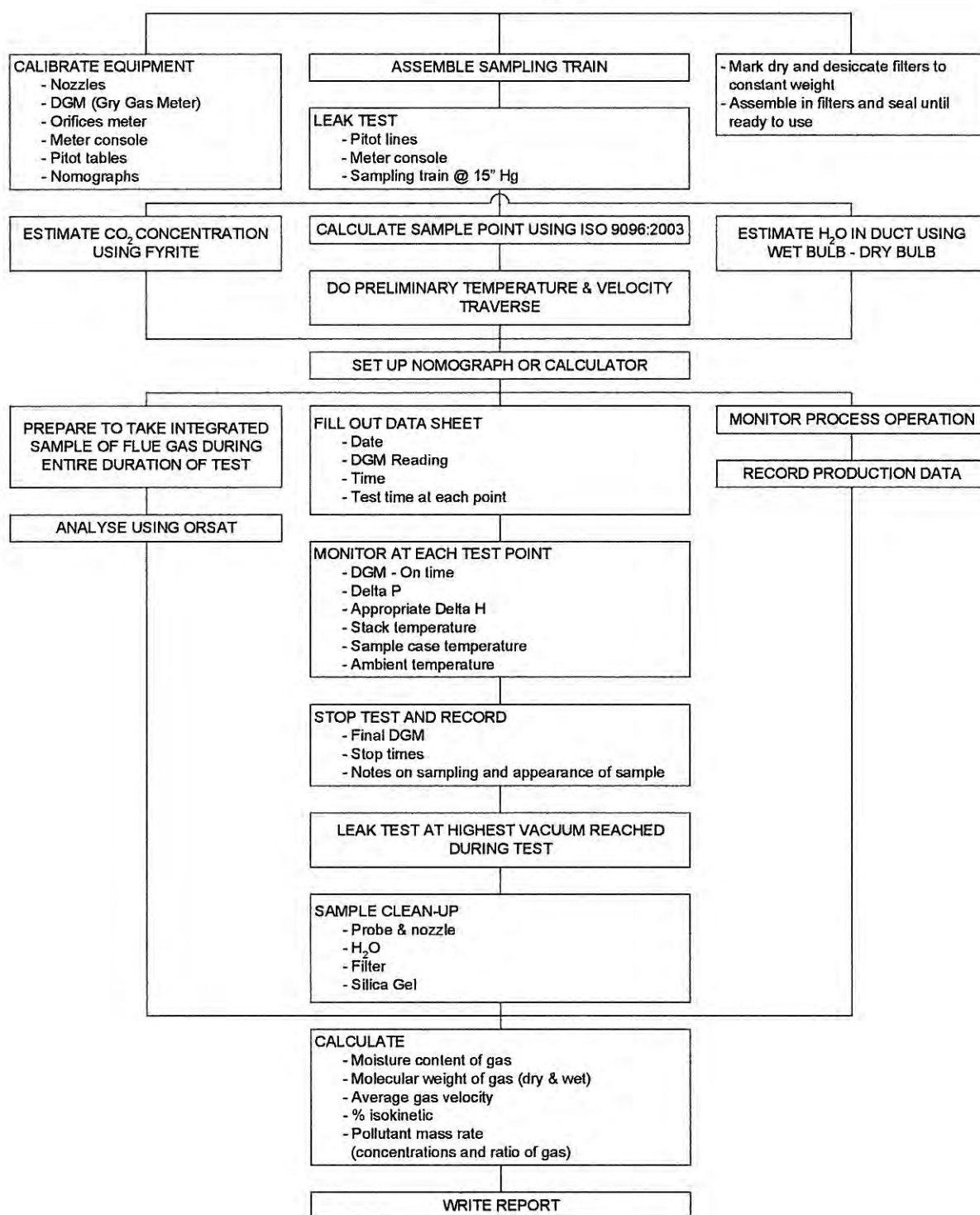
Planning and performing a stack test







Source Test Outline



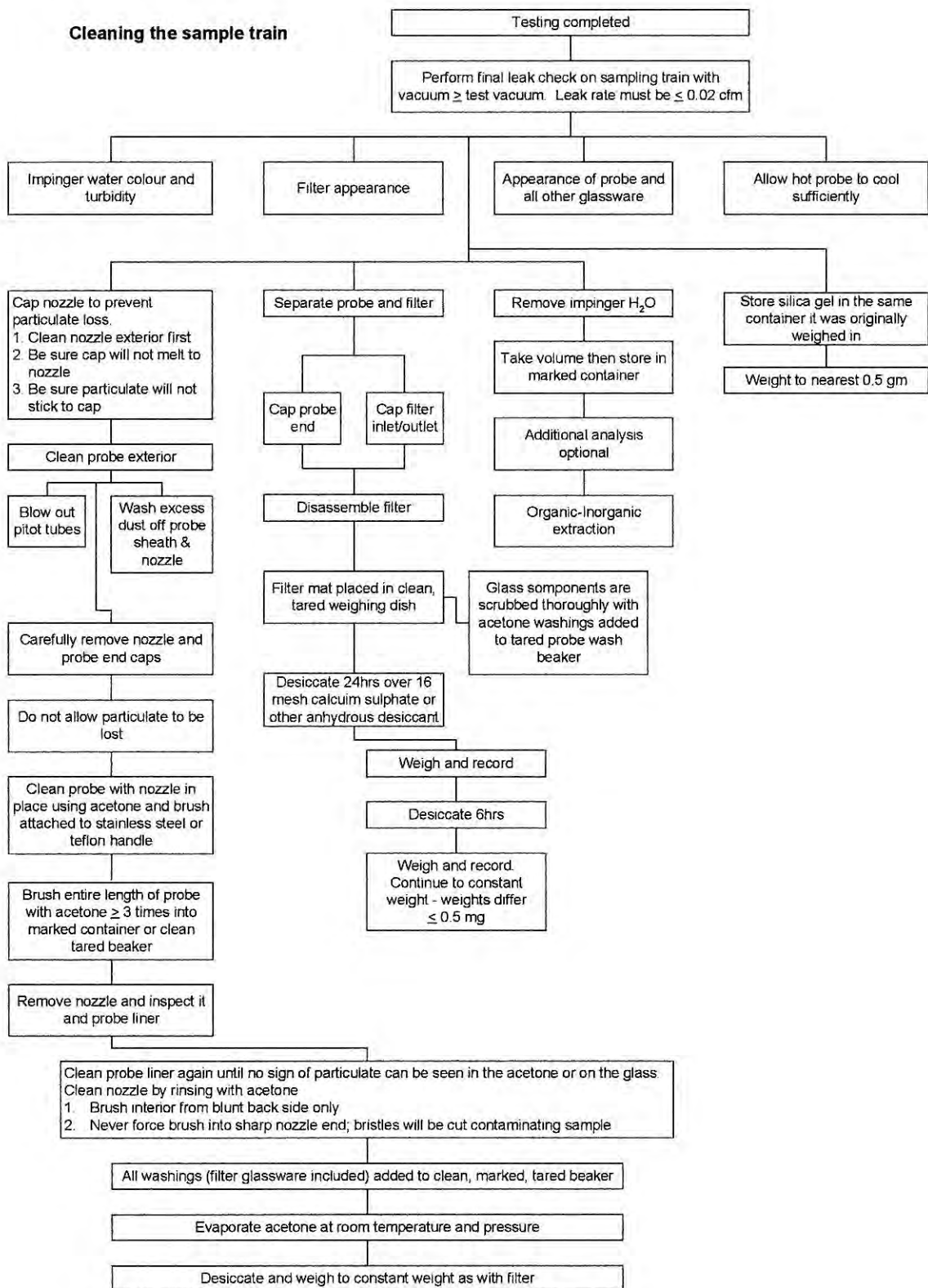


Table 1: Simple error analysis for particulate measurement, 4 Point Sampling (or 10 Point Sampling when Pitot Ratios >4:1≤9:1)

Type of Error	Source of Error	Quoted uncertainty	Estimate of component standard uncertainty (1SD)	Combined uncertainties (1SD)	Combined uncertainty (1SD)	Expanded uncertainty (95% confidence limits)
Precision-like Errors					±13.03%	±25.5%
Random	Errors in setting to isokinetic conditions	≤+1%	≤+0.58%	±4.66%		
	Minimum sampling time of 3 minutes	±8%	±4.62%			
Systematic						
Accuracy-like Errors						
Random	Measure flue dimensions to ±10mm/m	±2%	±1.15%	±1.15%	±13.03%	±25.5%
Systematic	Number of sampling points (see note below)	±13%	±6.63%	±7.22%		
	Minimum weight gain	assume ±2%	±1.5%			
	Pre=/Post-pitot reading within 10%	±2.5%	±1.44%			
	Temperature variations of 10% on 150°C	±1/5%	±0.87%			
	Gas flow axis deviates up to 30°	≤+3.5% velocity	≤+2.02% velocity			

Note: Type A component uncertainty, quoted at 95% confidence limits. All other component uncertainties assumed to be Type B.



Table 2: Simple error analysis for measurement of mass flow particulates when not all the requirements of BS 9096:2003 are met.

Deviation from standard: Only nearest 2 points of 4 on each of sampling lines can be reached (circular duct); pre/post sampling velocities differed by 20%; Highest to lowest pitot reading 15:1.

Type of Error	Source of Error	Quoted uncertainty	Estimate of component standard uncertainty (1SD)	Combined uncertainties (1SD)	Combined uncertainty (1SD)	Expanded uncertainty (95% confidence limits)
Precision-like Errors					+20.7%	+40.8%
Random	Errors in setting to isokinetic conditions	$\leq +1\%$	$\leq +0.58\%$	+4.66%		
	Minimum sampling time of 3 minutes	+8%	+4.62%			
Systematic						
Accuracy-like Errors						
Random	Measure flue dimensions to $\pm 10\text{mm/m}$	$\pm 2\%$	$\pm 1.15\%$	$\pm 1.15\%$		
Systematic	Number of sampling points, and highest:lowest pitot readings 15:1 (see note below)	$\pm (13+12)\%=25\%$	$\pm 12.78\%$	$\pm 14.88\%$		
	Bias due to non-symmetrical points	$\pm 7.5\%$	$\pm 4.33\%$			
	Minimum weight gain	assume $\pm 2\%$	$\pm 1.5\%$			
	Pre/Post-pitot readings differ by 20%	$\pm 10\%$	$\pm 5.77\%$			
	Temperature variation of 10% on 150°C	$\pm 1.5\%$	$\pm 0.87\%$			
	Gas flow axis deviates up to 30°	$\leq +3.5\%$ velocity	$\leq +2.02\%$ velocity			

Note: Type A component uncertainty, quoted at 95% confidence limits. All other component uncertainties assumed to be Type B.



SECTION 4

MEAN EFFLUX VELOCITY DATA



4 FLOW DYNAMICS RESULTS

The following results were determined using the calculations and correction coefficients detailed in ISO 9096:2003.

The following results were determined at the portal locations; -

TABLE 4.1 MEAN EFFLUX VELOCITY RESULTS.		
Sampling Location	Mean Efflux Velocity m/sec @ T	Discharge Temp K
Portal	13.08	427.52

The duct airflow stream temperature was measured continuously using a Casella W1720 thermo - anemometer probe (HE 03-034) in the stack portals.

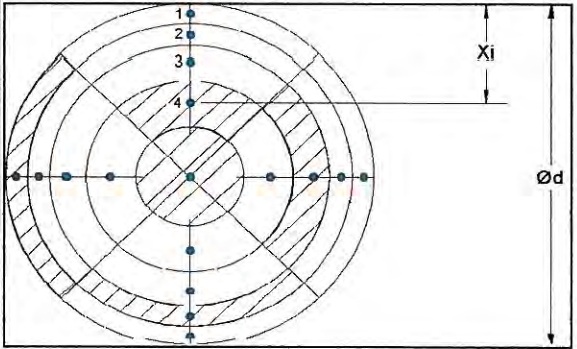
The implicit ISO 9096:2003 error factor of +/- 12 % was considered as satisfactory, as was the + 7% isokinetic correction factor applied to the calculation.

Differential Pressure Test:	Pass
Temperature Range Test:	Pass
Minimum Pressure Test:	Pass
Tmax:Tmin:	Pass
Vmax:Vmin:	Pass
Drift Angle:	< 15°
Droplet Test	No Droplets
Has Homogeneity Test:	20 point CO as 2 locations: Pass
Tester:	T Growcott MM 03/314
Sampling Location:	BS 3405 ports @ Compliant Location
Deviations (From Method):	None



Pitot Measurements

BS 13284-1		ISO 9096:2003	Y
BS6069:		Please tick the relevant box	

Client:	David Smith St Ives Limited	Date:	11th March 2011			
Address:	Marley Road	Operator:	T Growcott			
	St Ives	Job Number:	HE 11 / 7839			
	Huntingdon	Location:	Wood Burner			
	Cambs PE 27 3EX	Instruments:	IM Pitot + BS 1042 Pitot			
Details of Duct:	Insulated Steel		Atmos. P (pa)	Atmos. Temp K		
Duct Shape:	Circular	Initial:	103	279.1		
Dimension / Dia.:	0.3	Final:	104	279.9		
Area:		Mean:	103.5	279.5		
	Axis 1:	Axis 2:	Gas Homogeneity Check:	Pass		
Traverse Point	Temp K	Temp K ²	Velocity kPa	V ²		
1	154.2	23777.64	98	9604		
2	154.3	23808.49	104	10816		
3	154.4	23839.36	113	12769		
4	154.6	23901.16	129	16641		
5	154	23716	101	10201		
6	154.2	23777.64	112	12544		
7	154.4	23839.36	117	13689	O2 reference	11%
8	154.6	23901.16	126	15876	Humidity %	58.9
9	154.9	23994.01	101	10201	Ambient K	279.5
10	155	24025	109	11881	Negative Pressure	Pass
11	155	24025	113	12769	Drift Angle	<15°
12	154.9	23994.01	119	14161	Dry Gas Correction	Y
13	154.3	23808.49	92	8464	Pitot Correction	Y
14	154.4	23839.36	98	9604	T Correction	Y
15	154.6	23901.16	107	11449	Vmax : Vmin	Pass
16	154.5	23870.25	113	12769	Tmax : Tmin	Pass
17	154.6	23901.16	120	14400	V _{rms}	110.57018
Total	2626.9	405919.25	1872	207838	Pitot Calibration	1.003
Average	154.5235294	23877.60294	110.1176471	12225.76471	Static Pressure Pv (Pascals)	-1.41
RMS	154.5237941				Mean Stack Temperature K	427.5237941
					Moisture Content %	5.472



SECTION 5
ANALYTICAL RESULTS



5 ANALYTICAL SEQUENCE AND RESULTS

The monitoring strategy was undertaken over one day.

An ongoing continuous assessment of emission clarity, colour and odour at the point of discharge were also undertaken. At no time during this study was there any indication of colouration by dense black smoke.

Periodic monitoring of O₂, water vapour, CO, SO_x, NO_x and VOC were undertaken.

TPM measurement was undertaken on 2 x 30 minute sampling schedules with the filters located outside of the stack.

5.1 ANALYTICAL RESULTS

Analytical mean result data is detailed below: -

Analyte	Test 1	Test 2	Mean	PG 1/12 Max Limit
1. Carbon Monoxide CO (mg/m ³)	240 samples (60 minutes at 15 second intervals)		246	250
2. TPM (mg/m ³)	159.4 1 x 30 mins sample	147.3 1 x 30 mins sample	153.35	200
3. VOC as C (mg/m ³)	240 samples (60 minutes at 15 second intervals)		6.412	20
4. Oxygen (%)	240 samples (60 minutes at 15 second intervals)		9.91	-
5. Water Vapour (%)	2 x 30 mins sample	2 x 30 mins sample	5.472	-
6. Oxides of Sulphur SO _x (mg/m ³)	240 samples (60 minutes at 15 second intervals)		1.04	-
7. Oxides of Nitrogen NO _x (mg/m ³)	240 samples (60 minutes at 15 second intervals)		78.0	-
8. Formaldehyde (mg/m ³)	1.14 (1 x 30 min sample)	0.72 (1 x 30 min sample)	0.93	-
9 Chlorides (as HCl) (mg/m ³)	1.19 (2 x 30 min sample)	-	1.19	-



Stack S1 – Volatile Organic Compounds (VOC as C)

Job Number:	HE 11 / 7839
Client:	David Smith St Ives
Date:	11th march 2011
Release Point Stack Ref	S1
Instrument Type	FID
Calibration Gas	Methane
Sample Number	7839/VOC/001 - 240
Test Start (Ti)	07.55.00
Test Finish (Tf)	08.55.00
Test Duration (mins)	60
% Carbon	75
Sampling Rate Interval (secs)	15
No. of Samples	240
Maximum Reading (mgC/m³)	9
Minimum Reading (mgC/m³)	0
Mean Reading (mgC/m³)	6.412



Stack S1 – Total Particulate Matter

Job Number:	HE 11 / 7839
Client:	David Smith St Ives
Date:	11th march 2011
Release Point Stack Ref	S1
Tester	T Growcott
Test Method	ISO 9096:2003
STA Reference	MM 03 / 314
-ve Pressure Test	Pass
Droplet Test	Pass
Vmax:Vmin Test	Pass
Tmax:Tmin Test	Pass
Pressure Differential Test	Pass
Drift Angle	<15°
Gas Homogeneity Test	20 point CO Pass
Instrument Type	Anderson Portable
Sample Number	7839/TPM/001/2
Test Start (Ti)	08.00.00
Test Finish (Tf)	09.00.00
Test Duration (mins)	60
Heater Box Inlet C	18
Heater Box Outlet C	19
MID 1 Correction	Duplicate Samples
Sampling Head	TPM 002
Sampling Points	4
No. of Samples	2 x 30 mins
Maximum Reading (mg/m³)	159.4
Minimum Reading (mg/m³)	147.3
Mean Reading (mg/m³)	153.35



Stack S1 – Water Vapour

Job Number:	HE 11 / 7839
Client:	David Smith St Ives
Date:	11th march 2011
Release Point Stack Ref	S1
Instrument Type	US EPA method 4 test box
Sample Number	7839/Water/001/2
Test Start (Ti)	07.55.00
Test Finish (Tf)	08.56.00
Test Duration (mins)	61
No. of Samples	2 x 30 mins
Mean Reading (%)	5.472

Stack S1 – Formaldehyde

Job Number:	HE 11 / 7839
Client:	David Smith St Ives
Date:	11th march 2011
Release Point Stack Ref	S1
Instrument Type	Halcyon Test Box
Sample Number	7839HCHO/001/2
Test Start (Ti)	07.55.00
Test Finish (Tf)	08.58.00
Test Duration (mins)	63
No. of Samples	2 x30 mins
Maximum Reading (mg/m³)	1.14
Minimum Reading (mg/m³)	0.72
Mean Reading (mg/m³)	0.93



Stack S1 – Chlorides (as HCl)

Job Number:	HE 11 / 7839
Client:	David Smith St Ives
Date:	11th march 2011
Release Point Stack Ref	S1
BS 1911-3 Sampling Train	Test Box 2
Sample Number	7839/HCl/001/2
Test Start (Ti)	07.55.00
Test Finish (Tf)	08.56.00
Test Duration (mins)	61
Sampling Rate Interval (mins)	30
No. of Samples	2 x 30
Mean Reading (mg/m ³)	1.19

Stack S1 – Gaseous Components

Job Number:	HE 11 / 7839	HE 11 / 7839	HE 11 / 7839
Client:	David Smith St Ives	David Smith St Ives	David Smith St Ives
Date:	11th march 2011	11th march 2011	11th march 2011
Release Point Stack Ref	S1	S1	S1
Instrument Type	Eurotron Combustion Gas Analyser		
Calibration Gas	Self Calibrating Cells		
Sample Number	7839/CO/001 - 240	7839/NOx/001 - 240	7839/SOx/001 - 240
Test Start (Ti)	08.00.00	08.00.00	08.00.00
Test Finish (Tf)	09.00.00	09.00.00	09.00.00
Test Duration (mins)	60	60	60
Sampling Rate Interval (secs)	15	15	15
No. of Samples	240	240	240
Maximum Reading (mg/m ³)	730	91	3
Minimum Reading (mg/m ³)	124	63	1
Mean Reading (mg/m ³)	246	78	1.04

These results are reported in accordance with the protocol defined by LA-PPC/EPR and are expressed at standard reference conditions of 273K and 101.3 k Pa, with correction for 11 % oxygen content. The main VOC components determined in post sampling analyses were hydrocarbons and pyrolysis fragments as anticipated from wood feeds stocks. The TPM components determined in the duct air stream emission were composed mainly of carbonised soots.





SECTION 6
VISUAL ASSESSMENT



6 VISUAL ASSESSMENT

6.1 VISUAL ASSESSMENT

In accordance with the provisions of LA-PPC/EPR an assessment of discharge emissions was undertaken throughout the monitoring period.

The assessment was carried out with reference to the methods and procedures detailed in BS 2742C:1969.

The process related emissions were evaluated; the emission discharge colour for the stack was determined as < RInglemann shade 1 throughout the study period.



APPENDIX 1

INSTRUMENT CALIBRATION LOG



HALCYON ENVIRONMENTAL CALIBRATION RECORD LOG

	Doc. Ref:	CL001
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No.	Equipment	Serial Number	Model	Date of Calibration	Certificate Number
01	Airflow Developments	114575	PVM 100	28.11.2010	IC1145P
02	Airflow Developments	N / A	BS1042 2A	28.11.2010	IC1145P
03	Eurotron Gas Analyser	00724899	3000 Professional	24.11.2010	JMW
04	Eurotron	N / A	Probe	12.11.2010	20615
05	Rothero and Mitchell	7173	Airflow 3	Calibrated Internally Against Standard	HE 09 / 22612
06	Rothero and Mitchell	6886	Airflow 3	"	HE 09 / 22613
07	Rothero and Mitchell	4130	Airflow 3	"	HE 09 / 22614
08	Rothero and Mitchell	5217	Airflow 3	"	HE 09 / 22616
09	Rothero and Mitchell	9413	Airflow 3	"	HE 09 / 22617
10	Rothero and Mitchell	9228	Airflow 3	"	HE 09 / 22618
11	Rothero and Mitchell	1927	Airflow 3	"	HE 09 / 22615
12	Rothero and Mitchell	1567	Airflow 3	"	HE 09 / 22610
13	SKC	22721	22549 Rotameter 0.300mls/min	10.11.2010	10712
14	Knauer Modular HPLC System	162217		Daily Using Supelco Standards	
15	Digitron with pitot and thermo micro anemometer	451097801	PM 80	10.11.2010	ATP
16	Signal Instruments 3030	IHS		Hire certification	
17	Bubble Meter	22806	Optiflow 420	10.10.2009	HE 09 / 22714
18	Perkin Elmer 8600 GC	1092	S410 9C	16.11.2009	HE 09 / 22617

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APPENDIX 2

STATEMENT OF COMPETENCY



Halcyon Environmental
27 Brunel Grove
The Woodlands
Perton
Wolverhampton
WV6 7YD

Mobile: 07779 008725

E-Mail: tim@halcyon-environmental.co.uk

Age: 58

Qualifications: B Sc (Hons) Applied Chemistry
Member of the Royal Society of Chemistry MRSC
Chartered Chemist C.Chem
Chartered Scientist C.Sci
Member of the Institute of Metal Finishing (MIMF)
Member of the Source Testing Association (STA)
STA registration MM 03/314

Current Position

Halcyon Environmental: Senior Partner

Responsible for the operation of a specialist environmental consultancy including sales and marketing, presentations, technical procedures, litigation protocol, analytical strategies and Environmental Management Systems Protocols.

Halcyon Environmental is a consultancy specifically committed to advise and support Industrial and Private Sector clients in achieving and effectively maintaining compliance with existing and new environmental legislation.

Halcyon is a member of the Metal Finishing Association and Surface Engineering Association.

Courses Attended

2009	Lanyard Training and Working at Height – Kingfisher Access Course
2008	STA M Certs Level 1 Training Course
2008	STA M Certs TE3 Revision Training; Gases and Vapours by Extractive Manual Measurement
2008	IEMA presentations
	Introduction to the REACH Regulations Rolls Royce Sinfin
	Introduction to the EUPD Environment Agency
	Introduction to EPP Environment Agency
2001/2/3/4/7/8	PCME; Total Particulate Monitoring – Isokinetic, Triboelectric, Tribostatic, Scintillation, Optical and CEM methods and systems



2007	PCME; On Line, Real Time Monitoring and Calibration
2007	Environmental Compliance (ECL): An Introduction to BS 14181
2007	Environmental Compliance (ECL): Gas Monitoring Systems
2007	CBiss - Instrumental Continuous Gas Monitoring Applications
2006	PCME; Particulate Monitoring Techniques and Calibration Methods
2006	Turbidity Monitoring Techniques; Partech Instruments
2006	PCME; Dust Reporter 2 Software and Filter Management
2006	PCME; Improving OMA Score/ Interpreting Guidance Notes
2006	PCME; PMT in the Metal Industries – Case Studies
2006	MCERT for Effluent Monitoring; Partech Instruments
2005	PCME; – Continuous Particulate Monitoring Systems (CEMS)
2002	PCME; Optical and Probe based Technologies for Emission Monitoring
2002	PCME; CEMS Analyser Systems
2002	PCME / C Biss; Cross Duct, Heated Extractive and Drying Extractive Techniques and the requirements of CEMS Systems, MCERTS and OMA
2001	Disa An Introduction to Abatement Systems
2001	PCME Particulate Monitoring Solutions FMC
2001	PCME; Particle Velocity and Mass Monitoring Techniques FMC
2001	PCME; Ambient Monitoring Techniques FMC
2001	PCME; MCERTS and TUV Accreditation Schemes FMC
2000	PCME; Practical Demonstrations for TSP PM-10 and Pm 2.5 monitoring
2000	PCME; Monitoring of Suspended Solids in Gas Streams
2000	PCME; System Configuration and Reporting
2000	Servomex; The Continuous Monitoring of Gaseous Emissions
2000	PCME; Particulate Monitoring and the Workplace
1997	Air Pollution Standing Conference – NEC
1997	Monitoring as a Management Tool; SEC/ MFA Workshop
1997	FMEA to Design – Out Problems MFA / Ad – Qual Workshop
1997	Practical Application of Personal Protective Equipment – MFA / Racial Workshop



- 1997 Solid Wastes – A Finisher's Perspective MFA
- 1997 Oven Temperature Control using Radio Telemetry; Grant Instruments
- 1997 Introduction to Air Sampling; SKC Ltd
- 1997 Profitability and the Monitoring and Control of Energy and Water; Marquis Associates
- 1996 European Perspectives on Environmental Best Practice; ERM
- 1996 Regulatory Developments in the UK WM Hazardous Waste Unit
- 1996 Thermal Sand Reclamation – Economic Drivers Towards Installation, Landfill Tax and its Consequences; Thermofire
- 1996 Metal Screen Filters as a Candidate for Best Practice; Air Filters
- 1996 Ceramic Filters and Secondary Metal Processing; Withers Metals
- 1996 Environmental Technology Best Practice Programme; ETSU
- 1996 Accounting for Environmental Performance; MRC
- 1996 Principle and Practice of Waste Management; Wedge Holdings
- 1996 The Waste Minimisation Agenda; UOW Workshop
- 1995 Air Pollution Standing Conference; NEC
- 1994 Eurosafe - Personal Protective Equipment; Assessing Needs and Choice
- 1994 GEC A Practical Approach to Health and Safety Management
- 1994 MOHS – Health Surveillance
- 1994 Government Policy Towards Business and the Environment – MFA Conference
- 1994 Engineering Industry and Environmental Pressure – MFA Conference /EEF
- 1994 Is BS 7750 Relevant to Metal Finishing; MFA Workshop
- 1994 EPA and the Metal Finishing Sector; MFA Workshop
- 1994 Environmental Management; Practical Implementation and Action; Business Link
- 1993 Environmental Education – WALCAT Workshop
- 1991 Clean Air Engineering: Environmental Source Monitoring
- 1991 Clean Air Engineering: Isokinetic Emission Monitoring
- 1991 SGS "Green Dove - EMS Sales Strategy"
- 1990 SGS "Principles of International Trade"



1990	SGS "Sales and Marketing - Value Added Strategies"
1990	SGS Yarsley "TQM Principles and Practices"
1990	SGS "Principles of Environmental Auditing"
1990	SGS "BS 5750 Auditing Protocols"
1990	SGS "Introduction to Green Dove"
1990	SGS "BS 5750 Management Systems; Planned strategy"
1989	BASF – Source Testing
1989	BASF International Analytical Conference
1989	BASF – Principles of LIMS
1988	Qualified First Aider CPR Procedures
1986	Management and Motivation
1980	Paint Research Association: Paint Formulation
1979	Wolverhampton Polytechnic: Advanced Analytical Procedures

Recent Awards, Presentations And Publications

2008	Road Show Speaker – West Bromwich Albion; REACH and its Implications
2007	Williams Alloys and Residues – support to ISO 14001
2006 – 2009	Monthly contributor to Corporate Times
2006	SEA meeting; House of Lords
2006	PCME Road Show Speaker – Ricoh Stadium
2005	Tonge & Taylor ISO 14001
2003	Calcast Limited ISO 14001
2003	C E Marshall (Wolverhampton) Ltd ISO 14001
2003	PCME Road Show Speaker; Celtic SFC
2002	Speaker – Cortec Seminar, University of Coventry – An Introduction to IPPC
2002	PCME Road Show Speaker; Manchester United FC
2002	Kings Triplex Holdings – ISO 14001
2001/4	PCME Road Show – Monitoring of Particulates – Workplace and Environment
2001	Lanstar ISO 14001



- 2001 Yale Security Products UK Ltd – ISO 14001
- 2001 Oldbury Aluminium Alloys Ltd. – ISO 14001
- 1998 World Metals Congress - Budapest. First 10 ISO 14001 foundries - Consultancy support to Transtec Group.
- 1998 Transtec Group - ISO 14001 - Birmingham, Droitwich, Llanidloes.
- 1998 Johnson Controls - ISO 14001 - Silloth and Wednesbury.
- 1998 MPL-Key Group - 1st Plastic Moulder to ISO14001 - Tamworth.
- 1998 MFA - Waste management and minimisation seminar.
- 1998 ISO14001 -The Environmental Standard - BLB.
- 1997 JRI Technologies - 1st. Foam producer to ISO 14001.
- 1995 BS 7750 - A practical guide to compliance. Various industrial sites.
- 1995 "Environmental by Design" - fundamentals of design strategy seminars
- 1995 "Design for Disassembly" - fundamentals of product recycling and reuse.
- 1995 "Product Finite Life Analysis - Environmental Aspects" - GEC Group.
- 1995 Wolverhampton Centre of Engineering Excellence: "Safe usage, storage, handling and disposal of industrial liquids" seminars.
- 1995 Wolverhampton Centre of Engineering Excellence: EPA "Directors in the Dock" seminars.
- 1994 Wolverhampton Centre of Engineering Excellence: EPA Awareness workshop training.
- 1994 BLB: Practical Environmental Management.
- 1994 Birmingham Chamber of Commerce: EHS Management.
- 1994 Speaker - MPS "Environmental Awareness" Seminars.
- 1994 Inst. Elec. Engineers: EPA Evening presentation.
- 1994 Inst. Met. Finishing: Instrumentation and Capability.
- 1992 Metal Finishing Association: EPA Awareness Seminars.
- 1994 Transactions on the Inst. Met. Finishing: EHS legislation, effects on the M F Industry - Annual Technical Conference article.
- 1992 Ceramic Industries International: " Not Entailing Excessive Cost" EPA article.



Career Resume

Tim Growcott is the Senior Partner in Halcyon Environmental, a UK based consultancy, which specialises in Environmental Consulting Services. The consultancy works with around 500 company customers, from engineering to chemical specialists, foam and plastic users, MOD and RAF site's and specialist operators.

Trained formally as an Industrial Chemist, he has worked with companies including Mander Brothers in paints, BL Heavy Vehicles Division at Guy Motors in heavy vehicle manufacturing and Wilkins & Mitchell in domestic appliance manufacturing.

Latterly he worked with the Inmont Corporation and BASF in automotive and printing industry coatings development, and SGS in specialist environmental roles, undertaking diverse environmental issues including sales, marketing, site investigation work, litigation and liability, the development of environmental systems including EN ISO 14001.

Halcyon has undertaken specific and broad spectrum environmental issues with regard to environmental compliance, forward business environmental planning, and cradle to grave strategies that include environmental significance in product design and manufacturing, product finite life analysis, design for disassembly and renewable and recyclable resources.

Halcyon was recognised by the World Metal Congress, held in Budapest in achieving EN ISO 14001 with one of its customers as one of the world's first 10 foundries to achieve the standard.

Halcyon personnel have supported the recent transfer of business from the mainland UK to the Czech Republic, Norway and Bulgaria and are developing business in Portugal.

